

Metals Removal from Groundwater Using Permeable Reactive Barriers (PRBs)

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PRBs for Removal of Inorganic Contaminants from Groundwater

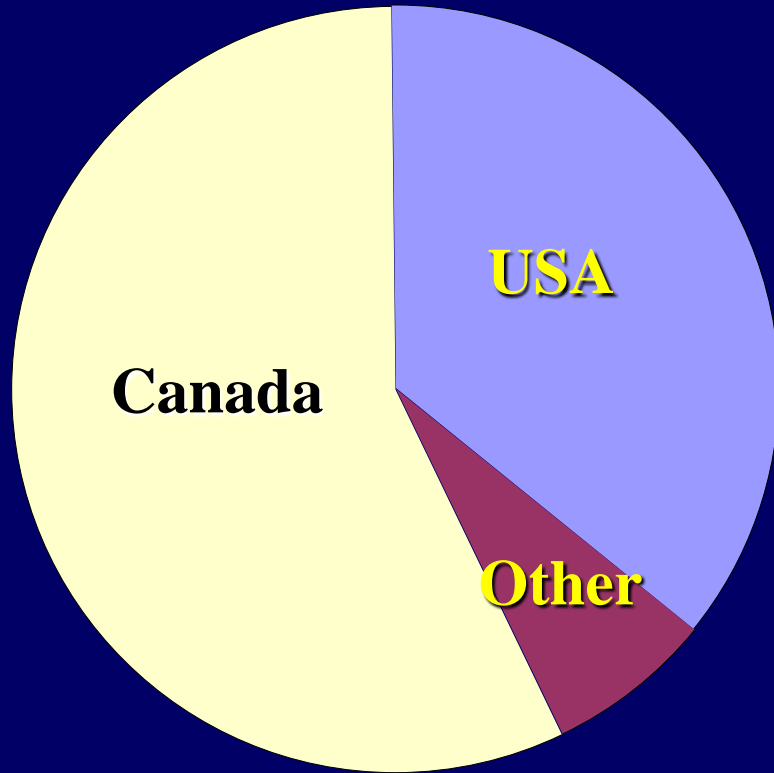
- **University of Waterloo experience**
- **Blowes, Ptacek and Robertson**
- **Metals, nutrients and water-borne pathogens**
- **Plume remediation or control**
- **U.S. Patents 5,362,394 5,514,279
5,876,606**

Geochemical Barriers for Metals

- **Zero-valent iron: reductive precipitation on grain surfaces**
- **Organic carbon: sulfate reduction, denitrification**
- **BOF Slag: sorption and co-precipitation phosphate and arsenic**
- **U.S. Patents 5,362,394 5,514,279 5,876,606**
- **Activated carbon**
- **Limestone (neutralization)**

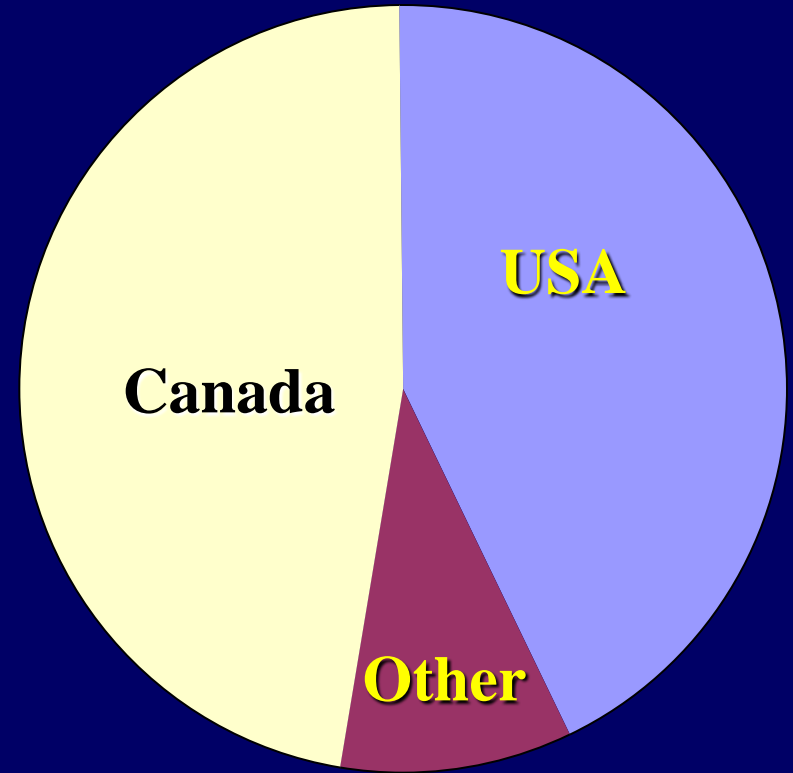
PRBs for Inorganic Contaminants

Pilot Scale Installations



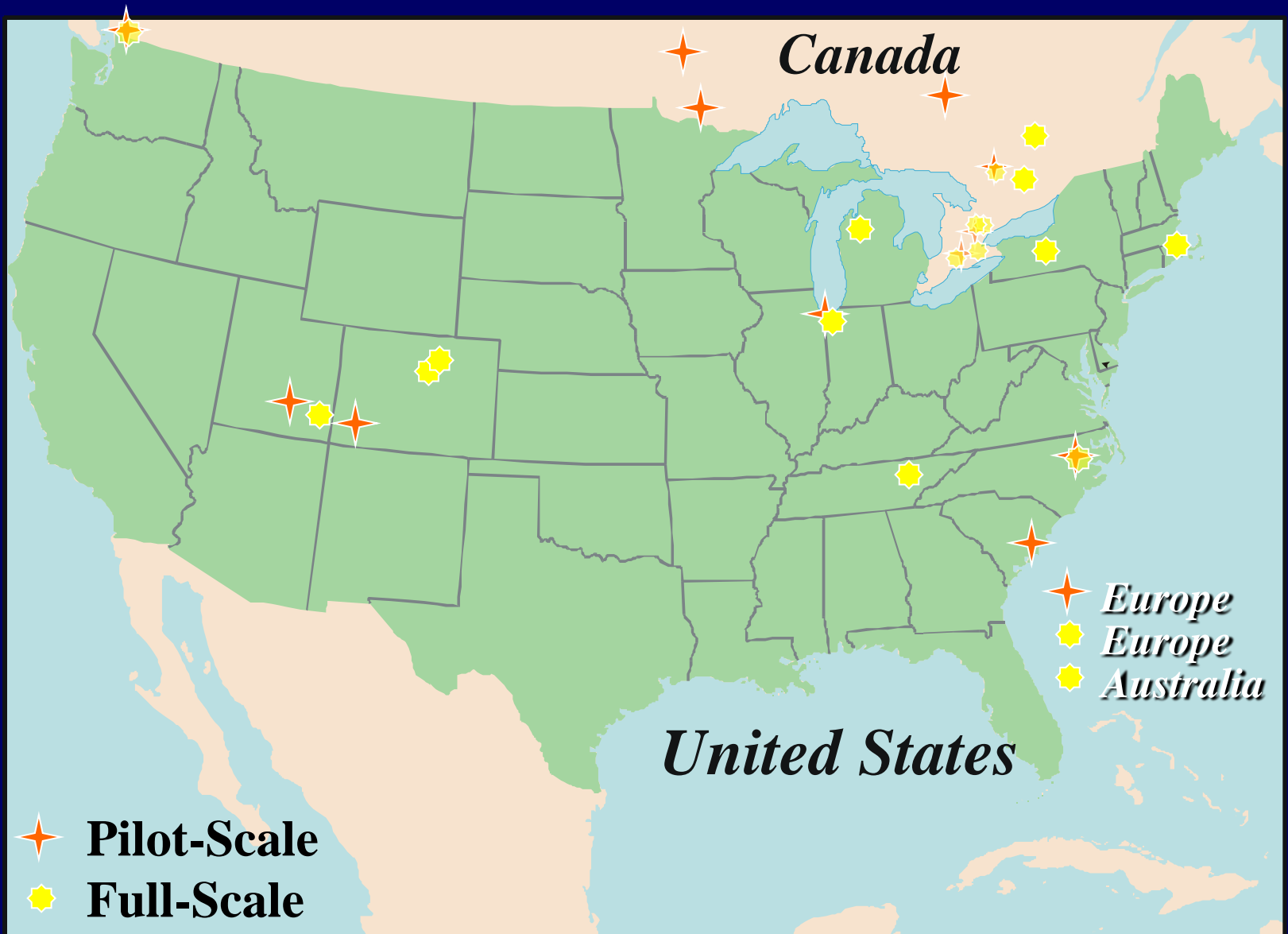
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Full-Scale PRB Installations



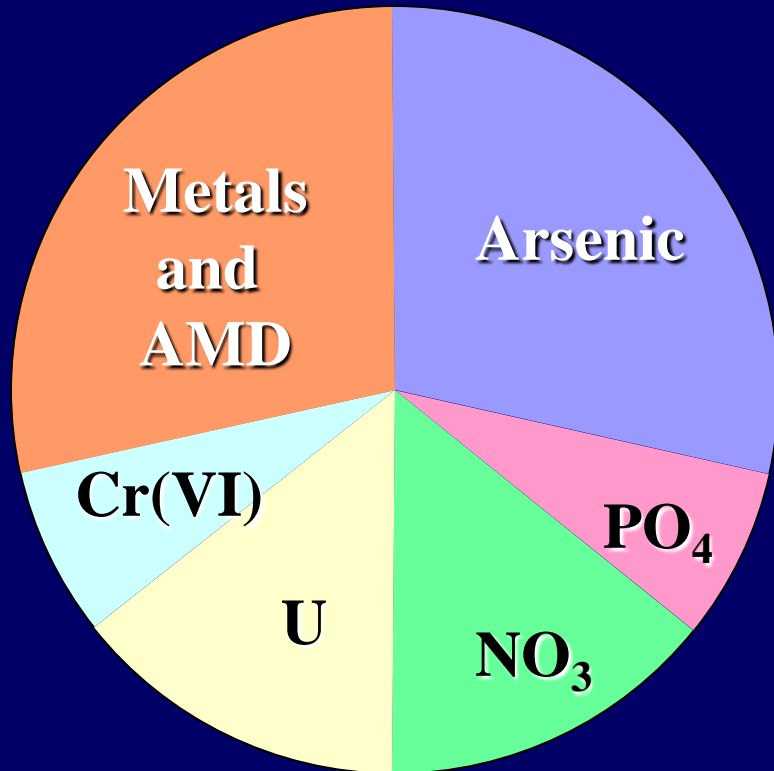
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Inorganic PRB Sites

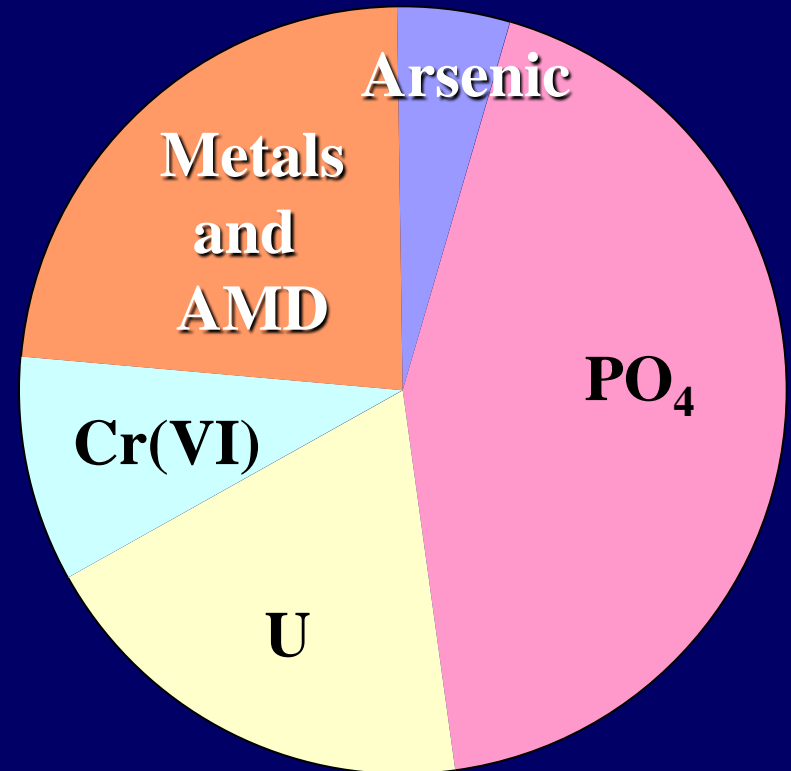


Contaminants Treated

Pilot Scale Installations



Full-Scale PRB Installations



Zero-Valent Iron for Electroactive Metals

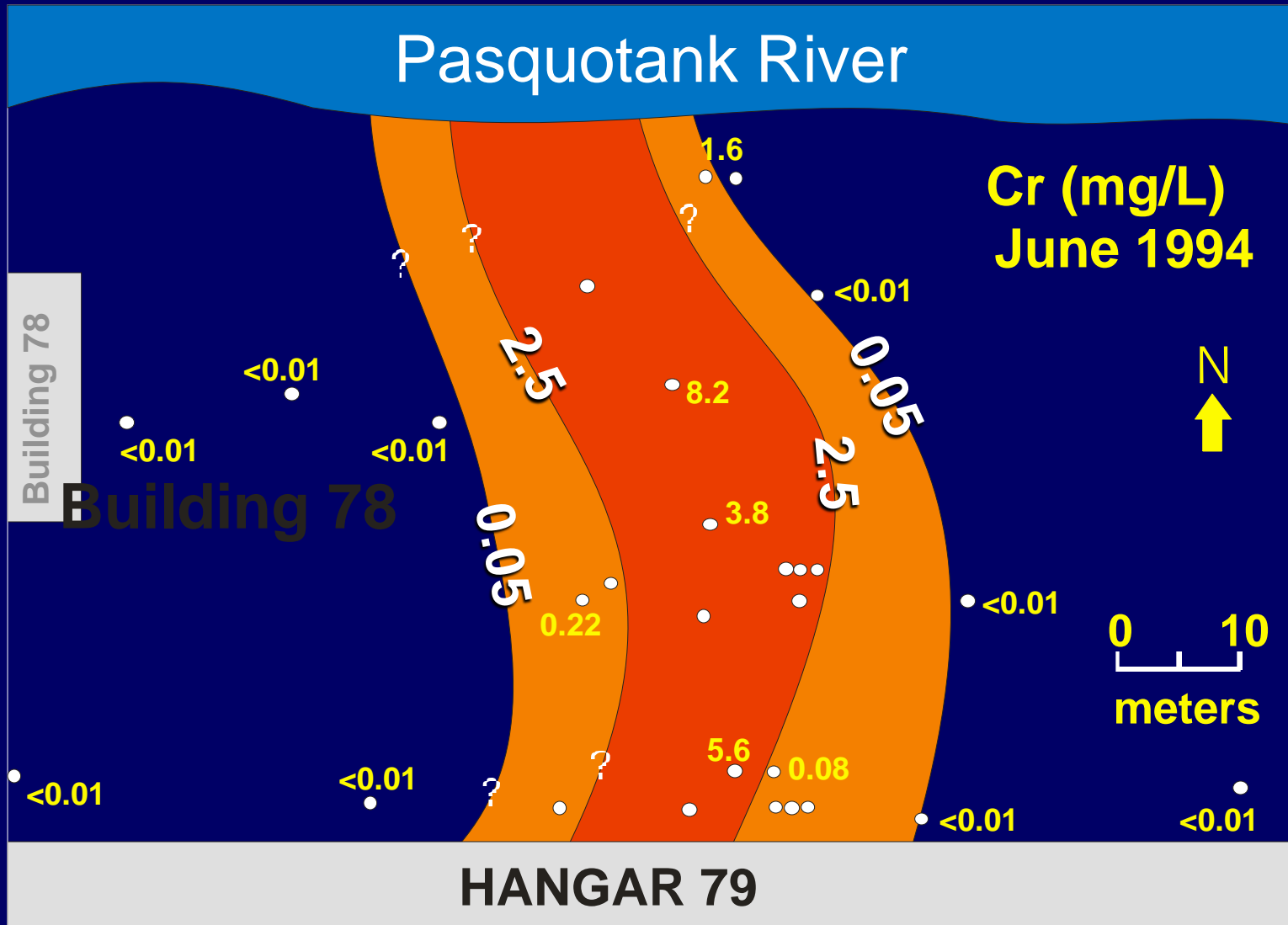
- **Field Installation: Chromium (VI), Elizabeth City, NC**
- **Radionuclides (DOE Facilities)**
- **Arsenic, selenium, mercury**
- **Reductive precipitation on grain surfaces; precipitation or co-precipitation**

Elizabeth City Site

U.S. EPA Project

- Reference

- Blowes, D.W., et al., 1999. An *In-Situ* Permeable Reactive Barrier for the Treatment of Hexavalent Chromium and Trichloroethylene in Ground Water: Volume 1 Design and Installation. Volume 2 Performance Monitoring. Volume 3 Multicomponent Reactive Transport Modeling United States Environmental Protection Agency, Cincinnati, OH, Report EPA/600/R-99/095abc.
- <http://www.epa.gov/ada/pubs/reports.html>



Reactive Material

- 150 m³ zero valent iron (280 tons)
- 46 m long, 7.3 m deep and 0.6 m wide barrier



One-Pass Continuous Trencher



One-Pass Continuous Trencher

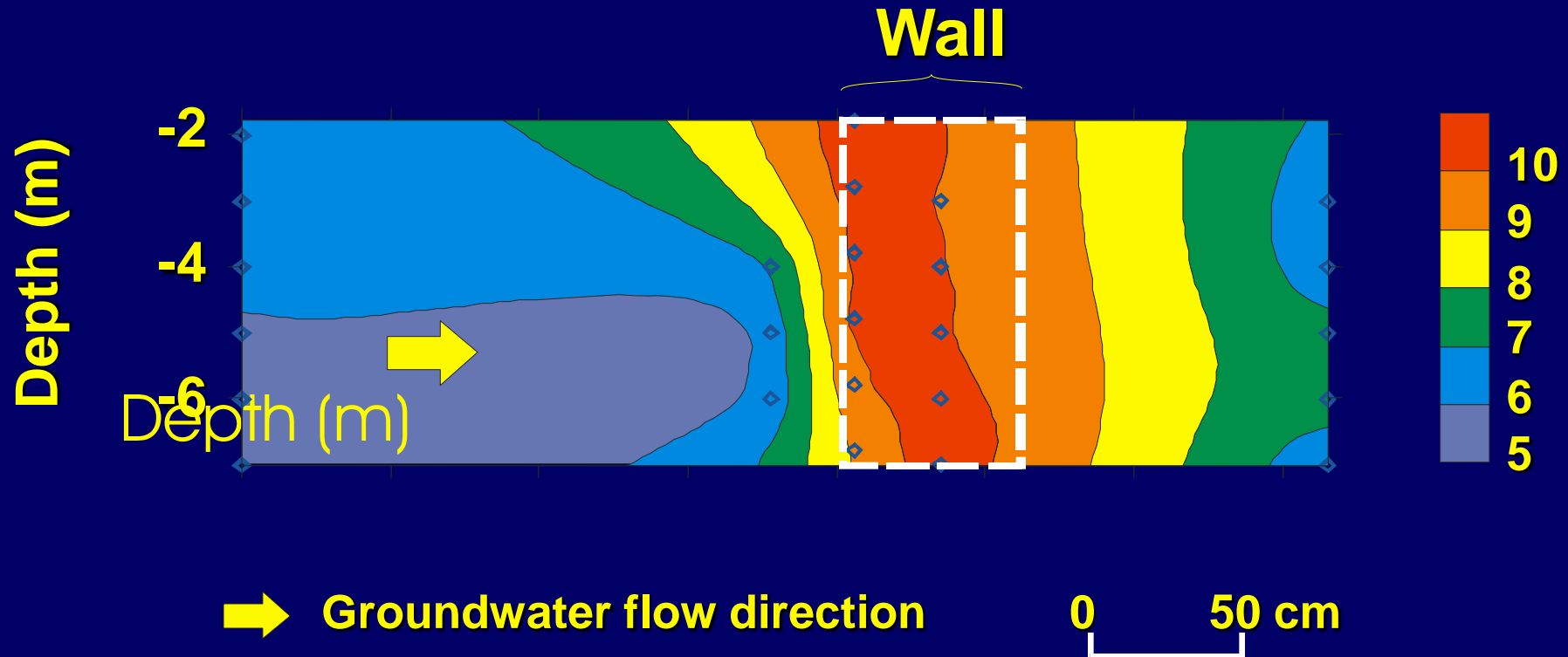


- Depths of < 30 ft
- Width 1-2 ft
- Very rapid installation
- Big equipment
- Mobilization

USCG Wall Installation

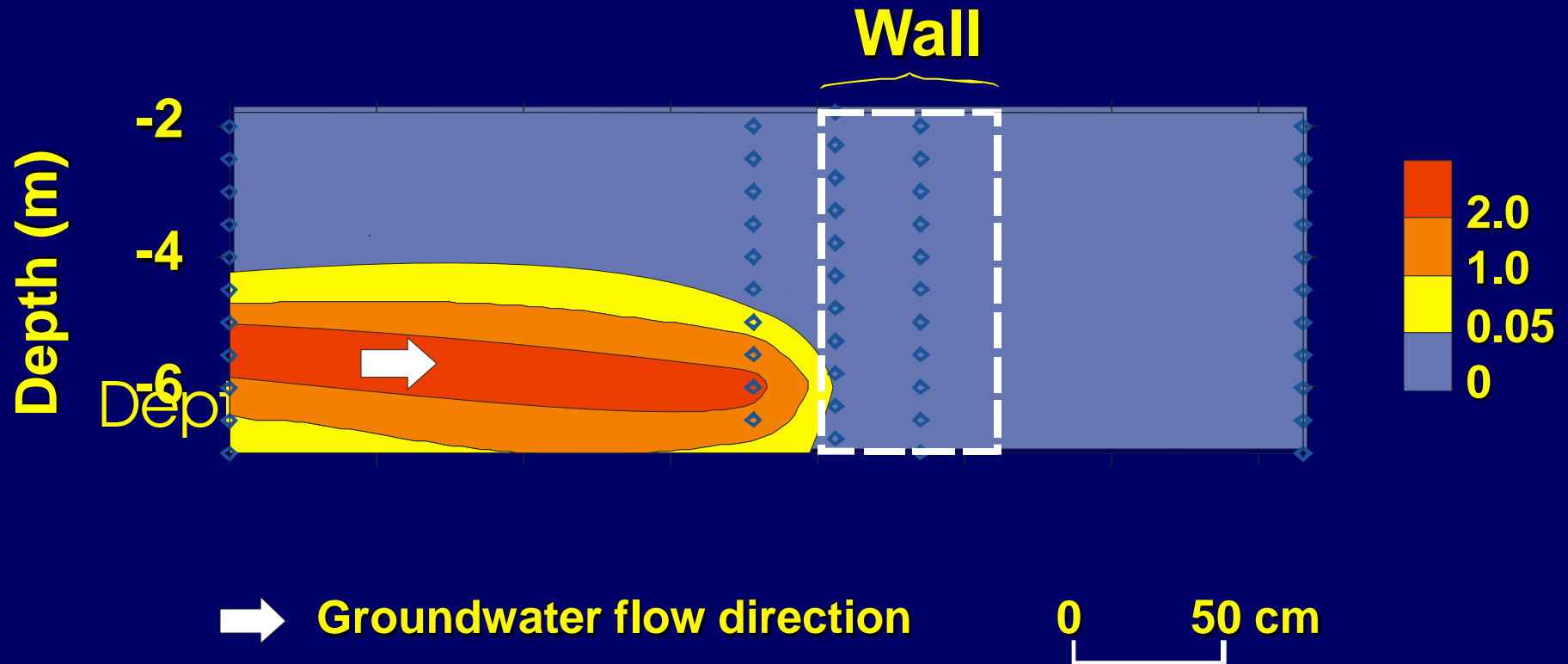


pH



Transect 1 (November 1996)

Cr(VI) (mg/L)

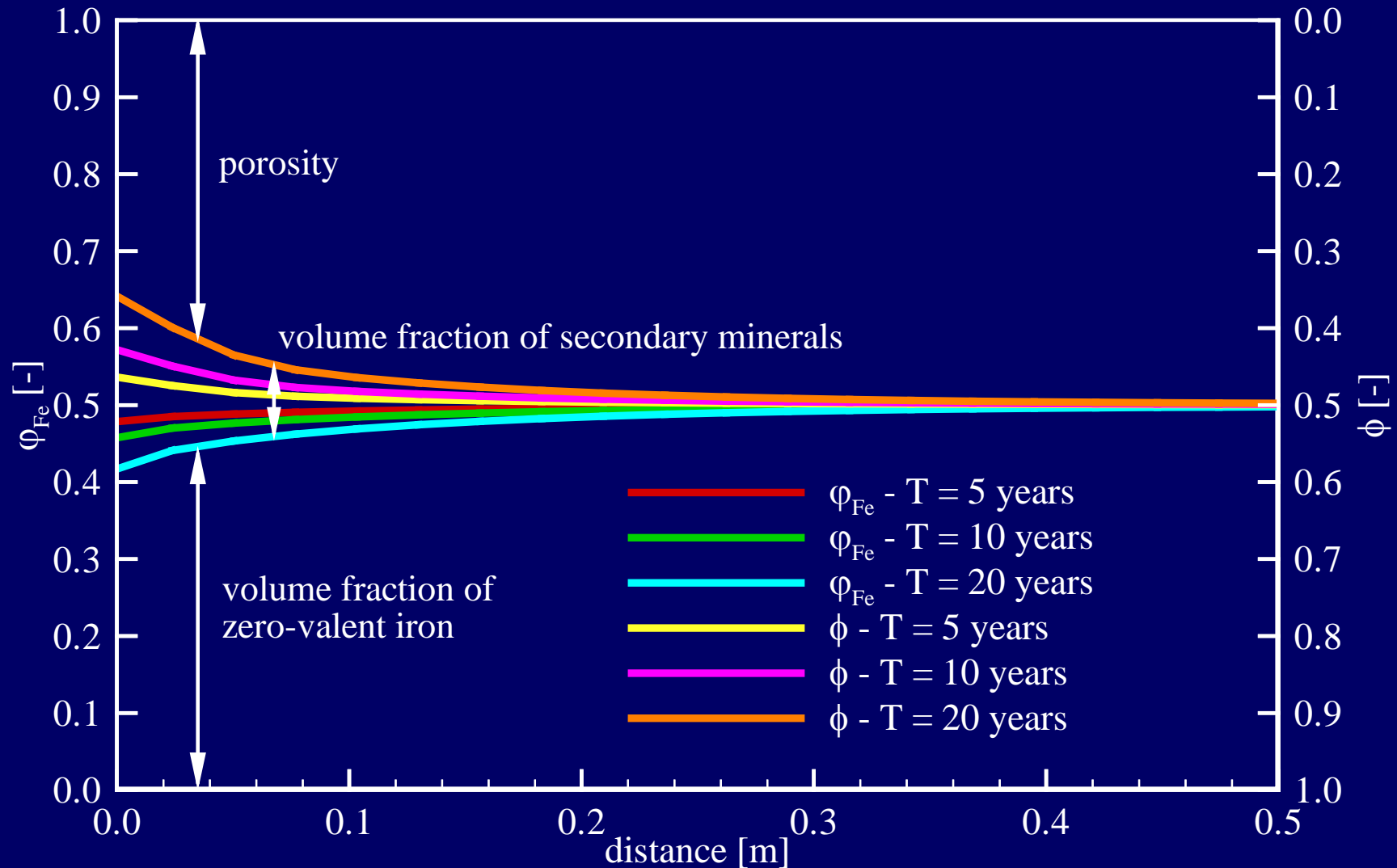


Transect 1 (November 1996)

Mineralogical Characterization

- **Increased solid-phase carbon**
 - Carbonate mineralogy
- **Iron oxyhydroxides**
 - goethite
 - ferrihydrite
 - green rust
- **Iron Sulfides**

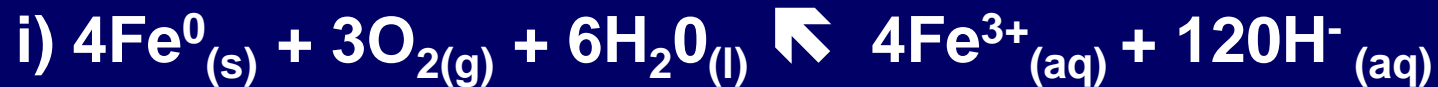
Long-Term Efficiency (Mayer)



ARSENIC

Mechanisms for Removal

1) Reduction and Co-precipitation with Goethite



2) Sulphate Reduction

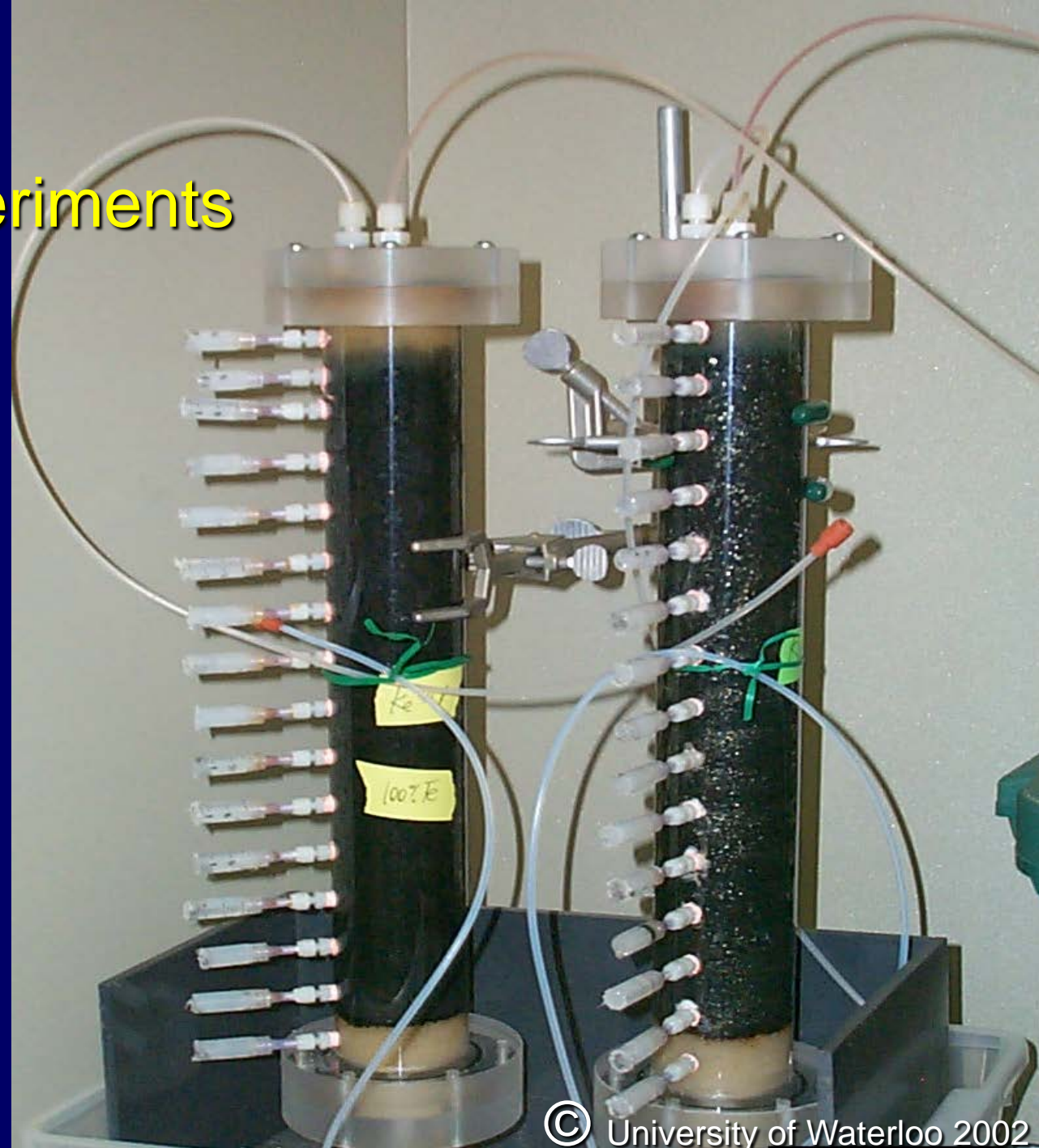


3) Adsorption

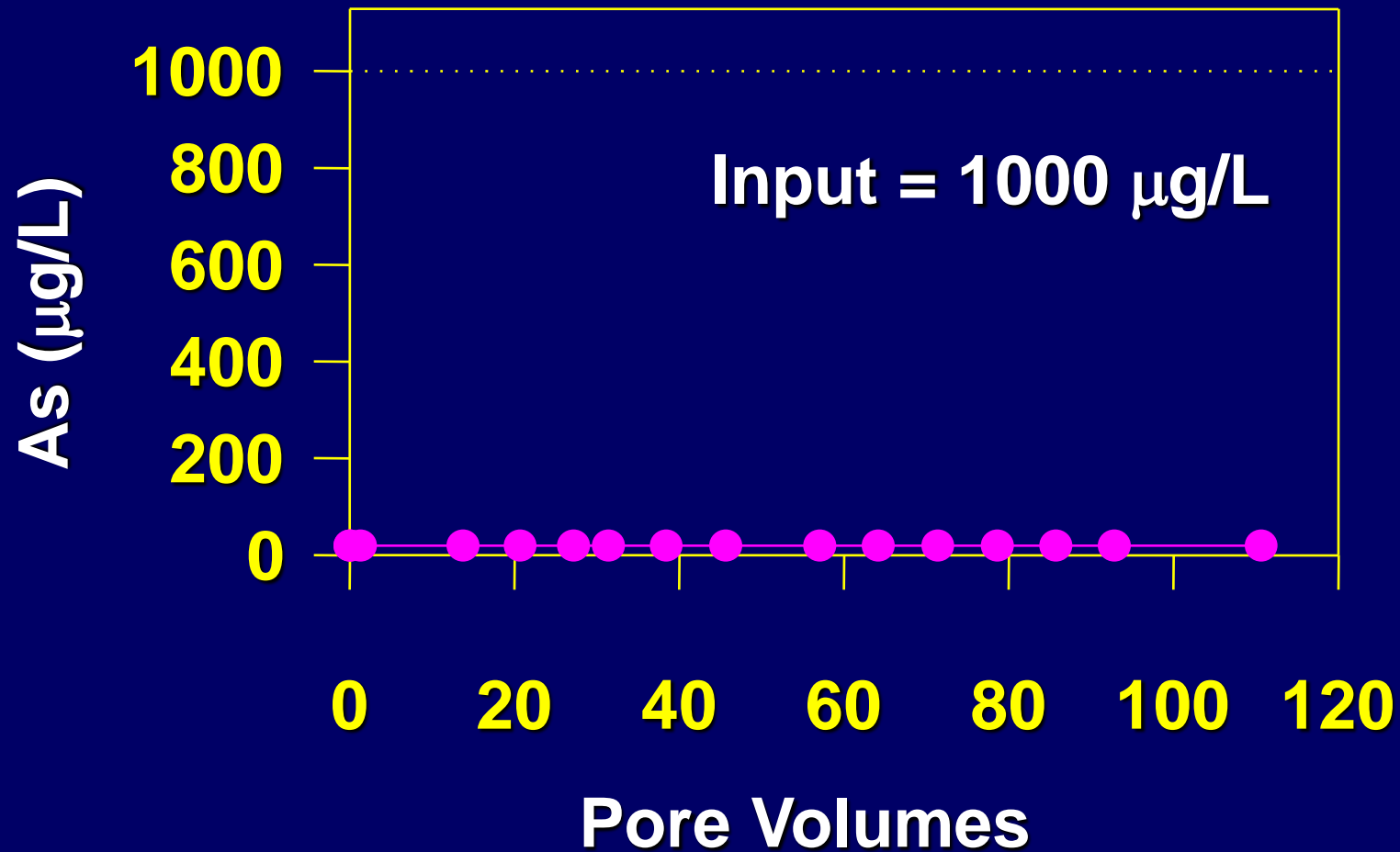
McRae (1999): Arsenic Removal Mechanisms

- **Energy Dispersive X-Ray Analysis**
 - As present in grain coatings and possibly on zero-valent iron grain surface
- **X-Ray Photoelectron Spectroscopy**
 - As(III) predominant in solid phase
 - Reductive precipitation and co-precipitation with goethite in coatings

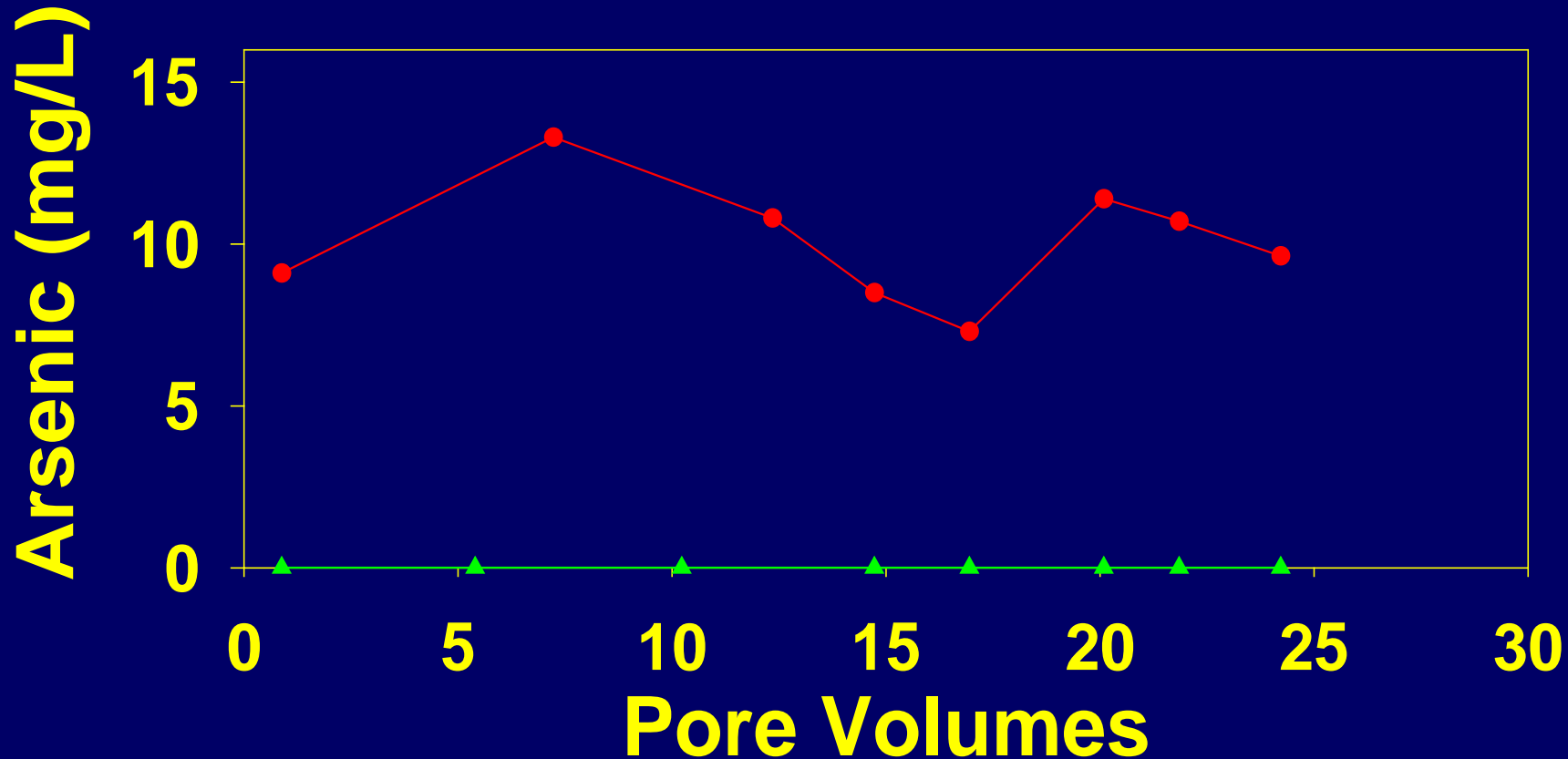
Column Experiments



Zero Valent Iron Column



Arsenic Concentration in 100% Iron Column

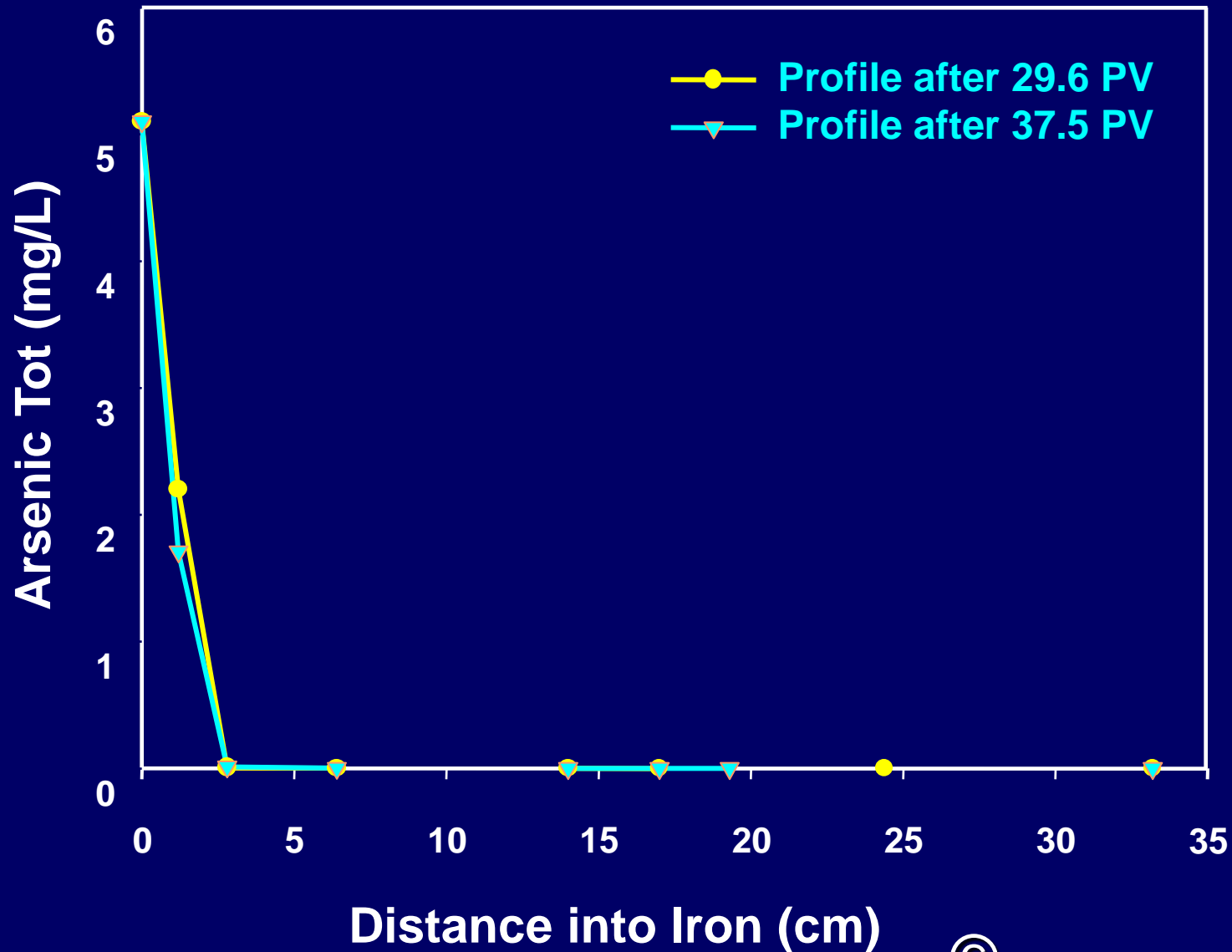


Note: Detection Limit is 0.005mg/L



Total Arsenic Concentration Profiles in ZVI Column

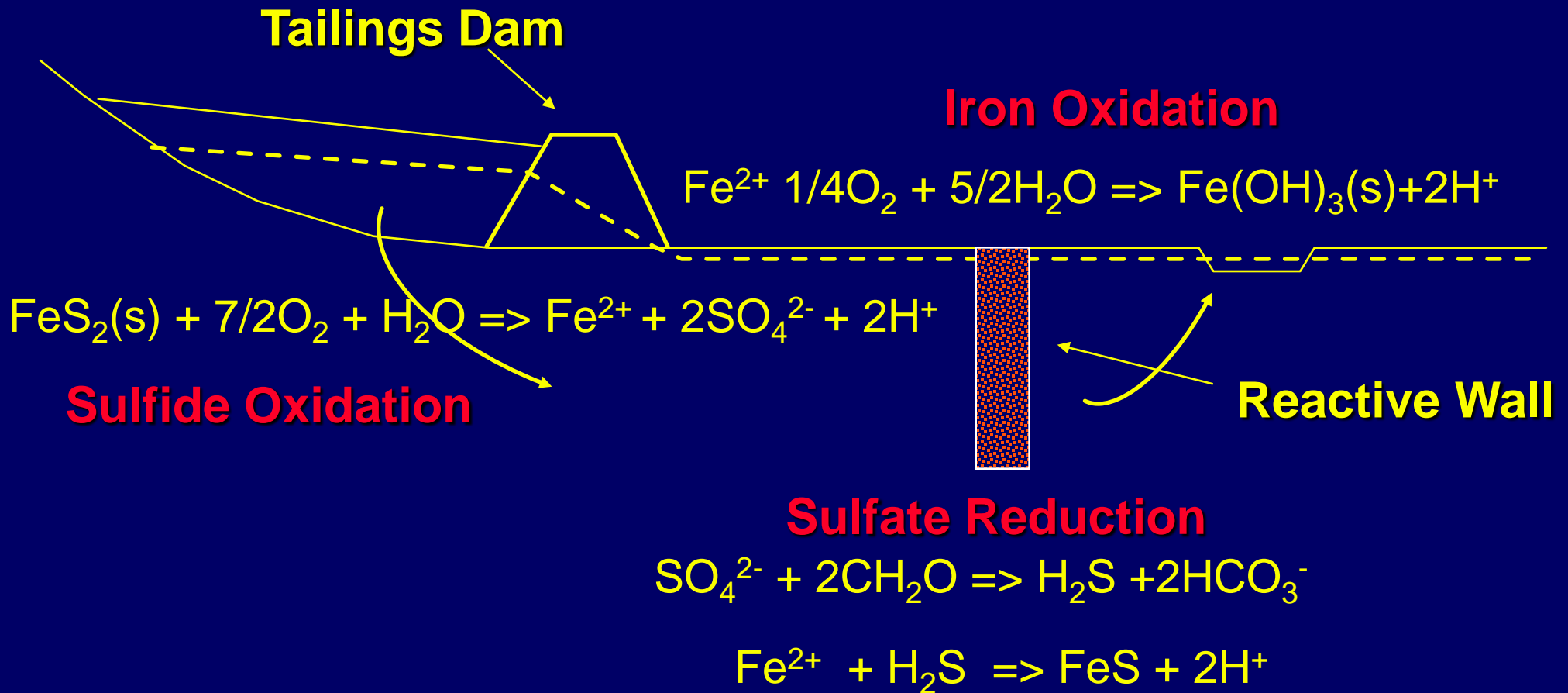
Mine Groundwater at Velocity of 6.75 cm/day



Sulfate-Reduction PRBs

- **Metals in sulfate rich water- AMD**
- **Sulfate reduction is microbially mediated process**
- **Purpose of PRB is to intercept groundwater flow and enhance sulfate reduction**
- **Generation of H₂S and precipitation of metal sulfide minerals**
- **Decrease acid-generating potential; remove dissolved metals**

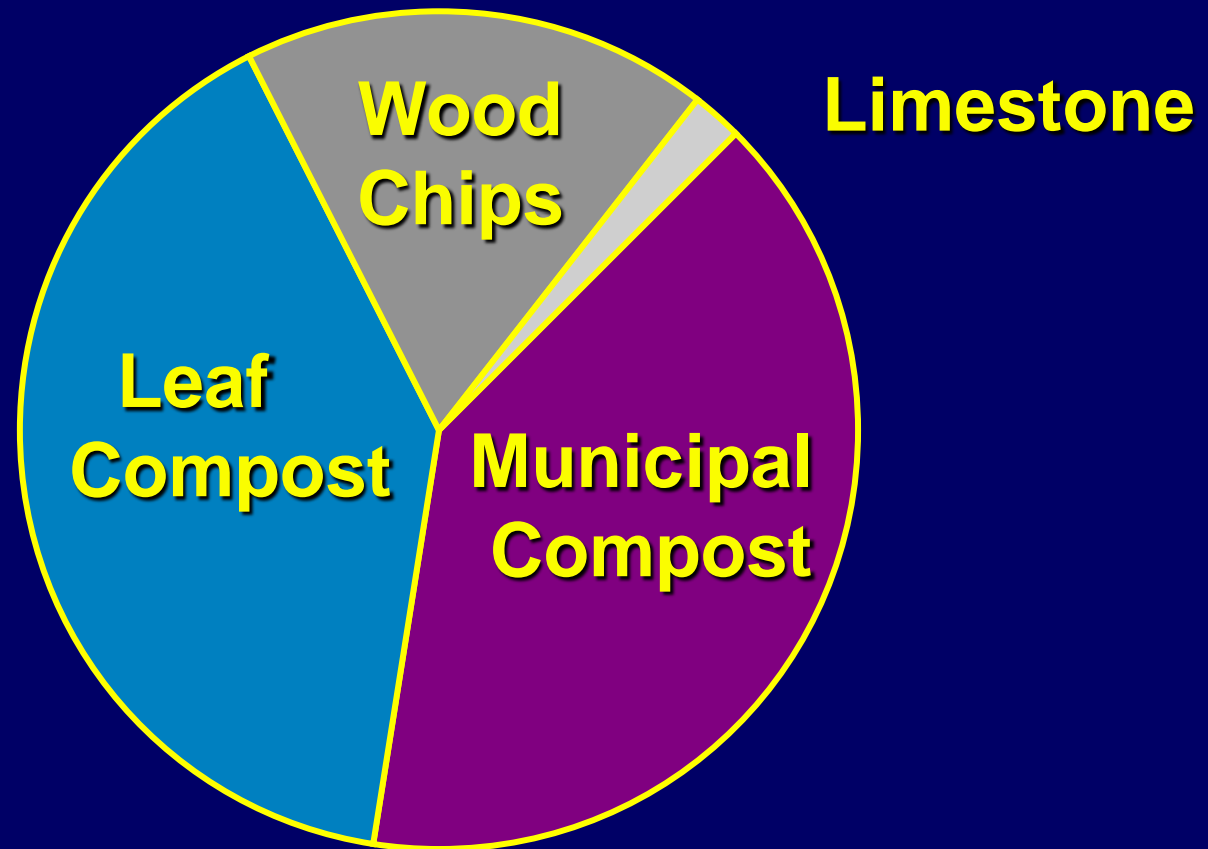
Acid Mine Drainage and Sulfate Reduction



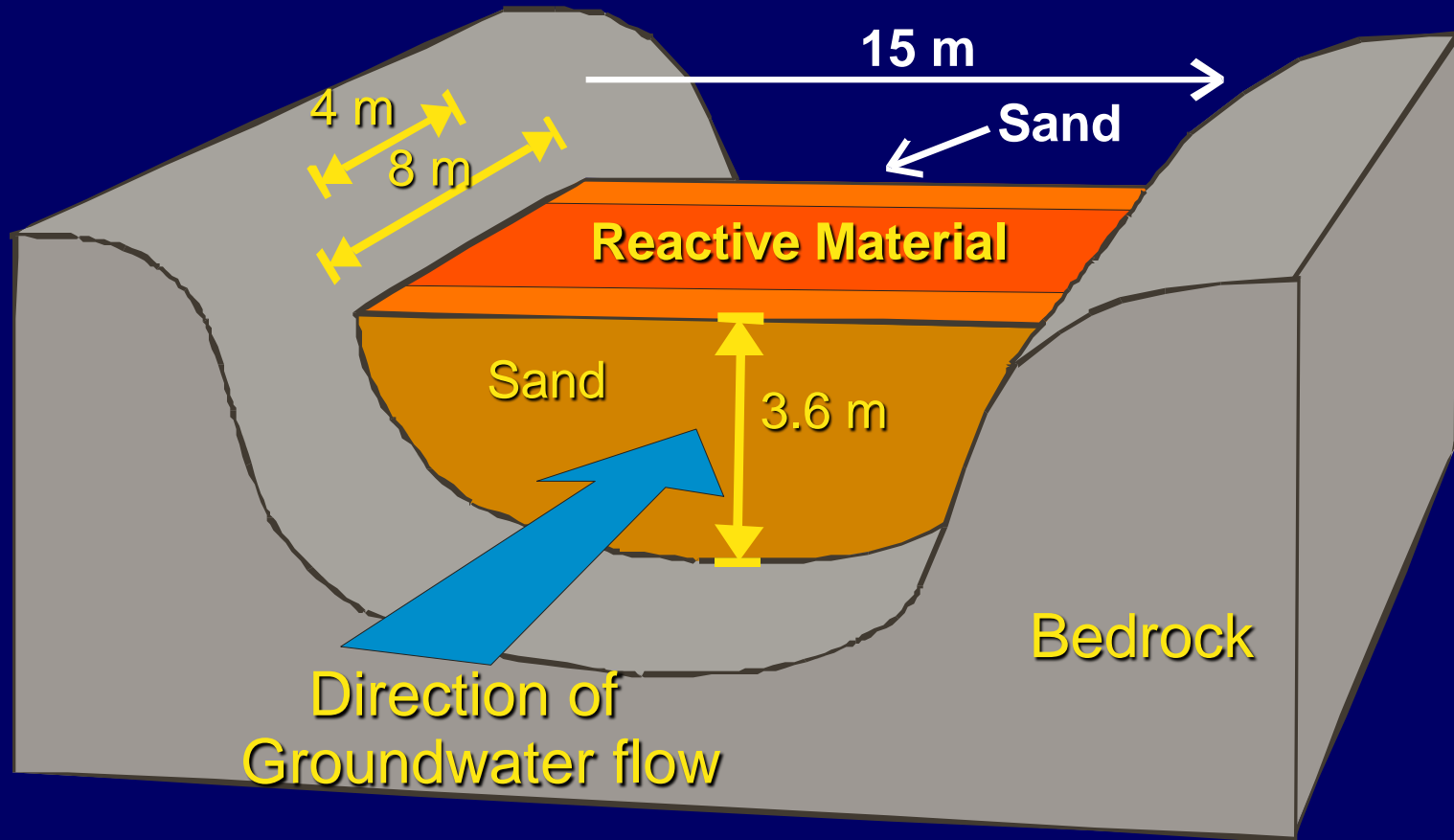
Nickel Rim Mine, Sudbury, ON

- **Laboratory batch and column study**
- **Predictive groundwater flow modelling**
- **Field installation (1995)**
- **Benner et al., 1997; 1999**
- **Waybrant et al., 1998**

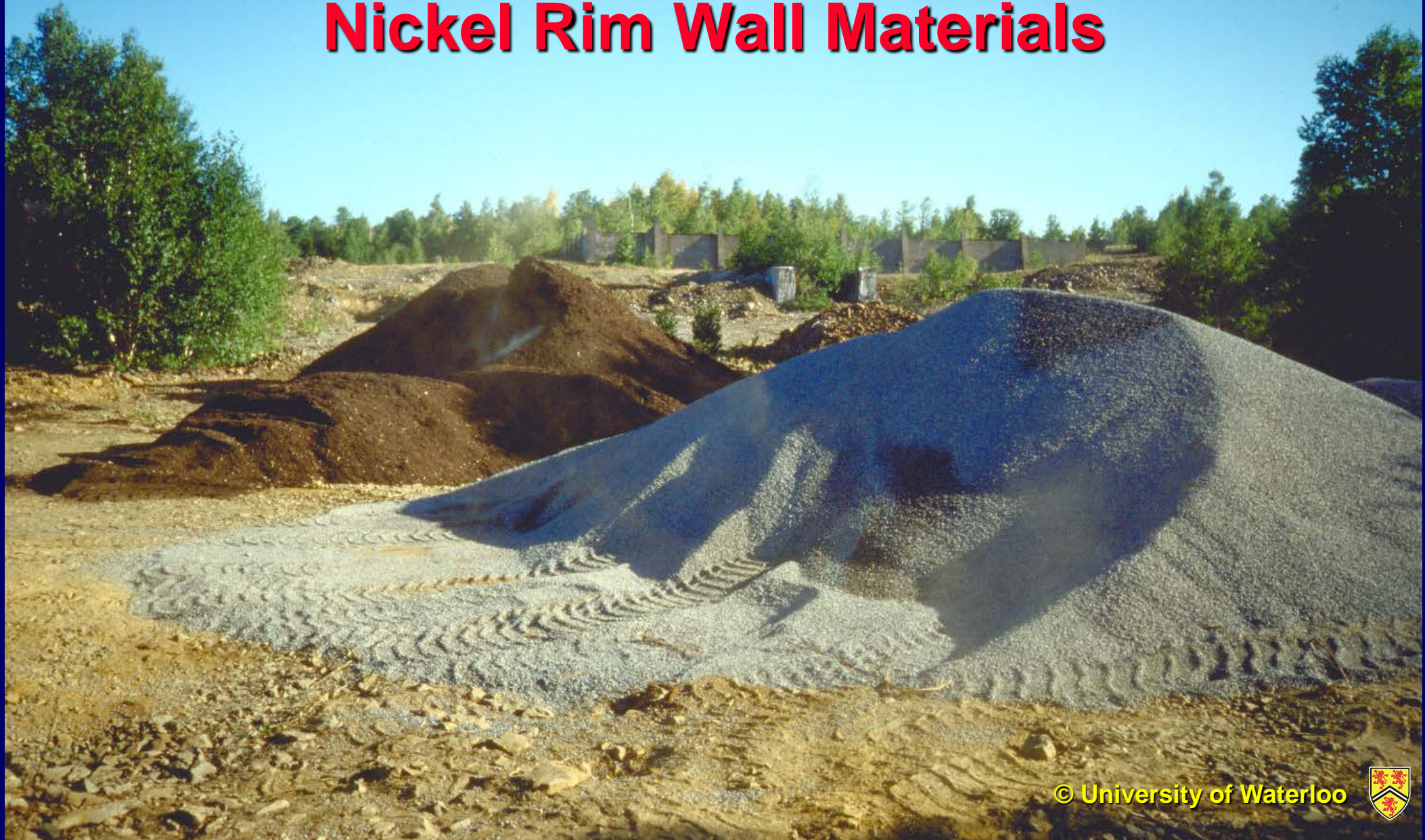
Reactive Mixture Composition for PRB



Porous Reactive Wall Installation



Nickel Rim Wall Materials



NR Wall Installation



Nickel Rim Wall

Sand

Compost

Sand

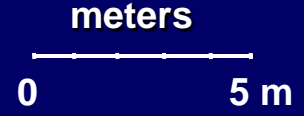
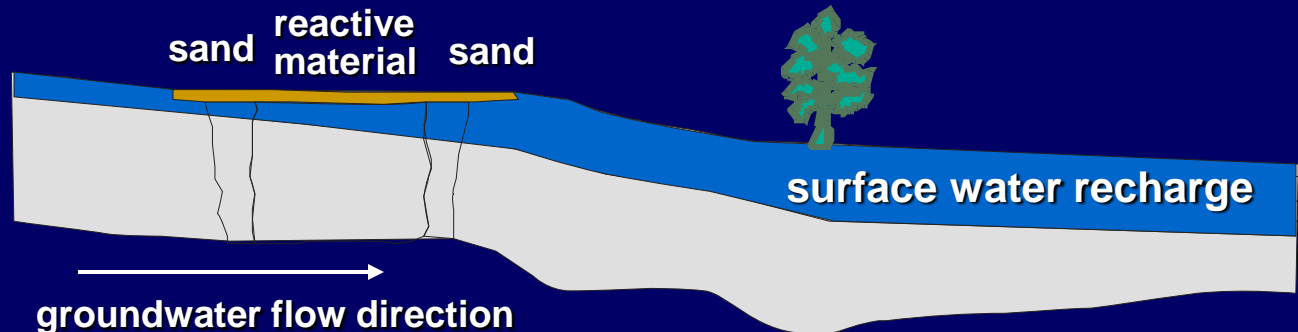


Nickel Rim Wall

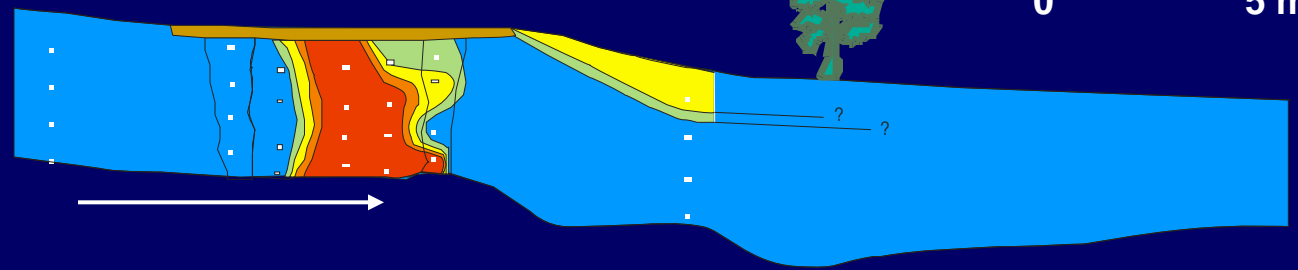
Clay Cap



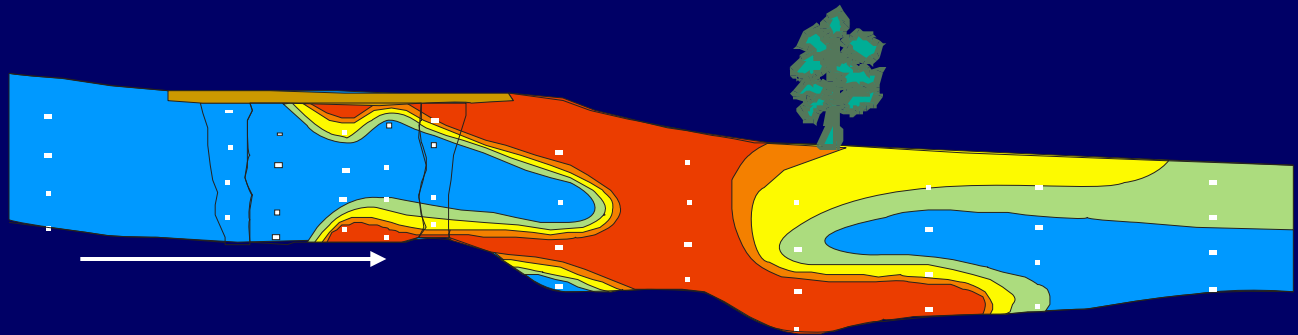
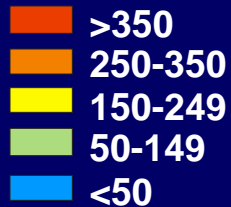
Groundwater Flow



Chloride (mg/L)
Nov. 95

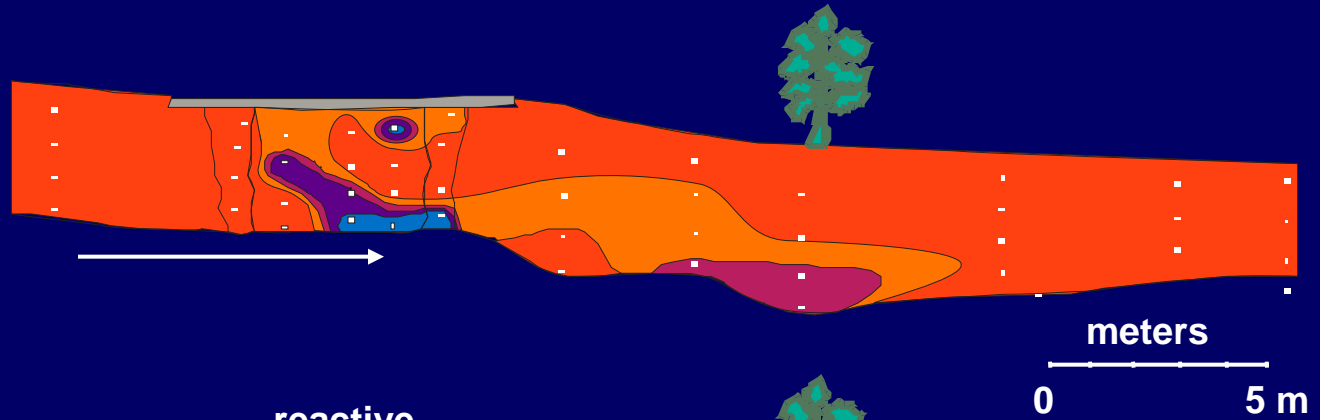


Chloride (mg/L)
June 96

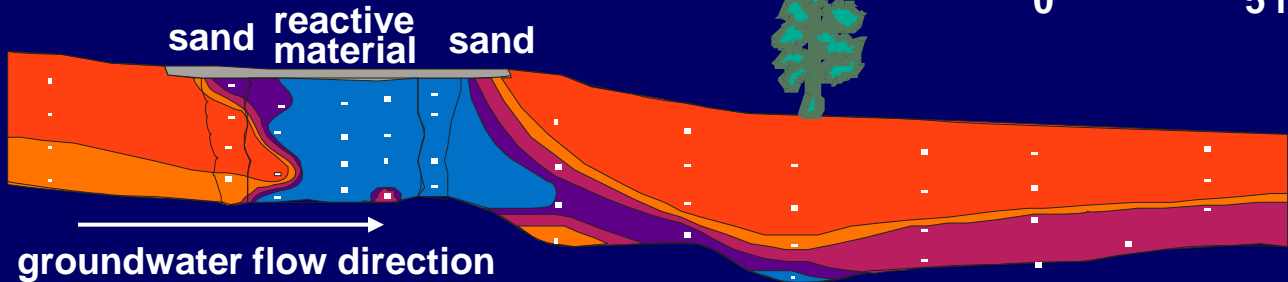


Treatment Results

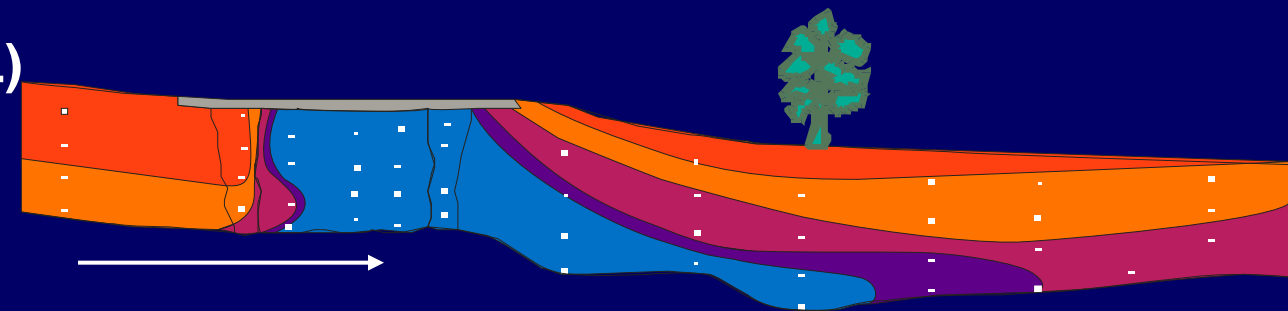
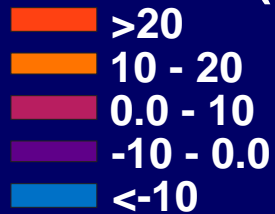
Sulfate (mg/L)



Iron (mg/L)



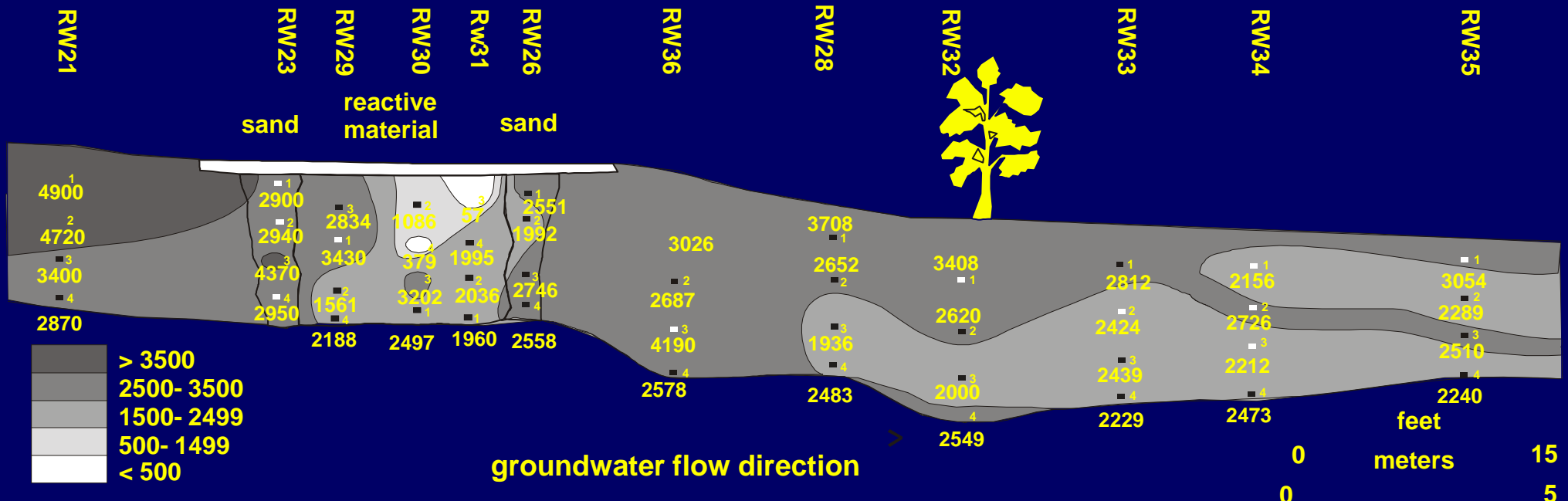
Acid Generating Potential (meq/L)



Sulfate Reduction in PRB

- Decreasing sulfate concentrations
- Sulfate-reducing bacteria
- Dissolved sulfide present
- Isotopic enrichment of ^{34}S in remnant sulfate
- Iron monosulfides identified in cores

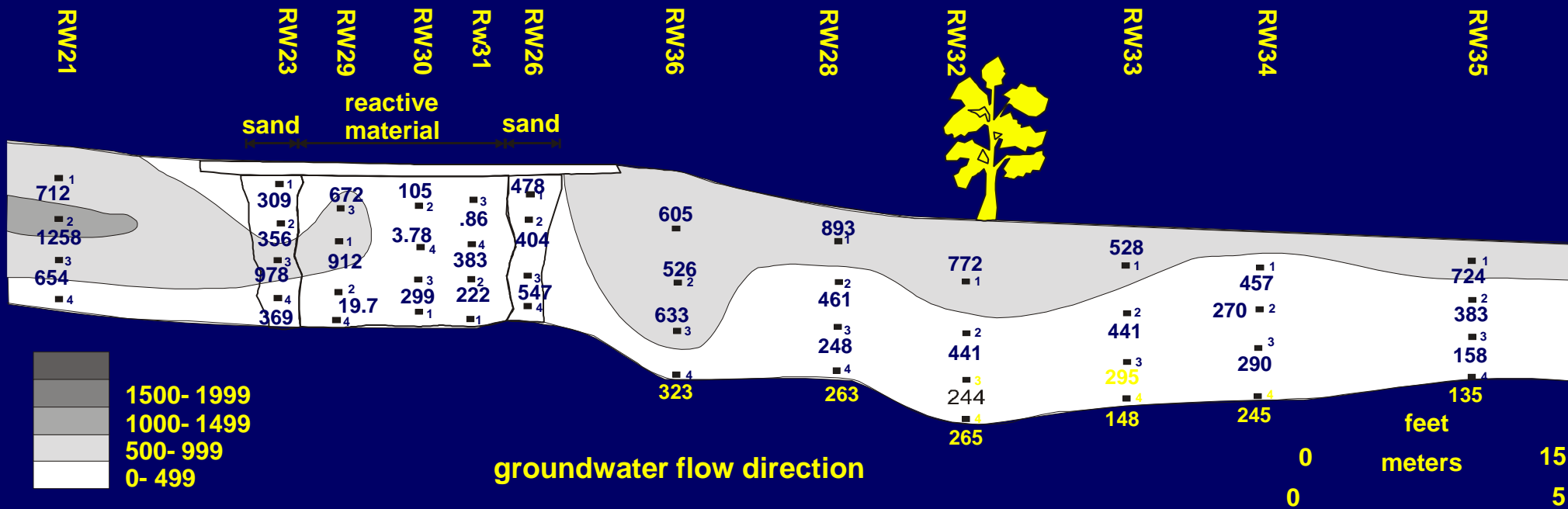
Sulfate (mg/L) August 2001



Well	Depth 1	Depth 2	Depth 3	Depth 4
RW21	4900	4720	3400	2870
RW23	2900	2940	4370	2950
RW29	2834	3430	1561	2188
RW30	1086	379	3202	2497
RW31	57	1995	2036	1960
RW26	2551	1992	2746	2558
RW36	3026	2687	4190	2578
RW28	3708	2652	1936	2483
RW32	3408	2620	2000	2549
RW33	2812	2424	2439	2229
RW34	2156	2726	2212	2473
RW35	3054	2289	2510	2240

0
5
meters

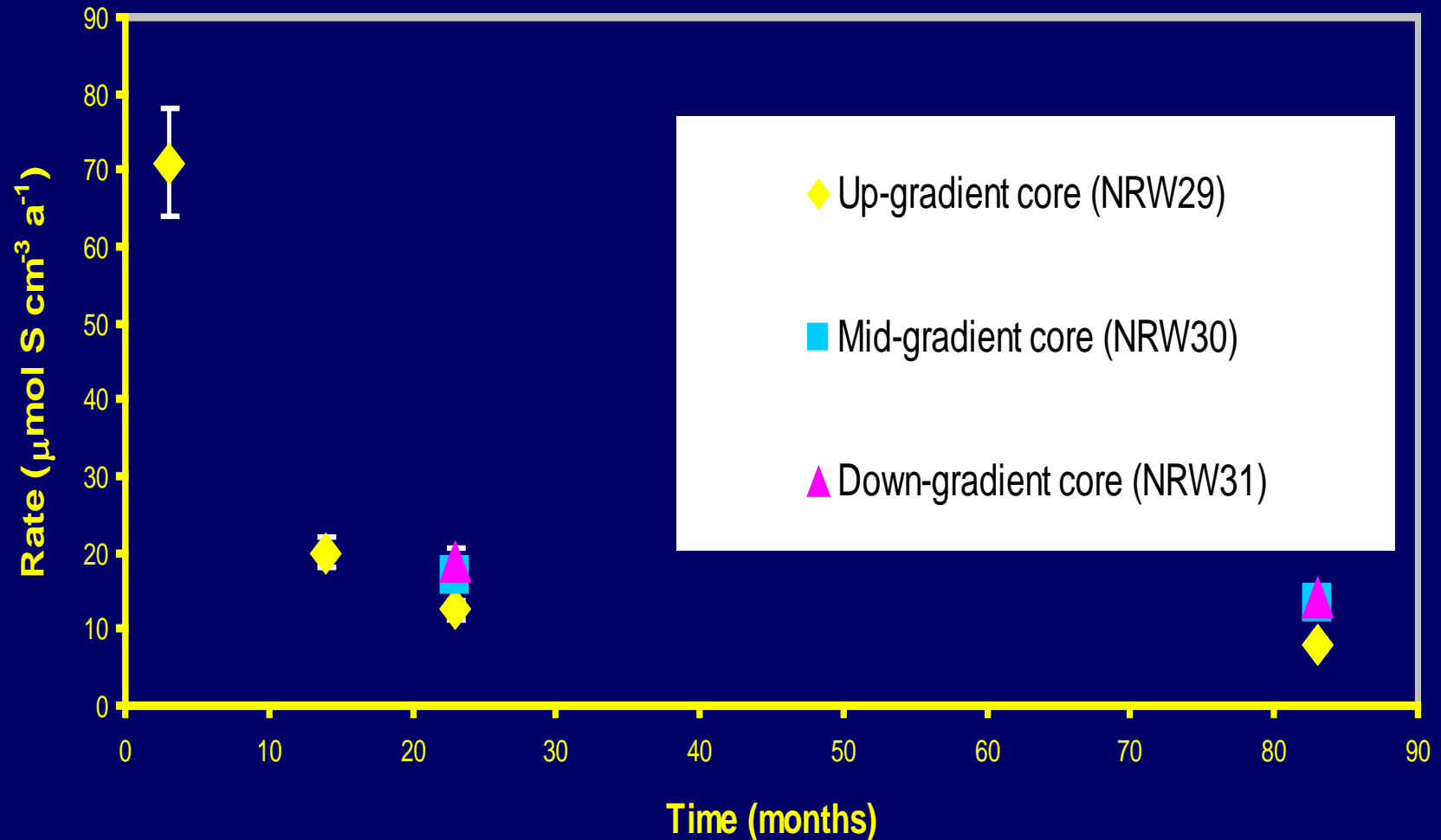
Iron (mg/L) August 2001



Well	Depth 1	Depth 2	Depth 3	Depth 4
RW21	712	1258	654	
RW23	309	356	978	369
RW29	672	912	19.7	
RW30	105	3.78	299	222
RW31	.86	383	222	
RW26	478	404	547	
RW36	605	526	633	323
RW28	893	461	248	263
RW32	772	441	244	265
RW33	528	441	295	148
RW34	457	270	290	245
RW35	724	383	158	135

0
5
meters

Sulfide Accumulation in Nickel Rim PRB (Daignault 2002, UW B.Sc.Thesis)



Summary of Nickel Rim PRB

- **The reactive wall is removing significant portion of the dissolved iron from the plume; full treatment would have required thicker PRB with longer residence time**
- **Reduced flux of contaminants in groundwater; reduced acid-generating potential of groundwater in receiving surface water**
- **Cost for materials and installation approximately \$25 K (US) in 1995**

Issues

- **Heterogeneities in PRB/ residence time of contaminated groundwater in PRB is critical to level of treatment achieved**
- **Some loss of reactivity with time; sustained availability of organic carbon**
- **Influence of temperature in shallow PRB systems**

STEEL PRODUCTION WASTES

Basic Oxygen Furnace (BOF) Slag

- **Steel production waste product**
- **Used as aggregate for construction**
- **High Ca and Fe oxides and hydroxides**
- **Interaction with water: high pH**
- **Removal of phosphate (Baker et al., 1997; 1998) and arsenic (McRae et al., 1999)**

Solid Reactive Mixtures

Aquifer Materials

Silica
Sand



Limestone

Reactive Materials



BOF-Oxide

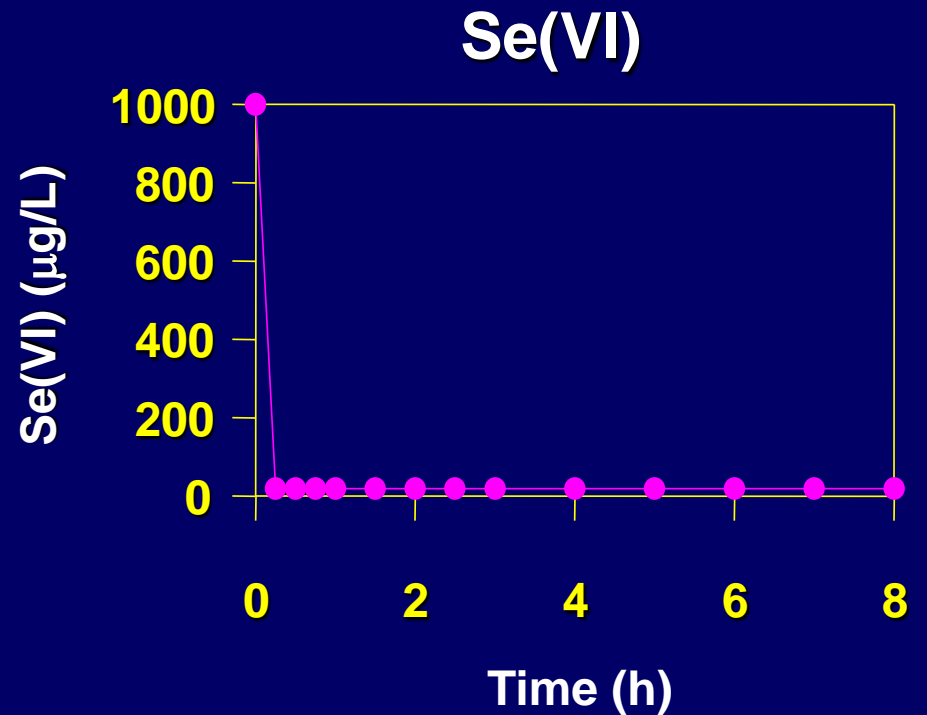
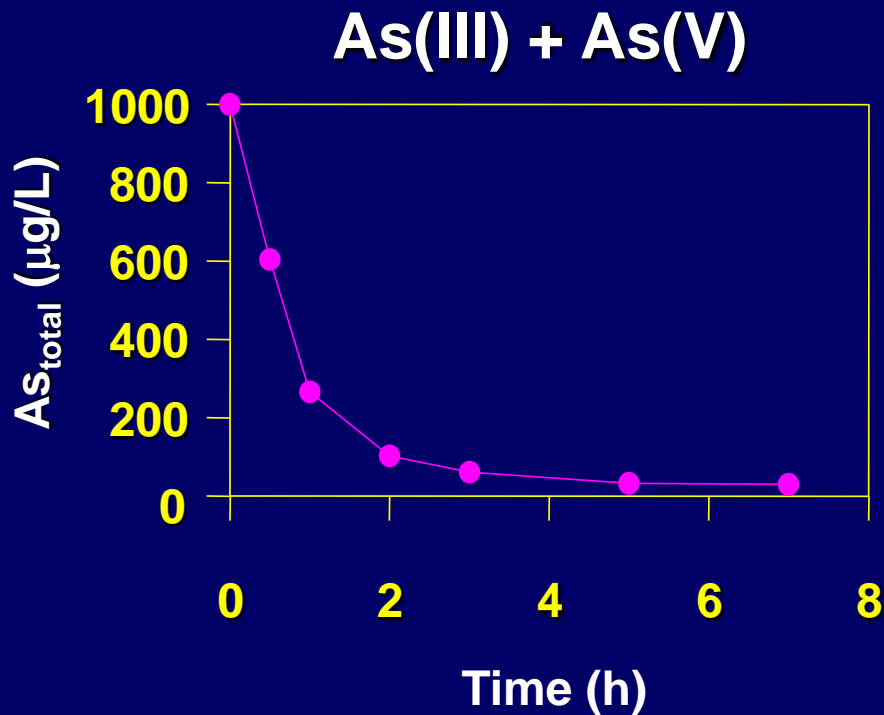


Zero Valent Iron



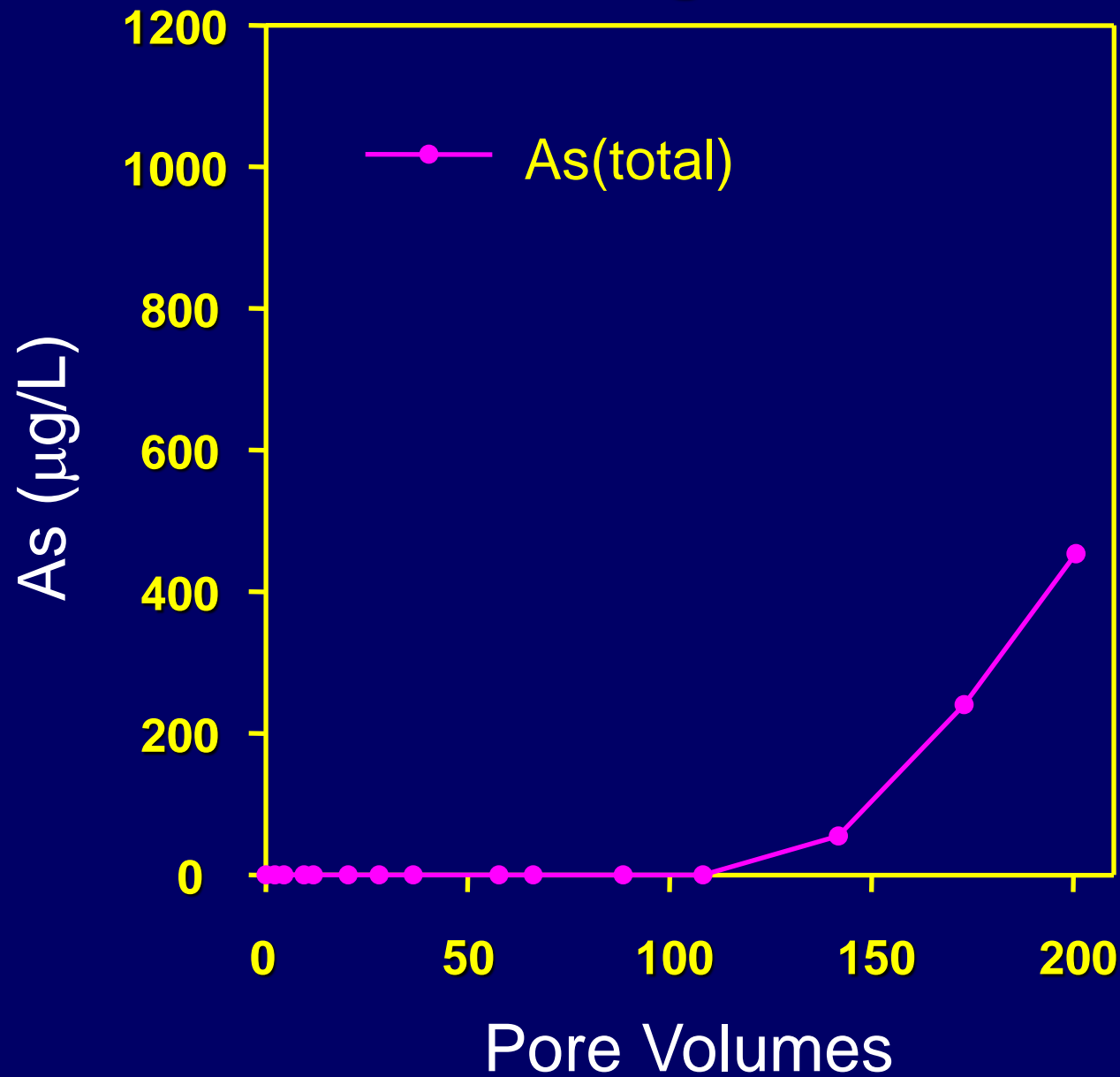
Activated
Alumina

Batch Removal Rates



Iron Slag

BOF Slag Column



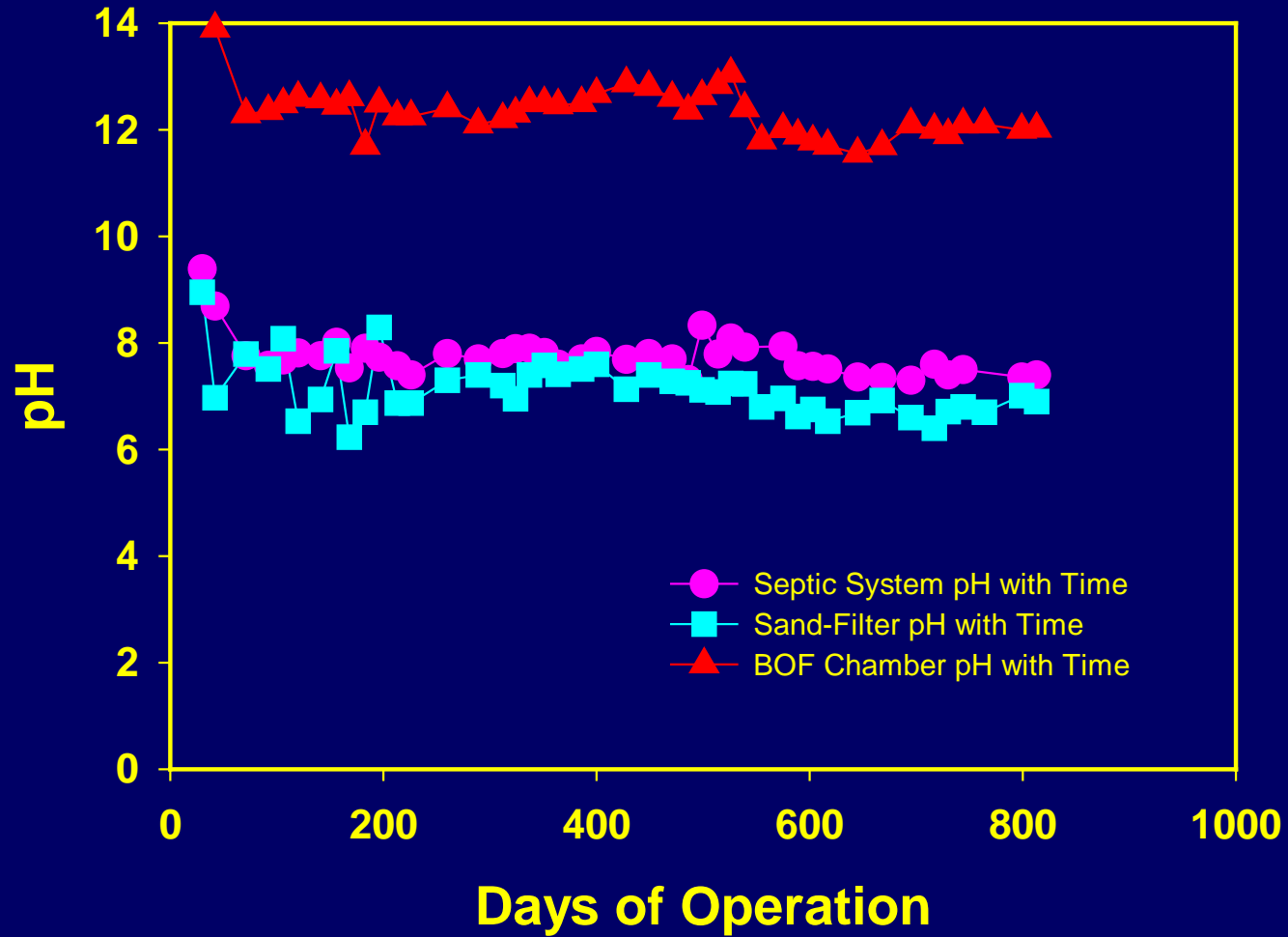
Second Column Test

- **50 % BOF slag/ 50 % gravel**
- **Low pH site groundwater with 4 mg/L arsenic**
- **More than 75 pore volumes of flow (velocity of 0.3 m/day)**
- **Total arsenic concentration in effluent less than 0.01 mg/L**

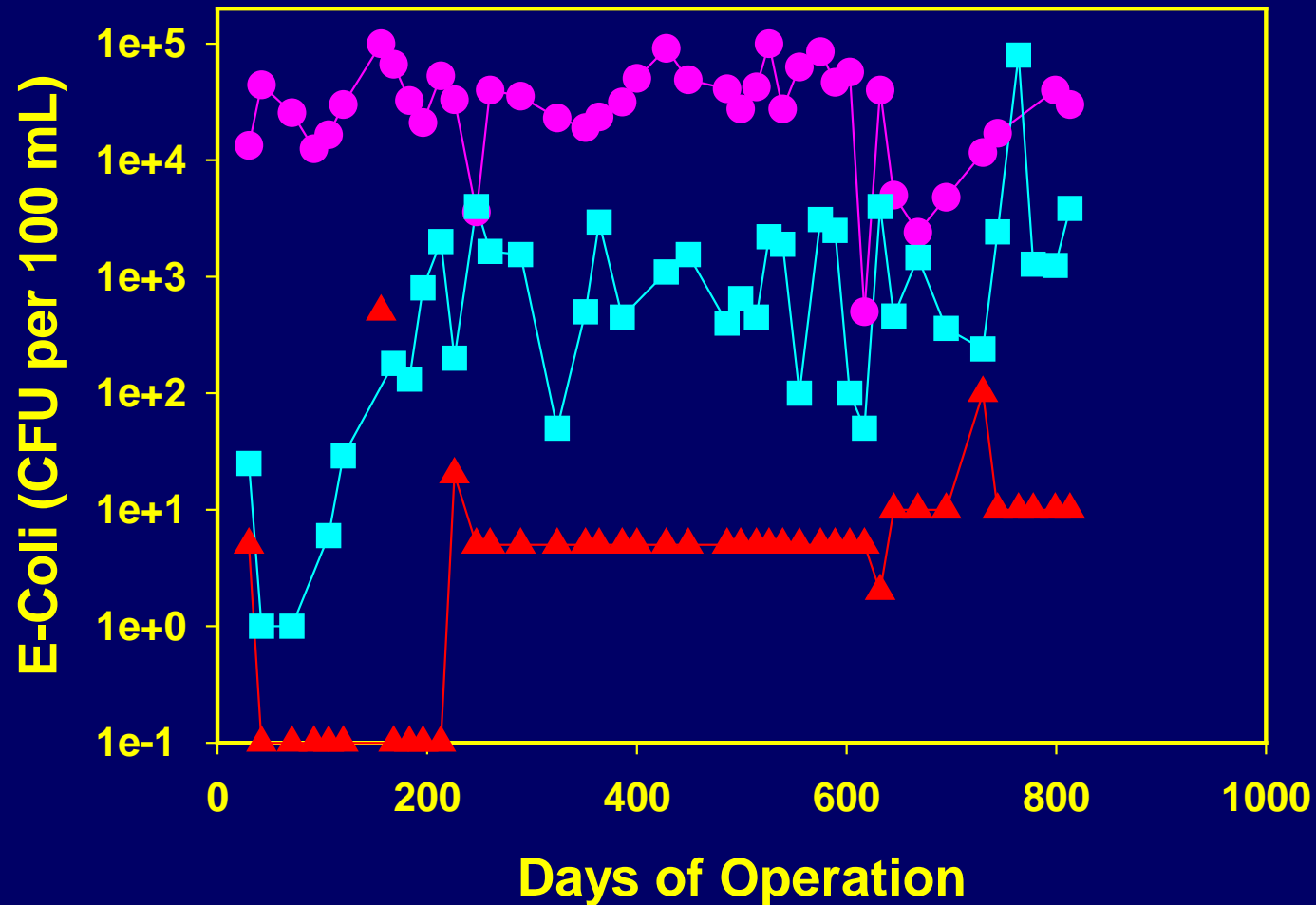
Arsenic Removal by BOF Slag

- **Removal of arsenic oxyanions by sorption iron and manganese oxyhydroxides in BOF**
- **Removal to low levels (<0.005 mg/L total arsenic)**
- **Sustained performance for 100 pore volumes of 10 % BOF mixture**

North Bay System: pH with Time



North Bay System: E-Coli with Time



- E-Coli in Raw Water
- E-Coli in Sand Filter
- ▲— E-Coli in BOF Filter

BOF-Chamber Performance

- **Effective removal of phosphorus**
- **Effective removal of E-Coli**
 - **Elevated pH provides environment that eliminates bacteria**
- **Elevated pH of 12 or higher**
 - **Elevated pH is buffered by soils and sediments upon release to subsurface**
 - **pH of groundwater approximately 1 m down-gradient of discharge gallery was 6.2 to 7 (August 2000)**

Zero-Valent Iron and Other Reactive Materials

- **Excellent removal of electroactive metals**
- **Sulfate reduction and AMD treatment**
- **Excellent treatment of nutrients**
- **Performance of field-scale applications**
- **Removal mechanisms**
- **Reactive capacity**
- **Formation of secondary precipitates**