Managing Acid Generation and Metal Leaching in High Sulphide Thickened Tailings During Operation: Lessons Learned at Xstrata's Kidd Metsite

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Gilles – The Se/Mo Review -- It's Done



A REVIEW OF ENVIRONMENTAL MANAGEMENT CRITERIA FOR SELENIUM AND MOLYBDENUM

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Kidd Metallurgical Site

- Three mines: Kidd upper mine, Kidd mine D, and Montcalm mine.
- Produces zinc and copper from Kidd mines and Nickel from Montcalm.
- Produces 2 3 Mt tailings per year
- Thickened tailings (65% solid) are mixed and deposited with other effluent streams in the tailings management area (TMA)
- Original TMA occupied about 1,200 ha
- Tailings contain Pyrite / Pyrrhotite (6% S)
- NP/AP < 1 Therefore acid generator when disposed on land



THICKENED TAILINGS

- What is "THICKENED" tailings?
 - Higher Density / % Solids produced in Thickener
 - Greater viscosity
 - Faster Settling
 - No or Little Segregation of Grain Sizes in Impoundment when Discharged



WHY THICKENED TAILINGS

- No need for Dams only berms to contain solids
- No classic "Beaches" and "Slimes"



Kidd TMA 2005















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Lesson 1 – Efficient at Shedding Water – Results in High Runoff





Annual Lime Use and Flows





Monthly Lime Use

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Daily Lime Use





Lesson 2 – Efficient Acid Generator with High Daily Lime Demands





Acid Generation Studies

- Early 1990's -
 - David Blowes and Tom AI (U of Waterloo)
 - Pore waters / above and below water table
 - Noranda Technology Centre (NTC) Surface Hydrology / Cover test plots
- Mid 1990's 2000's
 - Beak International
 - Modelling
 - oxygen consumption measurements
 - soluble extractions for regular monitoring



Acid Generation Studies

- Mid 2000's
 - EcoMetrix
 - Jarosite studies NP Consumption
 - Lime demand modelling / optimization



Spatial Trends of Dissolved Sulphate, Iron and Zinc in Pore Water



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Tailings Pore Water Variation from Drained to Wet Areas





Acidity and Metal Loads from Shallow Pore Water Flushing





Lag Time for Acid Generation

- Fresh tailings are neutral with reasonable Neutralization Potential (NP) values
- Sulphide Oxidation generates acid and consumes NP
- High acidity and metal loads only after NP depleted
- Lag time between start of oxidation and NP depletion is critical and depends on:
 - Oxidation rates
 - Available NP



Oxygen Consumption Measurements In-Situ / Real-Time Rates



Spatial Trends of Oxygen Consumption Rates



EcoMetrix

Carbonate Content (NP) and Pore Water pH As a Function of Depth





Lesson 3 – Lime Demand Increases after NP at Surface is Depleted







Annual pH / Conductivity Surveys



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Acidity Mass Balance





Need for Refinements

- Stop depositing in small areas for long periods reducing exposure times in older areas
- Reconfigure deposition areas
- Remove Jarosite from tailings
- Evaluate Lime Demand
 - Annual
 - Maximum Daily





Multiple Discharge Points







New Deposition Cycle and Internal



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The Lime Demand Model

Sources of acidity:

> oxidation of the sulphides near surface prior to covering with fresh material

- > acid released from the aged acidic tailings
- jarosite dissolution (iron sulphate bi-product of zinc process that dissolves and releases acid)
- > oxidation of thiosalts in mill process water

Variables affecting lime demand:

- acid generating factors (above)
- tailings Neutralizing Potential (NP)
- deposition cycling period (and LAG time)



Past Investigations

• Field study:

➤ The inactive area (base load) was estimated by pore water measurements to be 2,600 t-CaO/a.

> NP depletion rate from sulphide oxidation is 4 kg-CaCO₃/t/a.

Laboratory testing:

 \succ Mixture of jarosite in tailings showed that the half-life of jarosite is between 1 and 3 years.

> Pilot studies showed that the NP of mine D tailings (uncertain among the three) ranges from 5 to 23 kg-CaCO₃/t.



Calibration of the Model

- The lime demand from the active tailings using measured oxygen consumption rates.
- Jarosite dissolution rates from lab studies.
- The lime demand from the inactive perimeter tailings (base load) from field measurements.
- The model was then calibrated for the basecase conditions using the historical data.



Calibration of the Model and Prediction of Future Lime Demand



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Sensitivity Analysis

- Sensitivity analysis was performed to address uncertainty
- The factors and their levels are (**bold for base-case**):

 \succ Tailings deposition time: 1.5 – 3 years

Jarosite disposal: separate disposal – codisposal with tailings

> Tailings NP content: 5 - 10 - 14 - 23 kg CaCO₃/t

> Jarosite dissolution half-life: 1 - 1.5 - 2 years

> Sulphide oxidation rate: 2 - 4 - 6 kg CaCO₃/t/a



Effects of NP of Mine D Tailings on the Lime Demand





Effects of Jarosite Co-Disposal / Deposition Cycle Time





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Effects of Jarosite Removal in Future Years





Partitioning of Lime Demand to different Components

Base case – 2010:

- Active area: 17%
- Jarosite dissolution: 38%
- Thiosalt oxidation: 14%
- Inactive area: 23%
- Pump box: 8%
- Total Lime demand: 8100 t CaO

No-Jarosite – 1.5 year cycle – 2010:

- Inactive area: 72%
- Pump box: 28%
- Total Lime demand: 3600 t CaO



Conclusions

- Optimal cycle time for 0.3 m fresh tailings per cycle (1.5 years).
- The NP of the Mine D tailings and the average annual oxidation rate of sulphides are the two most important variables that will control lime demand.
- The presence of jarosite in the tailings can increase lime demand by 5,000 to 6,000 t-CaO/a and scheduled to be removed by late 2007 / early 2008.
- Proper cycling and deposition management can eliminate lime demand during operations.
- The largest uncertainty is the NP of the tailings and appropriate characterization is required to predict actual lime demand



The Art of Tailings Management

Photos: P.A. Tibble







