

High Altitude Mine Site Wetland Demonstration Constructed Wetlands Treatment

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Background



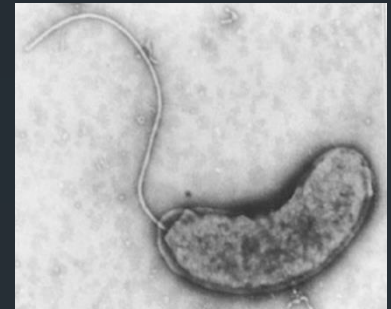
- Development of water treatment system required by EPA
- Safety and logistical concerns were drivers to investigate feasibility of constructed wetland system
 - Extreme winter weather
 - Avalanche hazards
 - Limited local population base
- Regulatory support for wetlands/passive treatment
 - Keen interest by EPA, state and local groups
 - Resurgence in acceptability as viable technology
 - Need viable passive treatment alternatives at numerous orphan sites

SRB Biotreatment Overview

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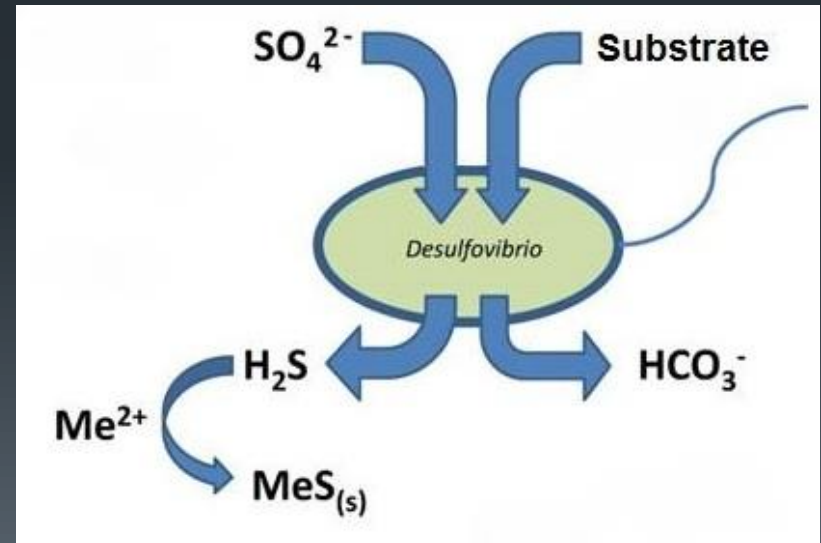
Microorganisms need three things:

- Energy Source (e^- donor) – Organics / Carbon
- Favorable environment - Anaerobic
- Nutrients and e^- acceptors – Sulfate and Micronutrients



Sulfate Reduction Process

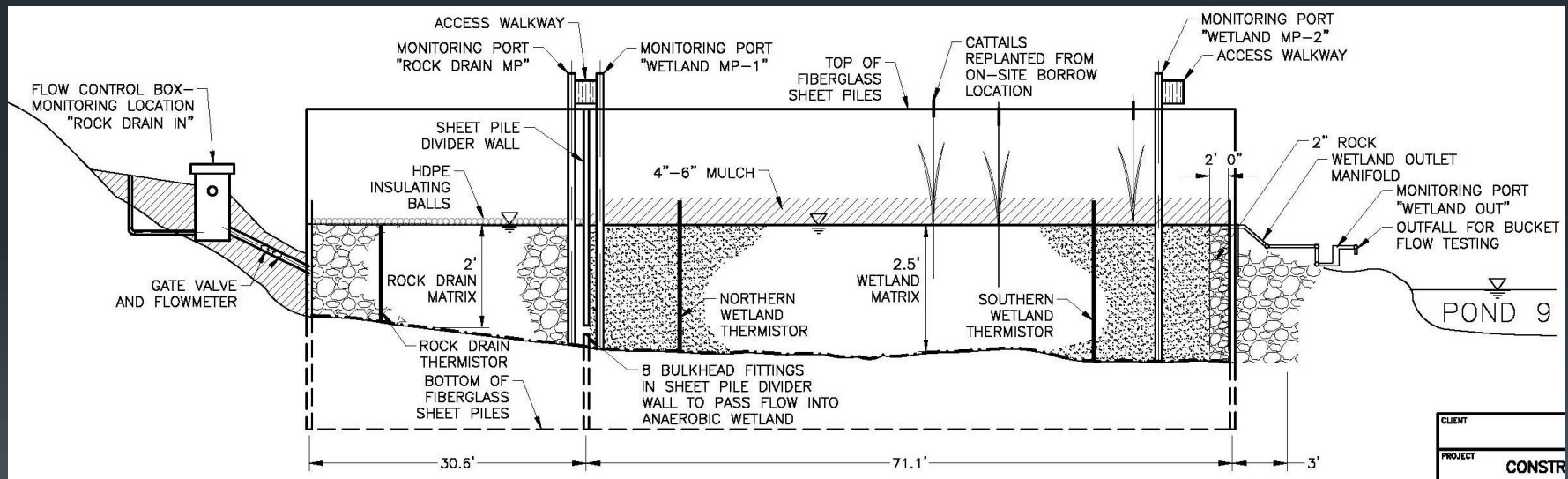
- Organics yield carbon and energy
- Sulfate (SO_4^{2-}) reduced to sulfide
- Metals bind with sulfide (MeS)
- Generates Bicarbonate (HCO_3^-)



Pilot System

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- Feasibility testing initiated in 2012
 - 12 liter per minute (lpm) system
 - Aerobic rock drain followed by horizontal-flow anaerobic wetland
 - Operated December 2012-August 2014 with favorable results



AMEC, 2012

Wetland Demonstration Systems ⁵

- 2014 - Two parallel 115 lpm demonstration-scale systems constructed
 - Horizontal wetland treatment train (HWTT)
 - Vertical wetland treatment train (VWTT)
- 2015 – Enhanced Wetland demonstration (EWD)
 - Scaled-up to 2,100 lpm
 - Largely based on VWTT, plus Mn removal step after settling basin similar to pilot wetland rock drain

VWTTT Overview

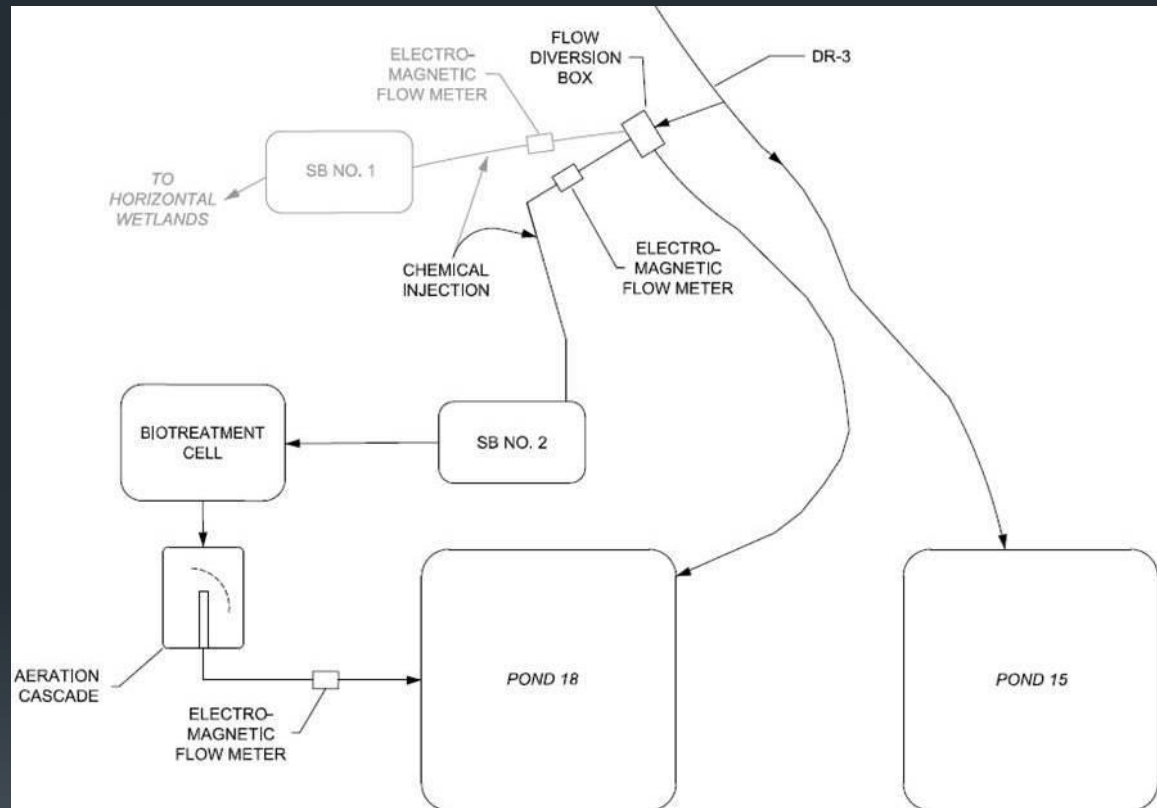
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■ Components

- Coagulant addition (aluminum chlorohydrate)
- Settling Basin (SB2)
- SRB Biotreatment Cell (Biocell)
- Aeration Cascade

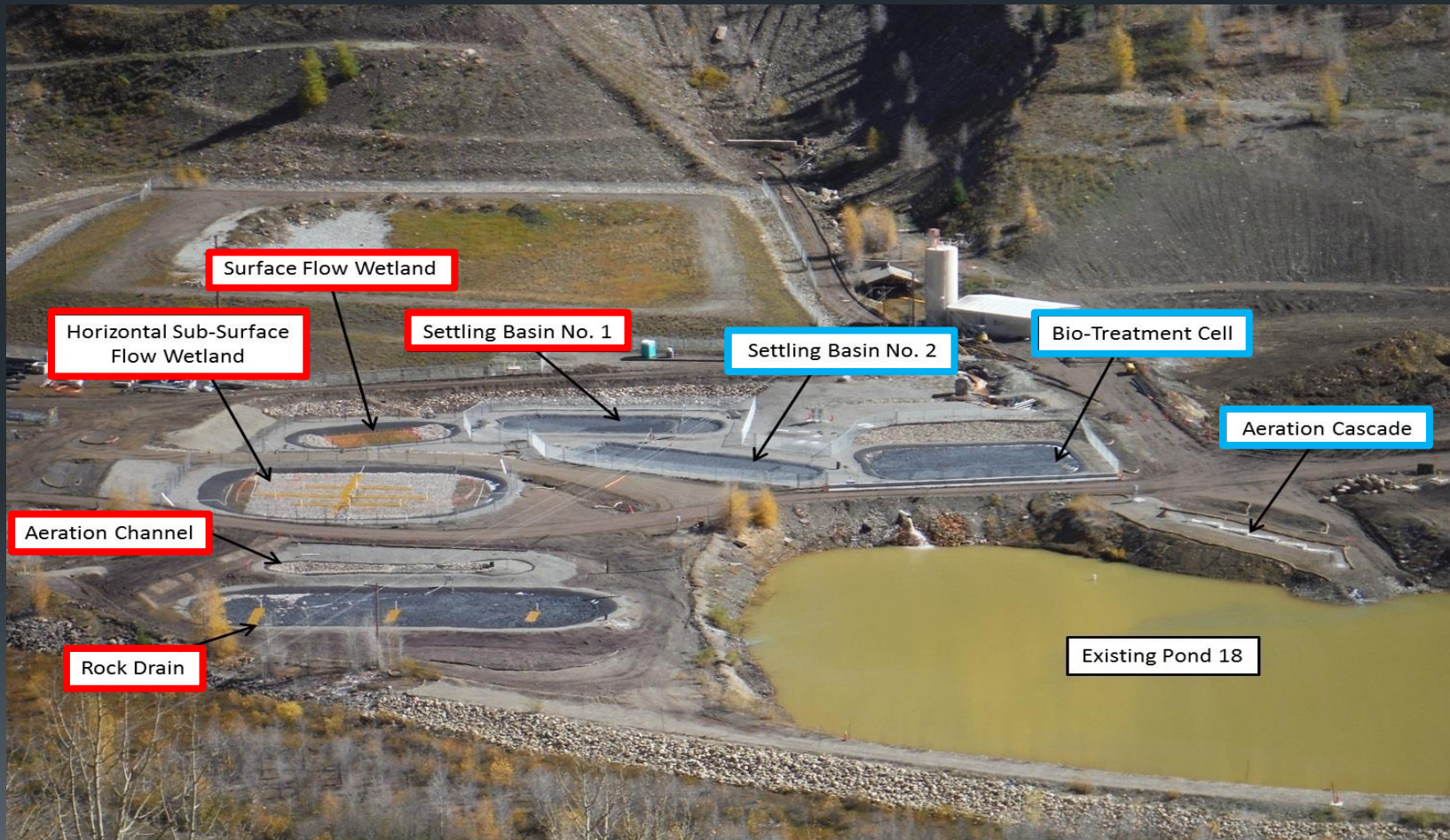
■ Metals of Concern

- Cd
- Cu
- Fe
- Mn
- Zn



Wetland Demonstration Systems ⁷

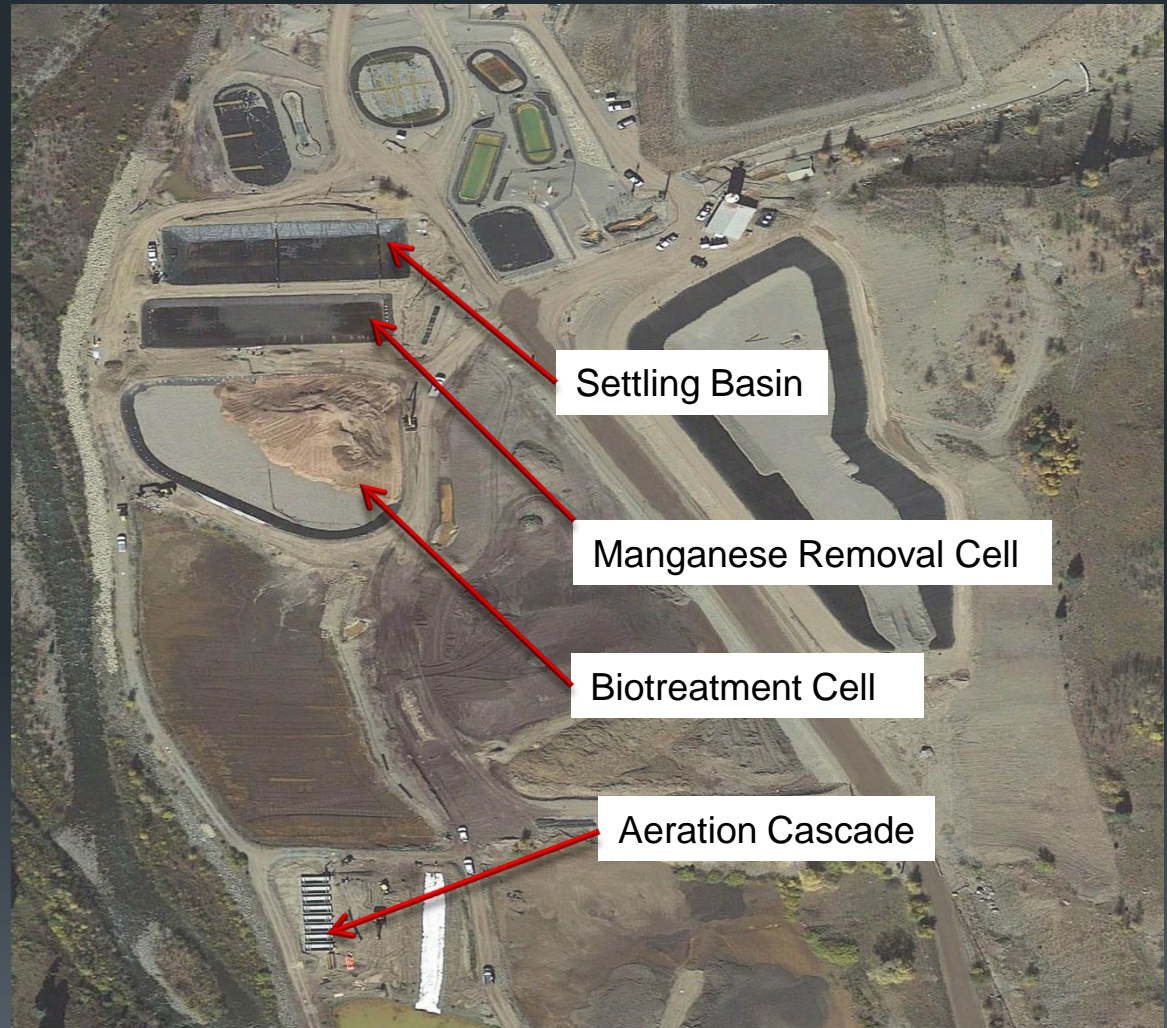
VWTT (blue) and HWTT (red) Overview



Wetland Demonstration Systems ⁸

EWD overview

- EWD treatment performance consistent with VVTT treatment performance

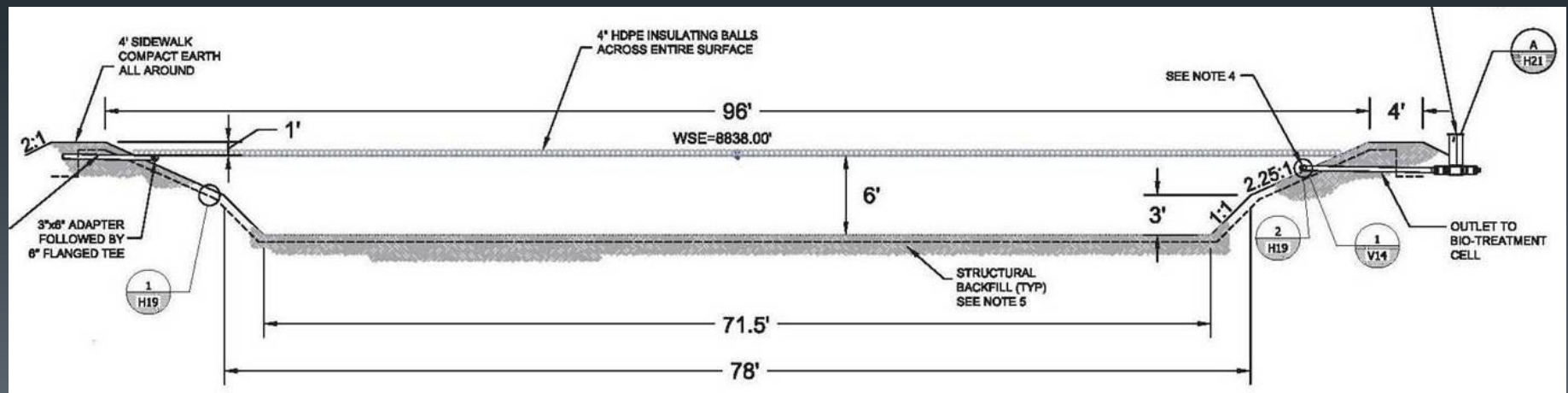
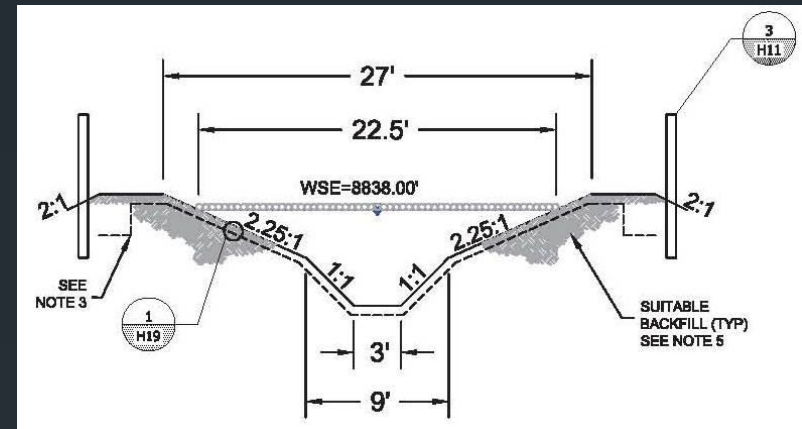


VWTT Overview

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■ Settling Basin No. 2

- Al, Cu, Fe, Pb and TSS Removal
- Volume: 140 m³
- Area: 191 m²
- Depth: 1.8 m
- HRT: 20.5 hrs



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Diagram illustrating the cross-section of a wastewater treatment cell, showing the inlet, treatment area, and outlet.

Key Components and Dimensions:

- Inlet:** Inlet from settling basin, 1.75' high, with 2:1 slopes. Inlet structure is 1.5-inch washed angular limestone (see Note 8).
- Treatment Area:**
 - Top Layer:** 4" HDPE insulating balls across entire surface.
 - Bottom Layer:** 3" perforated SCH 40 PVC piping array.
 - Structural Backfill:** (TYP) 1' thick.
 - Water Surface Elevation (WSE):** 8837.50'.
 - Dimensions:** 72' total length, 5' distance from inlet to start of treatment area, 48' distance from end of treatment area to outlet.
- Outlet:** Outlet to aeration cascade, with 2:1 slopes.
- Notes:**
 - BIOTREATMENT CELL INFLUENT/EFFLUENT ACCOMPLISHED THROUGH HEADER CONNECTED TO 3" PERFORATED PVC PLACED AT 8' CENTERS ACROSS TOP AND BOTTOM.
 - 3 V14, 2 H19, 1 H19, 2 V14 (likely valve or vent identifiers).

VWTTT Overview

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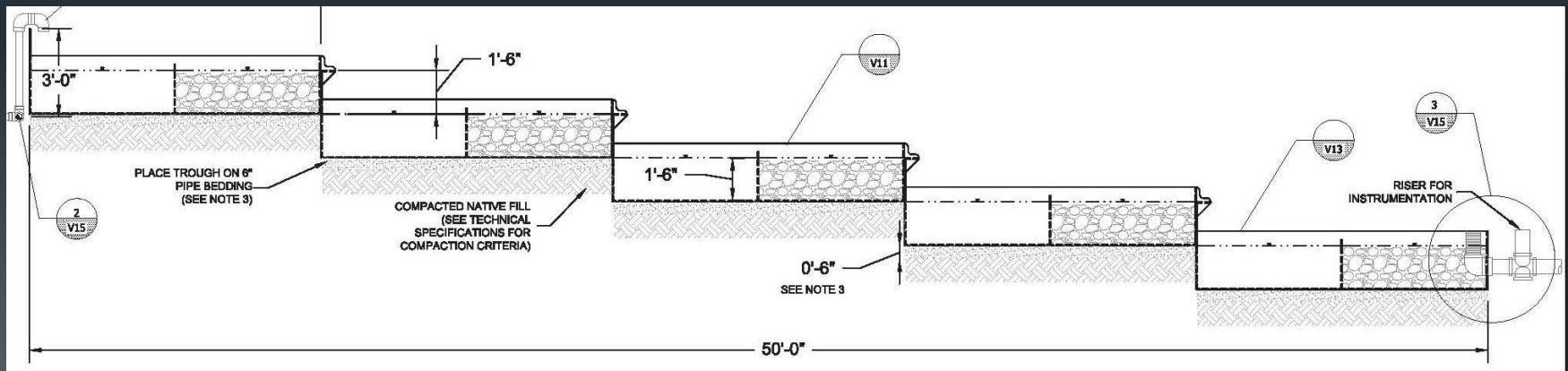
- Settling Basin and Biotreatment Cell Outlet Control
 - Agridrain™ Inline Water Level Control Structure
 - “Weir in a box”



VWTT Overview

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- Aeration Cascade
 - Sulfide and BOD Removal, Restore DO
 - 5 sequential drop troughs
 - Trough Length: 3 m
 - Trough Width: 0.6 m
 - Trough Depth: 0.6 m
 - Inter-trough drop height: 0.45 m
 - HRT: 28 min



VWTTT Overview

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■ Hydraulic Conductivity

- Hydraulic gradeline calculations indicate minimum required K of $\sim 10^{-3}$ cm/s
- Column test substrate falling head test results were $\sim 10^{-1}$ cm/s
- Hydraulic head can be manipulated via Agridrain weir slats, allows accommodation of K changes

■ Minimal Instrumentation

- Water entering upstream side of Agridrain is representative of conditions in bottom of cell
- Low short circuiting/preferential flow potential due to short flow path

■ Temperature/Freezing

- Minimal heat loss through SB No. 2 and Biocell using HDPE insulating balls
- REMC has successfully operated biotreatment cells at water temperatures below 4° C

VWTTT Overview

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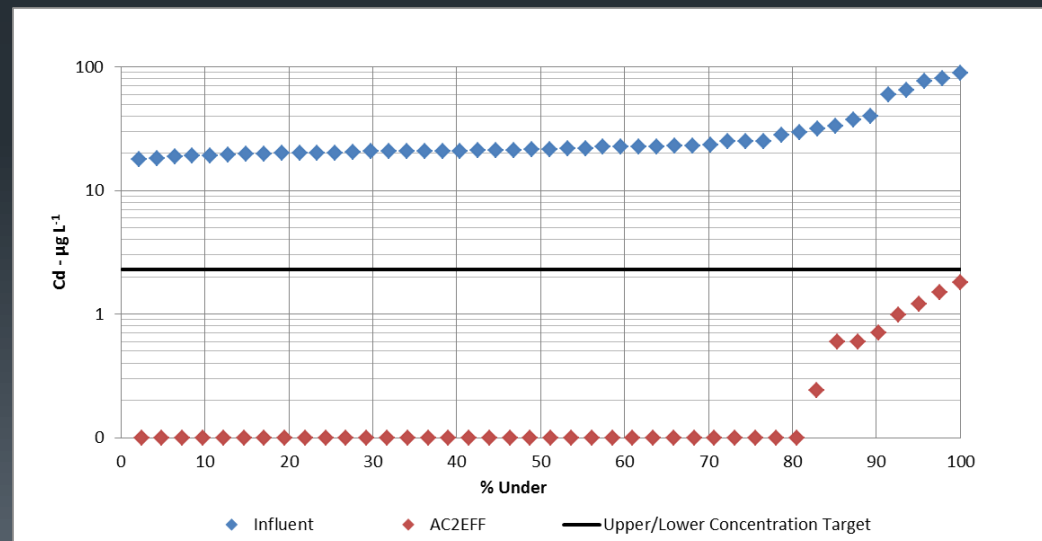
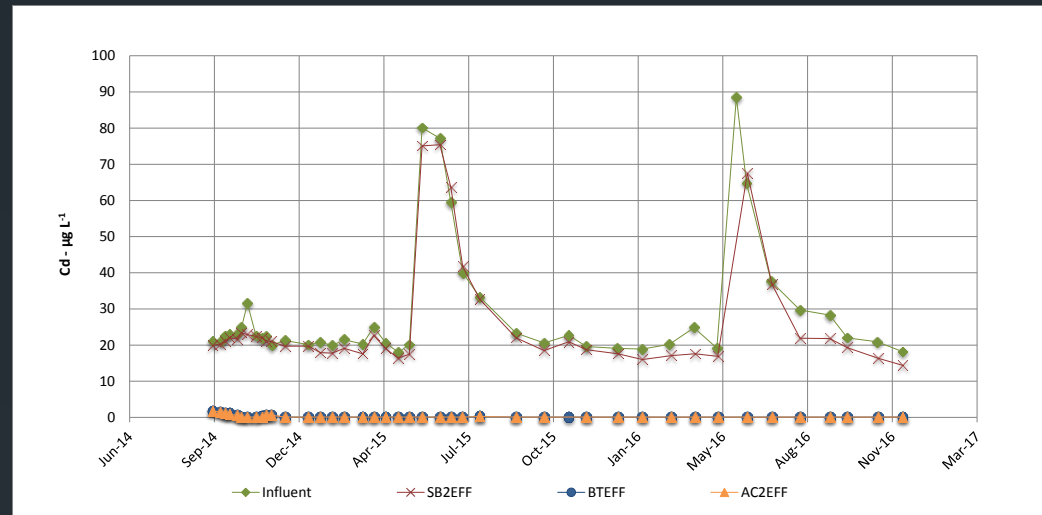


VWTT Results

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■ Total Cadmium

- Influent average: 22 $\mu\text{g/L}$
- Influent max: 88 $\mu\text{g/L}$
- 100% of effluent samples below concentration target
- Avg. removal efficiency: >99%
- Includes start-up period data
- All effluent results non-detect (<0.5 $\mu\text{g/L}$) since December 2014

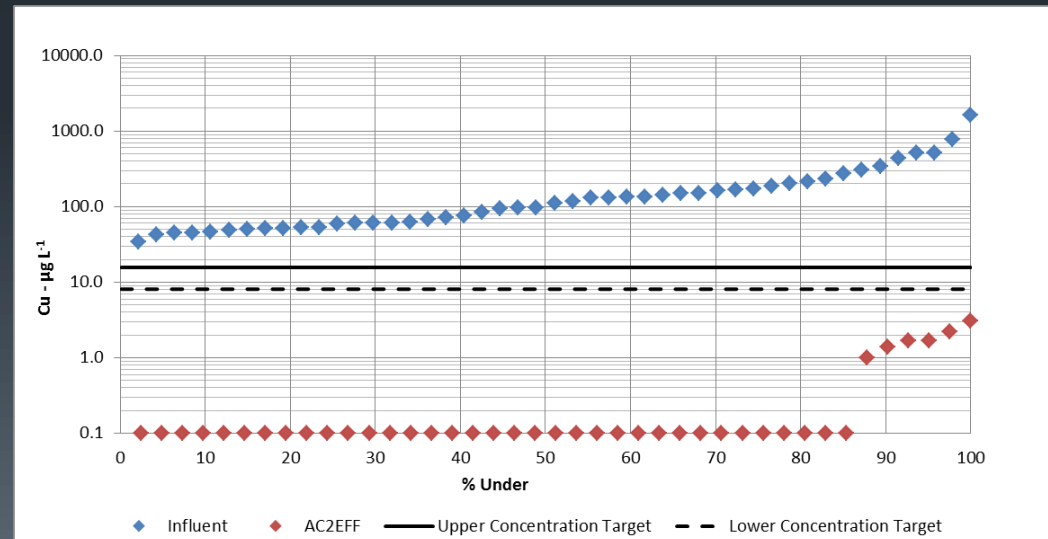
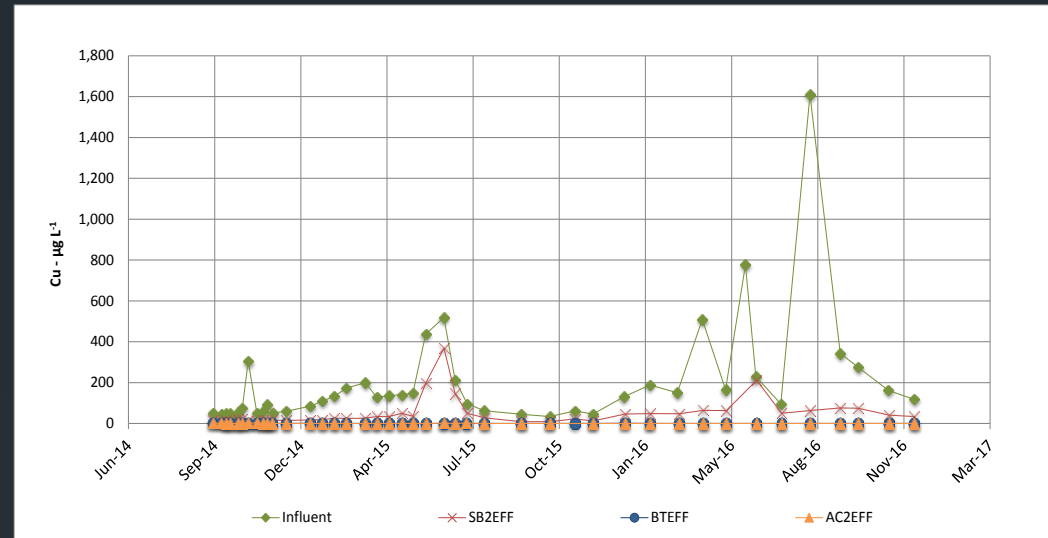


VWTT Results

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■ Total Copper

- Influent average: 133 $\mu\text{g/L}$
- Influent max: 1,610 $\mu\text{g/L}$
- 100% of effluent samples below all concentration targets
- Avg. removal efficiency: >99%
- Majority of load is particulate removed in SB2, possibly sorbed to Fe
- Most results non-detect

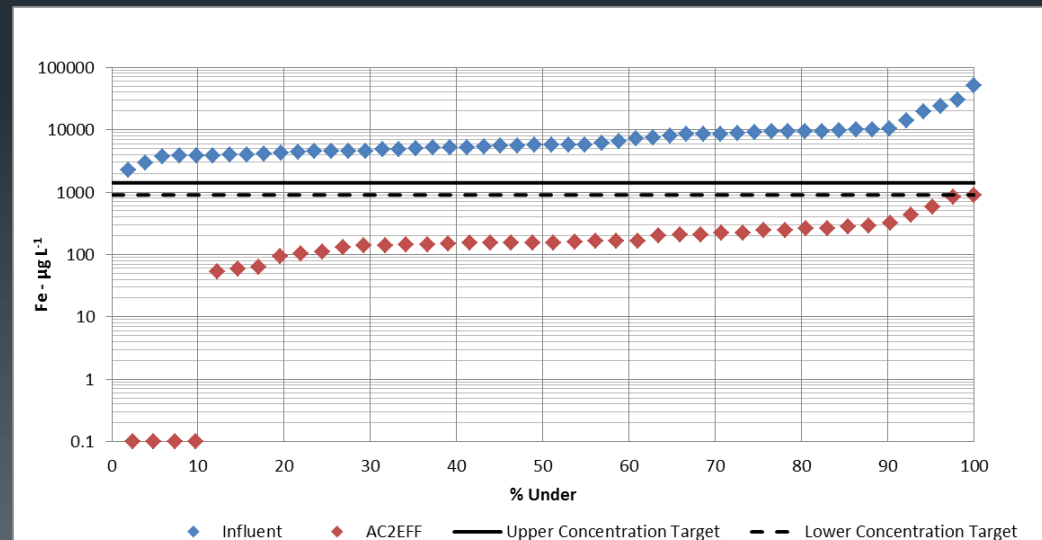
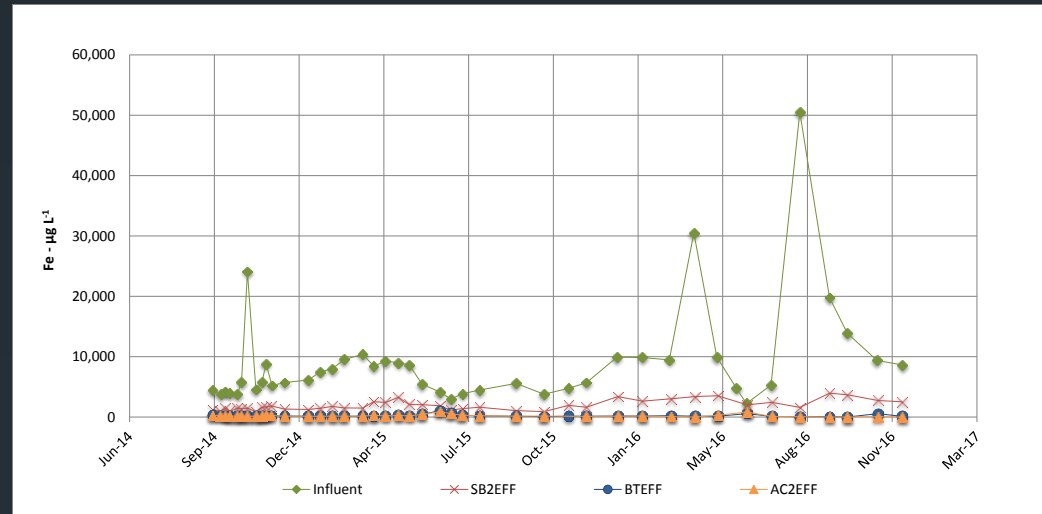


VWTT Results

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■ Total Iron

- Influent average: 9,400 $\mu\text{g/L}$
- Influent max: 30,500 $\mu\text{g/L}$
- 98% of effluent samples below lower concentration target
- Avg. removal efficiency: 98%
- SB2 effluent average: 1,800 $\mu\text{g/L}$
 - Insufficient iron removal to prevent solids loading to Biocell matrix
- <500 $\mu\text{g/L}$ is ideal
- Residual iron primarily fine colloids, some dissolved Fe(II)

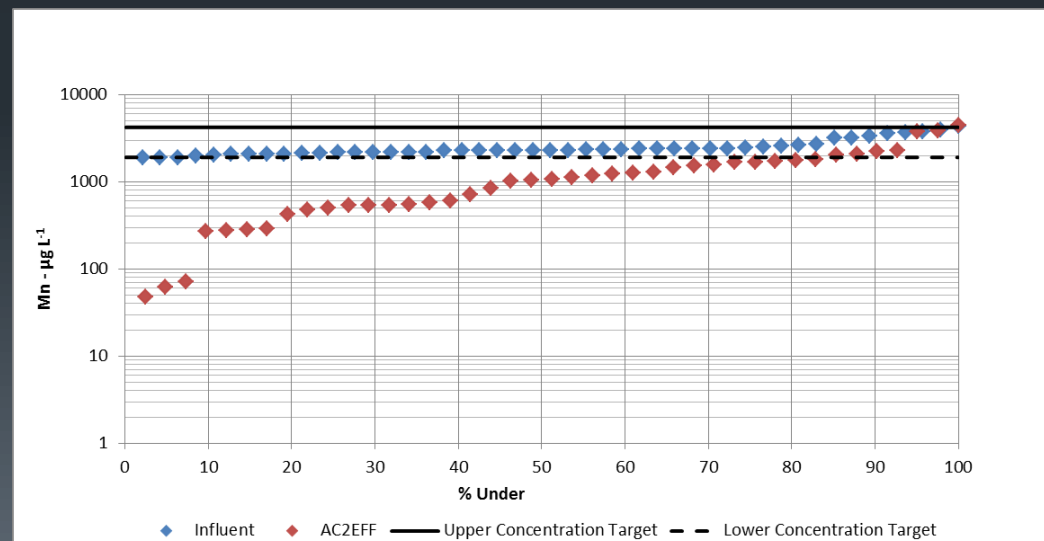
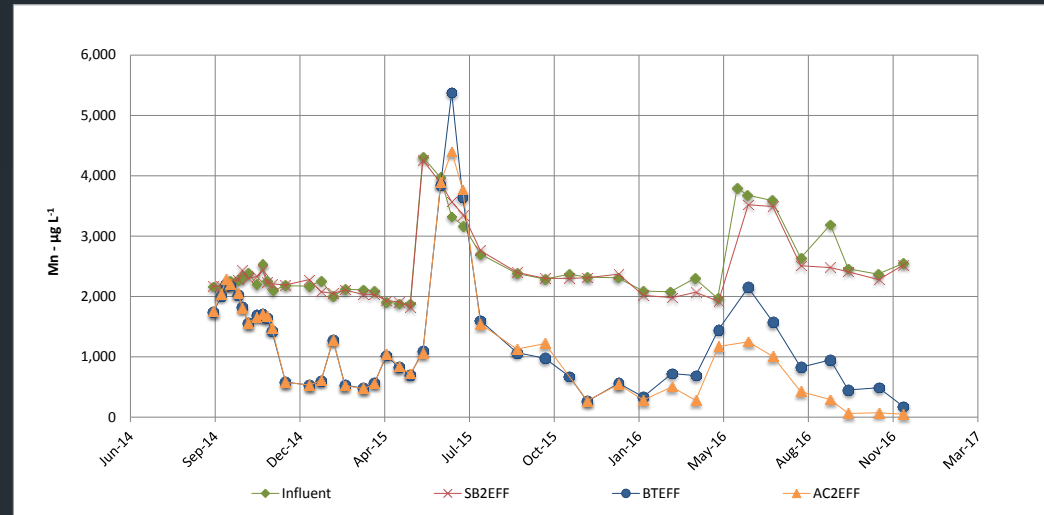


VWTT Results

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■ Total Manganese

- Influent average: 2,300 $\mu\text{g/L}$
- Influent max: 4,310 $\mu\text{g/L}$
- 83% of effluent samples below lower concentration target
- Avg. removal efficiency: 54%
- Mn removal not a design goal of the VWTT
 - Unexpected in anaerobic cell
 - September 2017 sampling indicates oxic removal in upper 15 cm of organic matrix
- Additional Mn removal occurring in aeration cascade
 - Last 3 troughs
 - Rapid removal (minutes)
- Ongoing investigation of Mn removal mechanisms

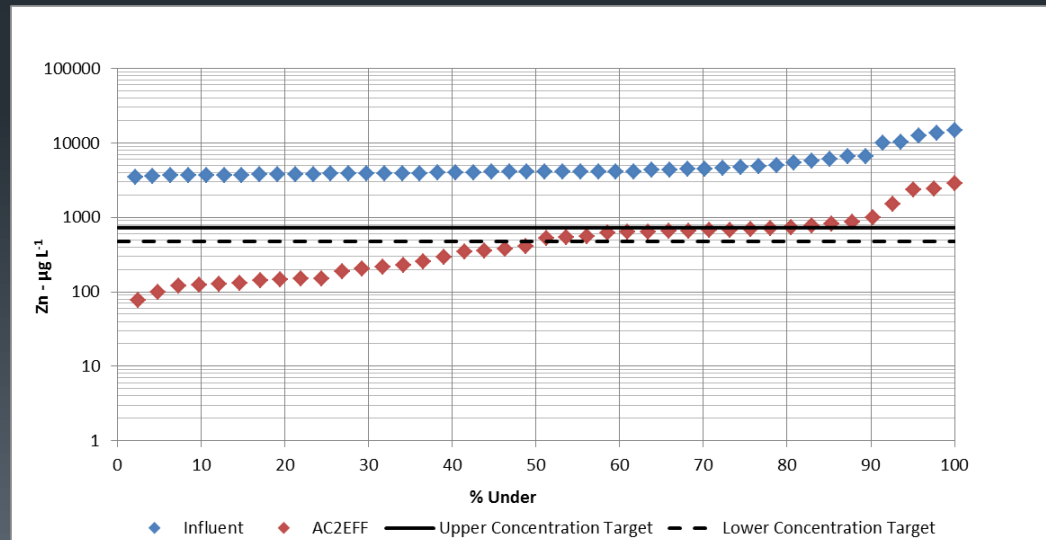
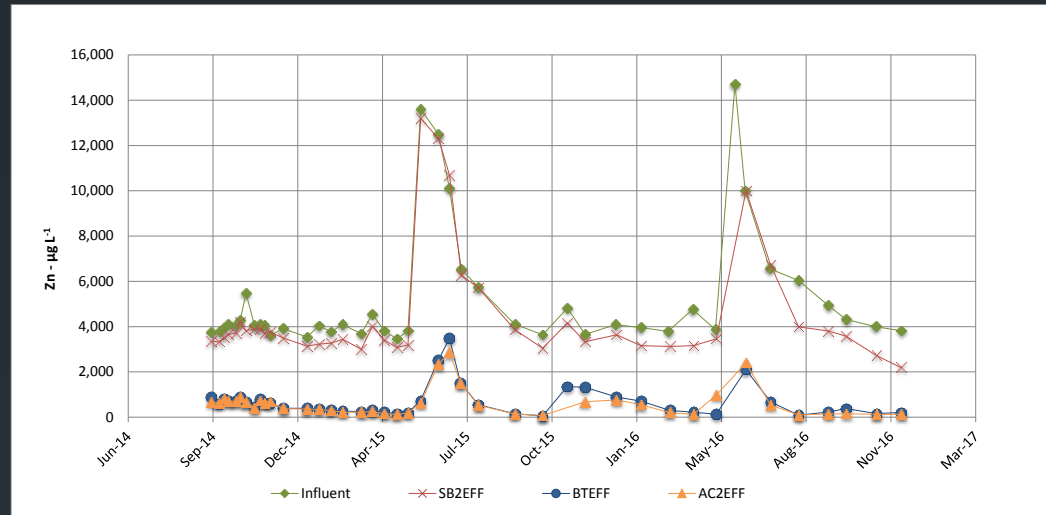


VWTT Results

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■ Total Zinc

- Influent average: 4,100 $\mu\text{g/L}$
- Influent max: 14,700 $\mu\text{g/L}$
- 49% of effluent samples below lower concentration target
- 90% of effluent samples below 1,000 $\mu\text{g/L}$
- Avg. removal efficiency: 89%
- Includes start-up period data
- Removal is seasonally variable
 - >90% during majority of year
 - 65-80% during freshet peak
- Baseflow effluent concentrations are typically 100-300 $\mu\text{g/L}$
- Peak freshet effluent concentrations 1,000-3,000 $\mu\text{g/L}$, but decreasing in magnitude each year

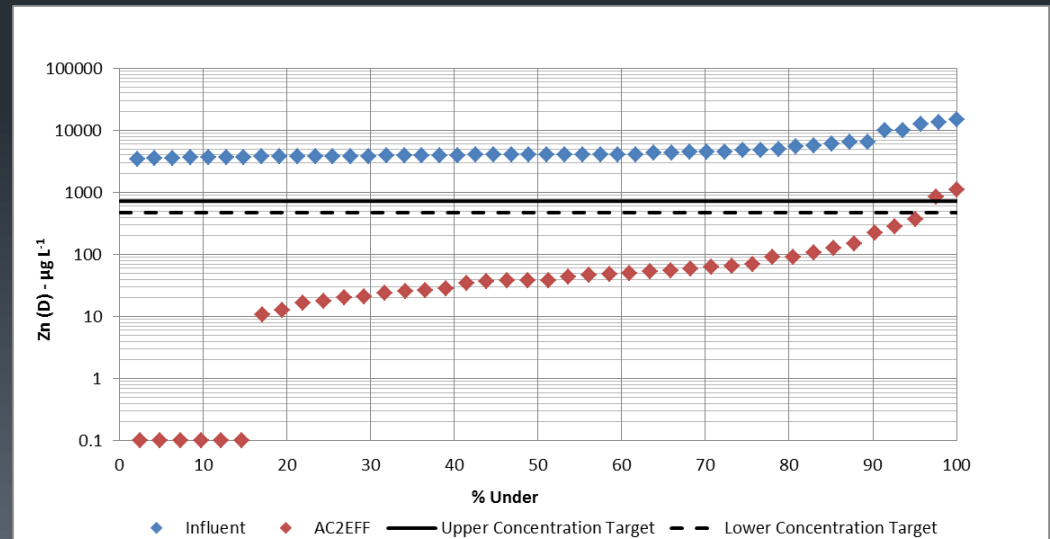
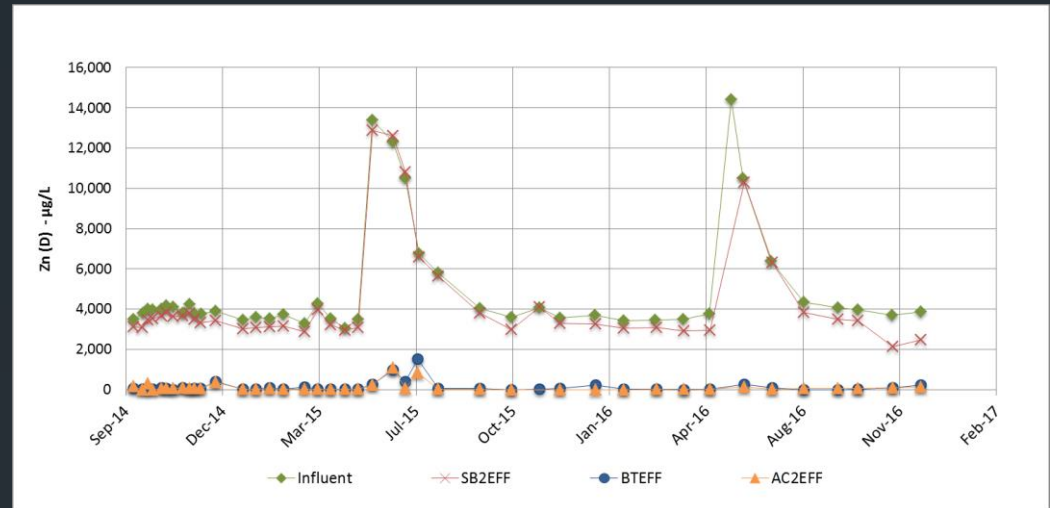


VWTT Results

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■ Dissolved Zinc

- Zinc removal appears limited by matrix capacity to filter precipitated ZnS colloids
- 95% of effluent samples below lower concentration target
- Avg. dissolved Zn removal efficiency: 98%

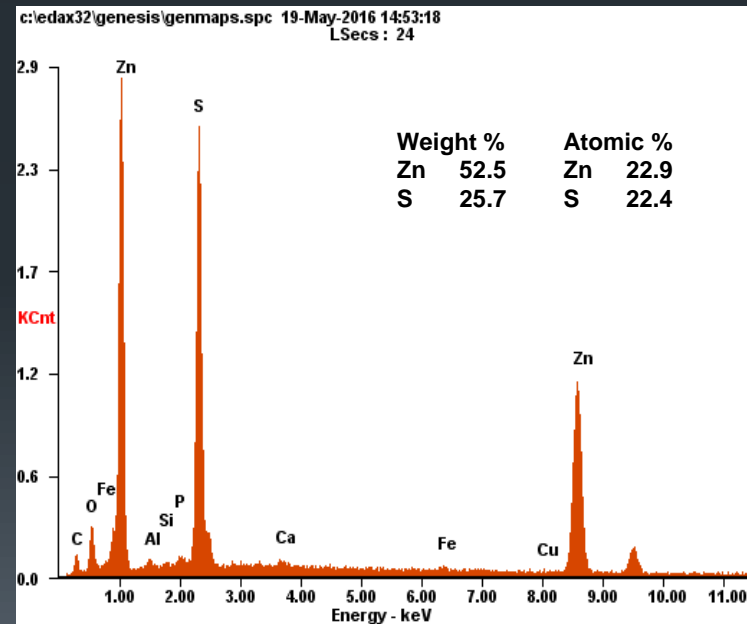
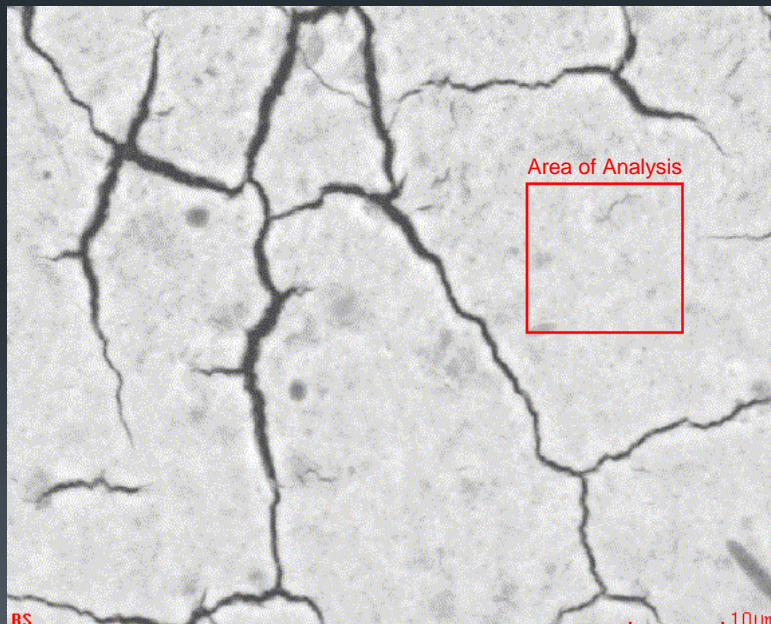


VWTT Results

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■ Total Zinc

- SEM micrograph of Biocell effluent filter residue shows nearly pure ZnS
- Lack of visible particles in SEM image indicates sub micron-sized ZnS particles in filter residue



Design Challenges

- High elevation location

- 2,700 m above sea level
- Maximum length of construction season is June 1-Nov 1
- Snow depths can exceed 2 m
- Multiple avalanche paths terminate at site
- Winter temperatures commonly reach -30° C
 - Mine water temperatures are above normal from geothermal influence (19° C)
 - Insulating balls used to minimize heat loss

- Siting

- Site is large (12 hectares), but most areas unsuitable for construction of treatment units
- Near-surface groundwater is common
- Limited hydraulic head available for gravity flow

Treatment Challenges

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Iron/solids loading

- Influent solids load highly resistant to gravity settling
- Particle size analysis consistently shows that ~90% of particles are <1 micron
- SEM analysis of filter residue indicates presence of significant quantity of clay minerals.
- Avg. 2 mg/L iron in SB2 effluent. Filtered by Biocell matrix surface which impacts hydraulic conductivity.
- Removal of iron sludge from Biocell surface required in 2017
- Improving solids removal is current design focus.

Treatment Challenges

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Freshet

- Annual drop in pH and increase in metals loading during spring runoff
- Influent pH drops by 1 s.u. on average
- Influent metals concentrations increase 2-5x
- Negatively impacts removal of iron, manganese and zinc
- Iron
 - Total iron load shifts toward dissolved phase
 - Iron oxidation rate slows at lower pH
 - Reduces effectiveness of coagulant
- Zinc
 - Breakthrough of total Zn in Biocell effluent
 - Biocell effluent dissolved Zn concentrations remain low
 - May be due to simple overload of filtering capacity, or change in ZnS particle size
- Manganese
 - Mechanism unknown, but Mn(II) oxidation well known to be pH-dependent

Questions?

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