

# Mine water treatment, resource recovery and sustainability

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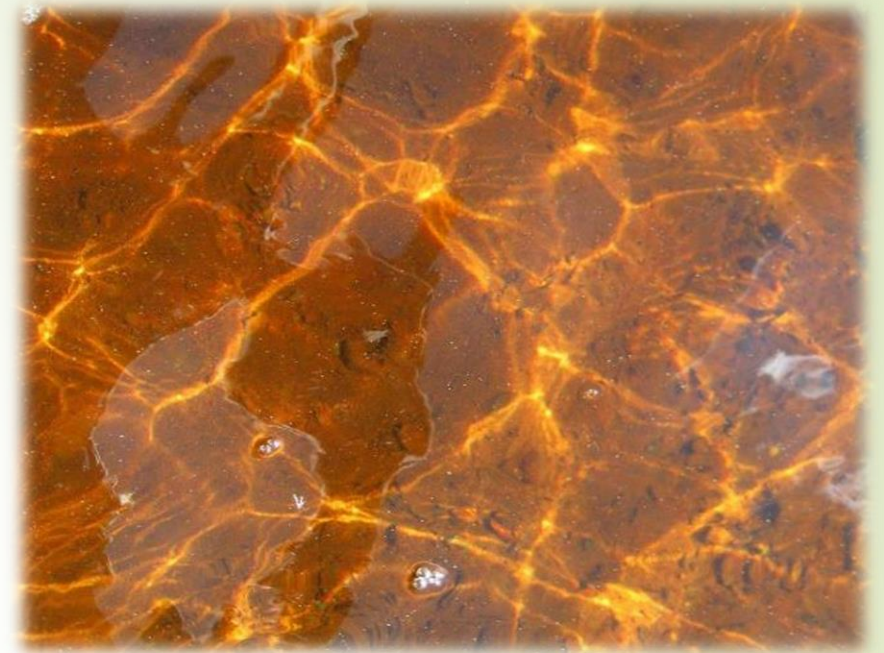
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Chair

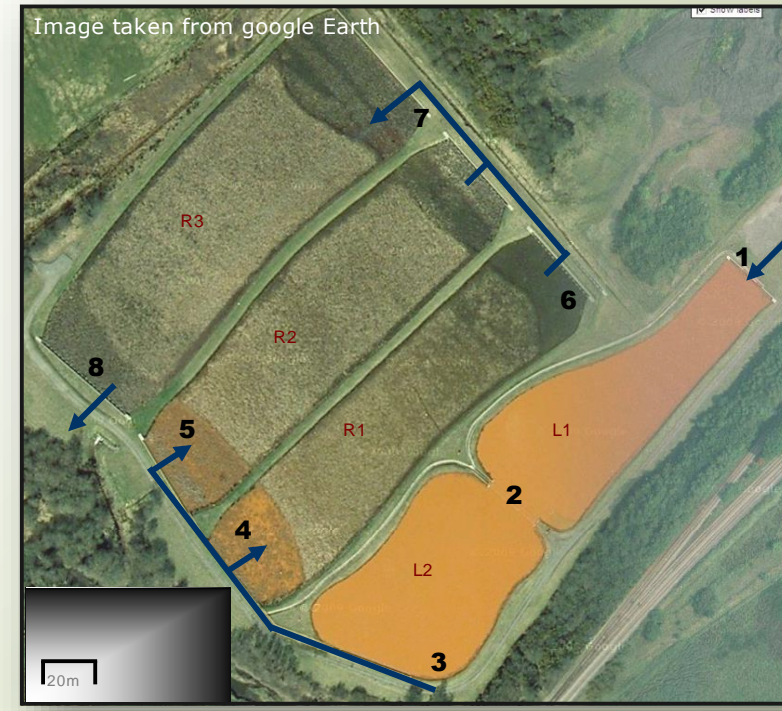






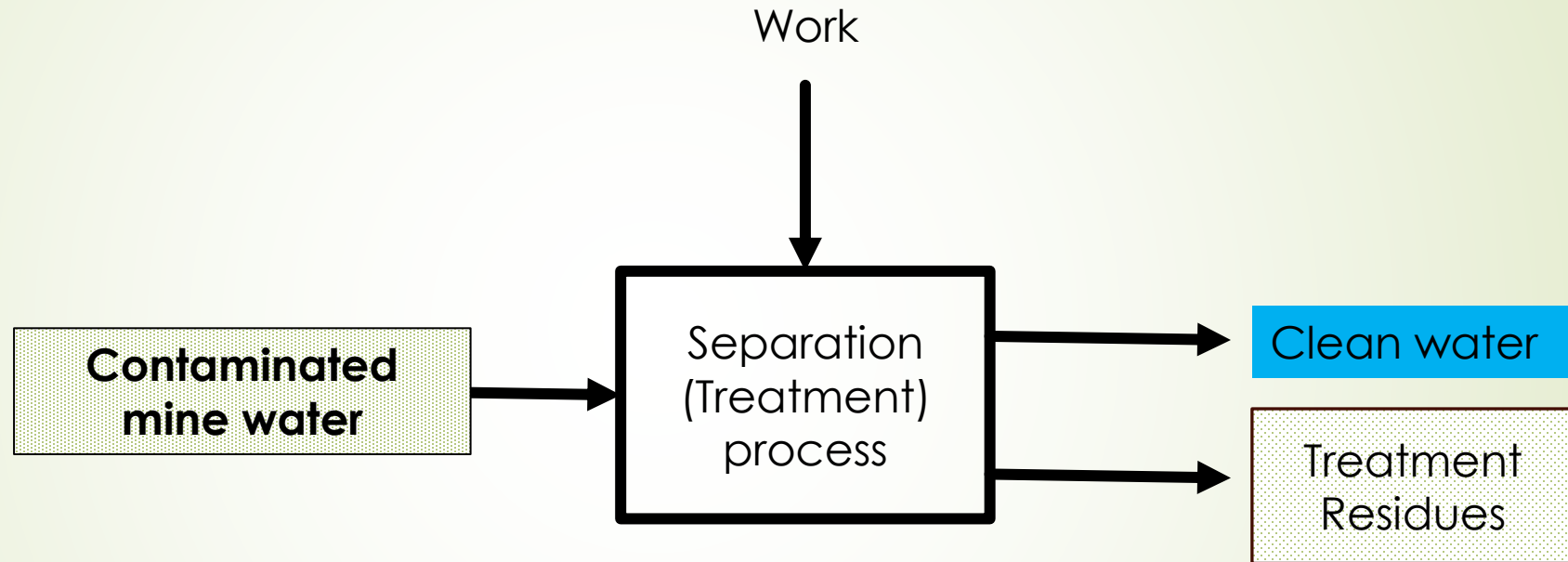


# Mine water treatment: Passive v. Active and sustainability



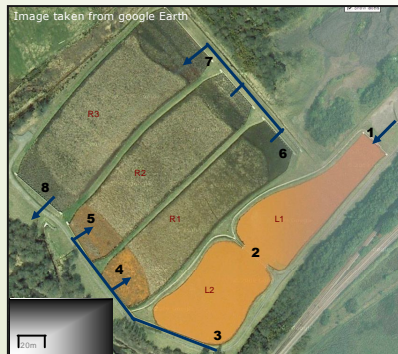
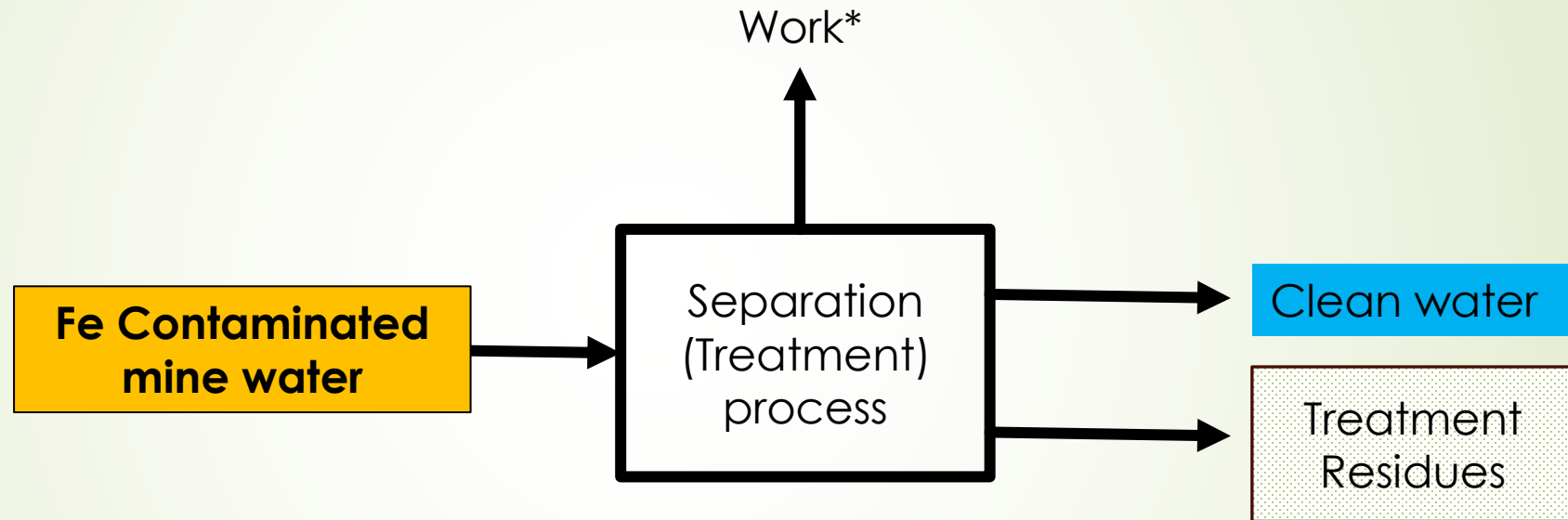


## Mine water treatment process



....but not for all contaminants

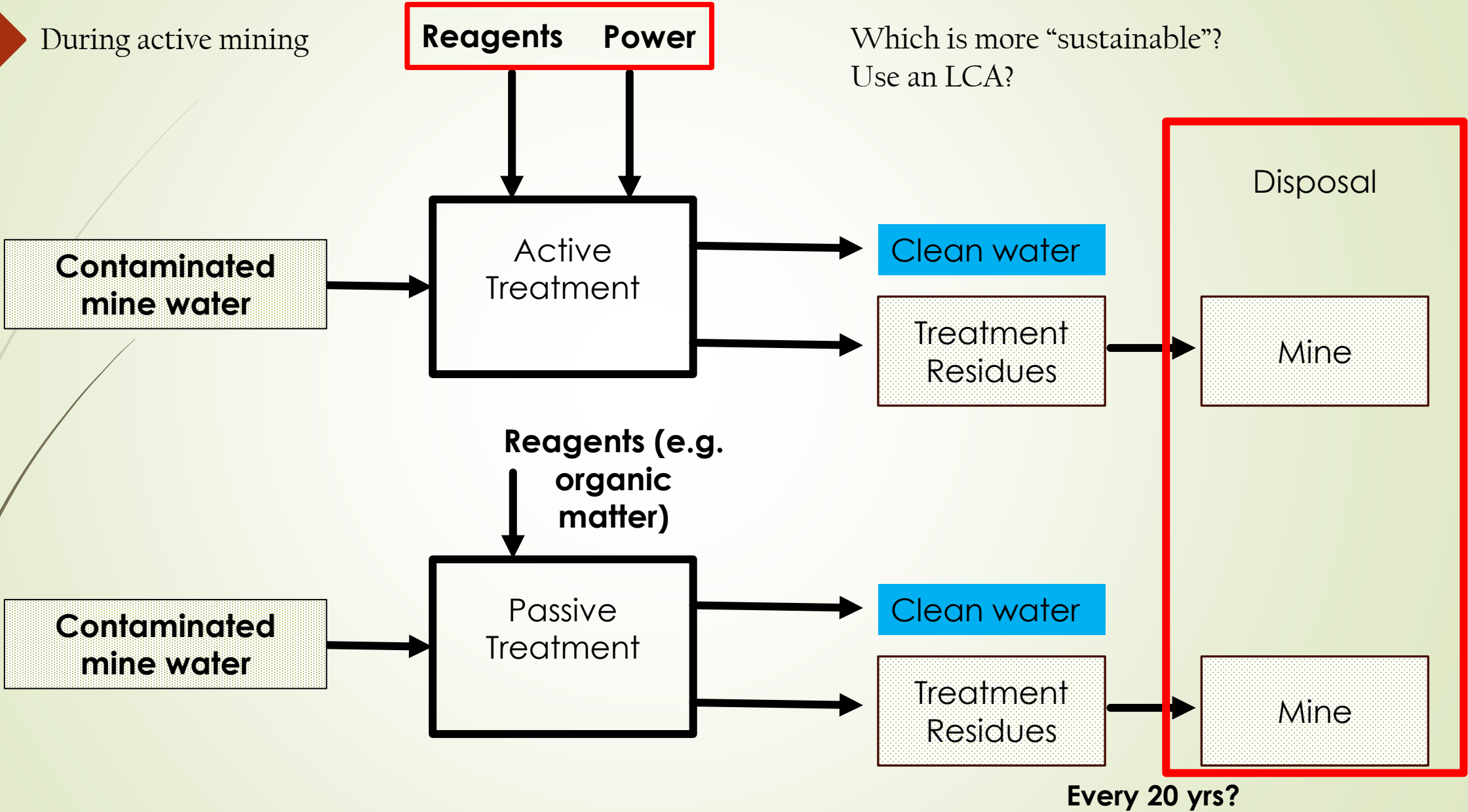
\*Cheng, S., Dempsey, B.A. and Logan, B.E., 2007. Electricity generation from synthetic acid-mine drainage (AMD) water using fuel cell technologies. Environmental Science & Technology, 41 (23), pp.8149-8153.



Which is lower cost?

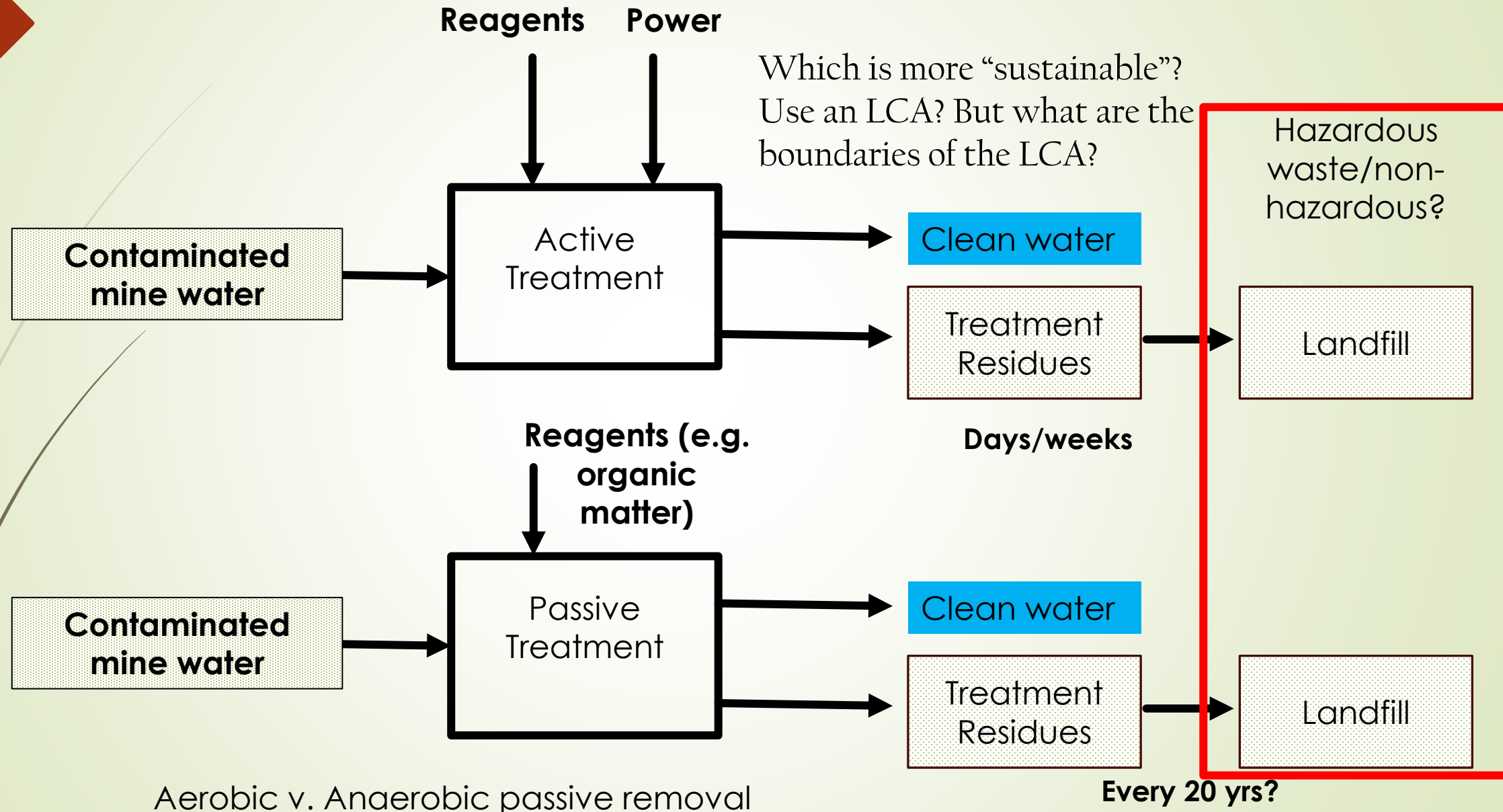
Which is more “sustainable”?  
Use an LCA?

During active mining



Legacy mine water in highly waste-regulated countries such as UK

Which is lower cost? Hazardous waste disposal a costly problem



# Outcomes from the METAL-SoVLER project



The central research questions are around cost and sustainability/circularity:

Can passive and semi-passive treatment options which produce residues which are either easy to recycle/reprocess or at least have improved waste disposal cost implications?



## Semi-passive (or semi-active) treatment of circumneutral zinc-bearing drainage



Abbey Consols and sodium carbonate dosing – why  $\text{Na}_2\text{CO}_3$ ?



# Previous work

Field trial 2020 (NRW, WSP and Cardiff University)



## 1. Zinc concentration in effluent

- Dissolved zinc remaining in effluent 9-42%
- Total zinc remaining in effluent 39-73%

## 2. Precipitate properties

- Moisture content - 95%
- Zn content – 46%
- Inorganic carbon – 1.2%

## Lab Research Objectives

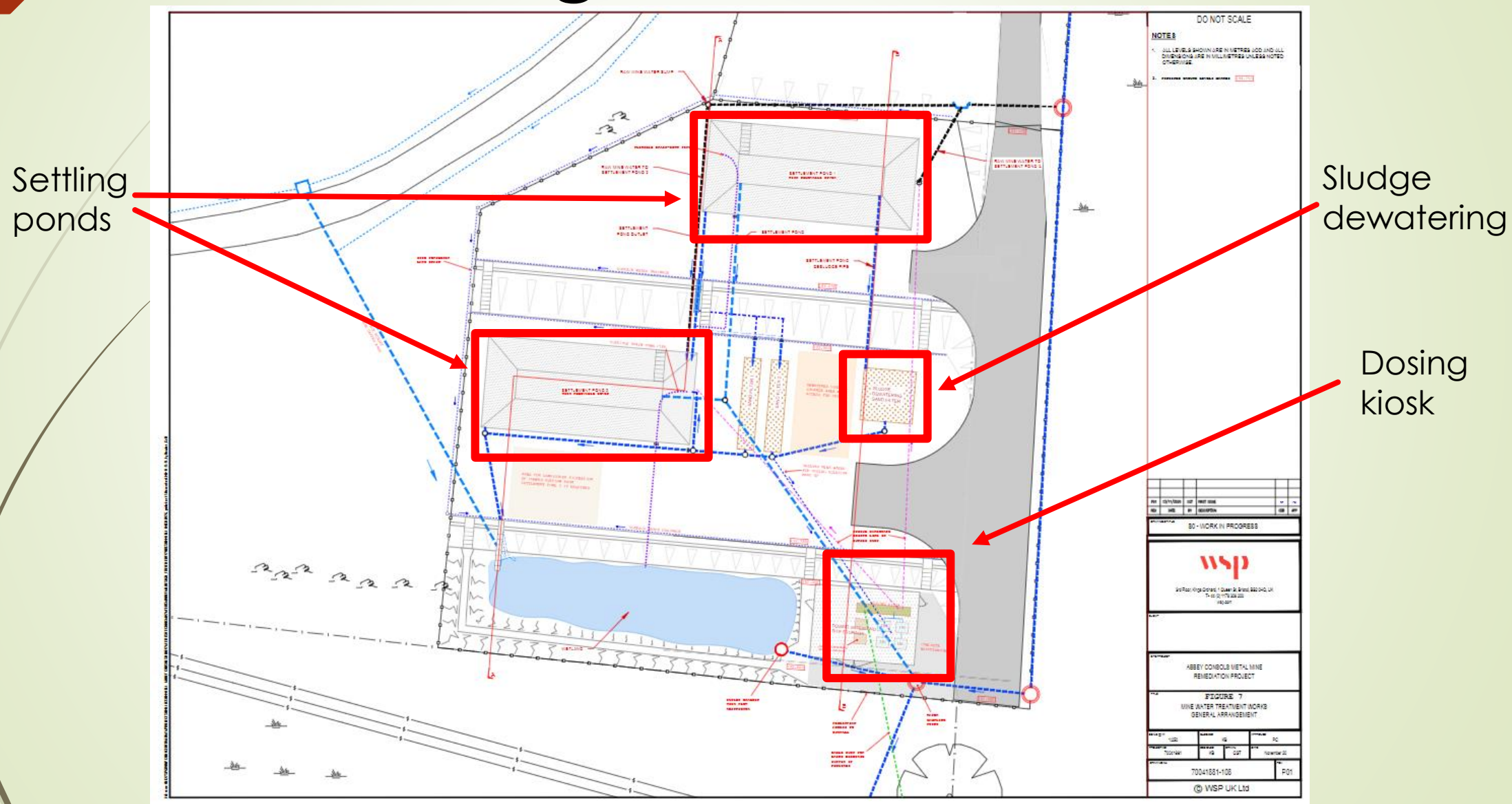
1. Research methods to increase settling velocity/reduce sludge volume
2. Characterize precipitate

[1] Williams, T., Dent, J., Eckhardt, T., Riding, M. and Sapsford, D., 2020. Treatability Trials to Remove Zinc from Abbey Consols Mine Water, Wales, UK. Pope, J. et al, pp.225-230. [2] Dean, J., Alkhazraji, B. and Sapsford, D.J., 2021. Alternative reagents for the treatment of Pb-Zn mine drainage in Wales. In IMWA 2021—"Mine Water Management for Future Generations (pp. 109-114)..



# Reactor Design

## Full scale demonstrator build



# Methods to increase settling velocity/reduce sludge volume

## Jar tests

Established optimum dose and time to react

- 1:3.5
- Very fast reaction

## Dosing rate

- Slower rate of addition halved sludge volume
- Potential to trial this at full scale
- Trial multipoint dosing within the settling ponds

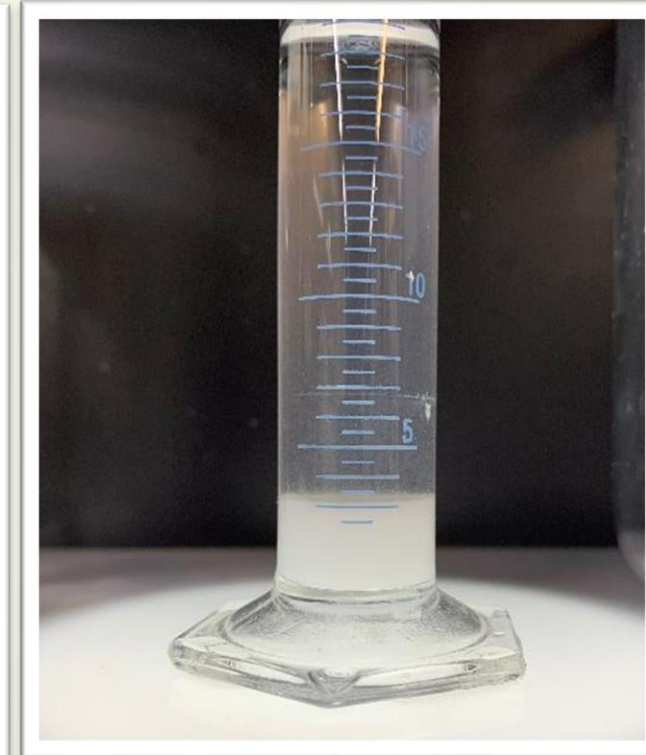
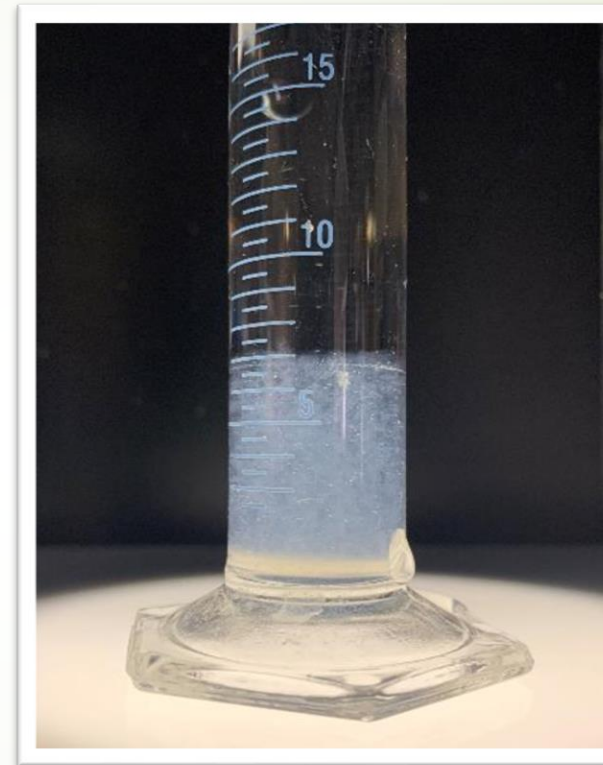
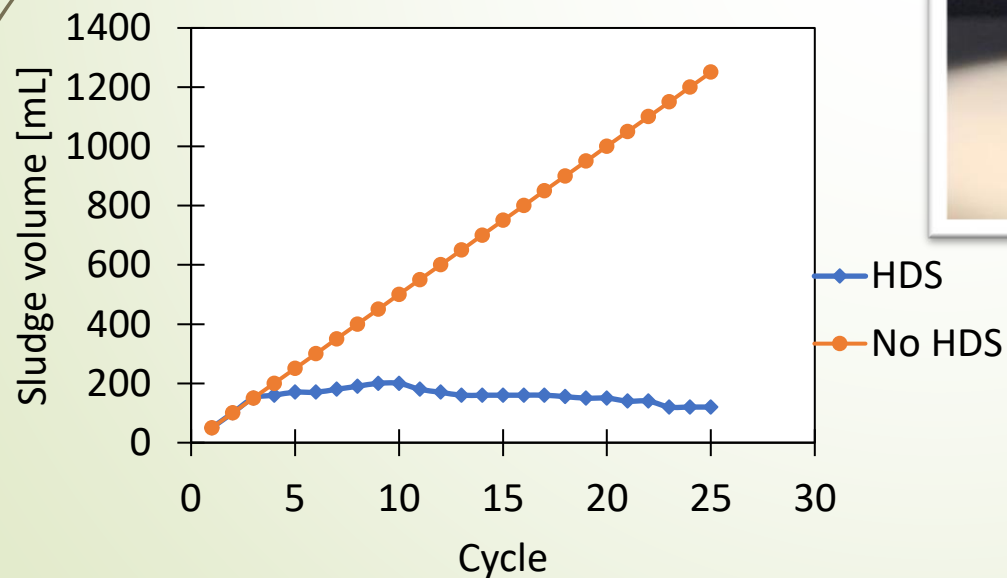




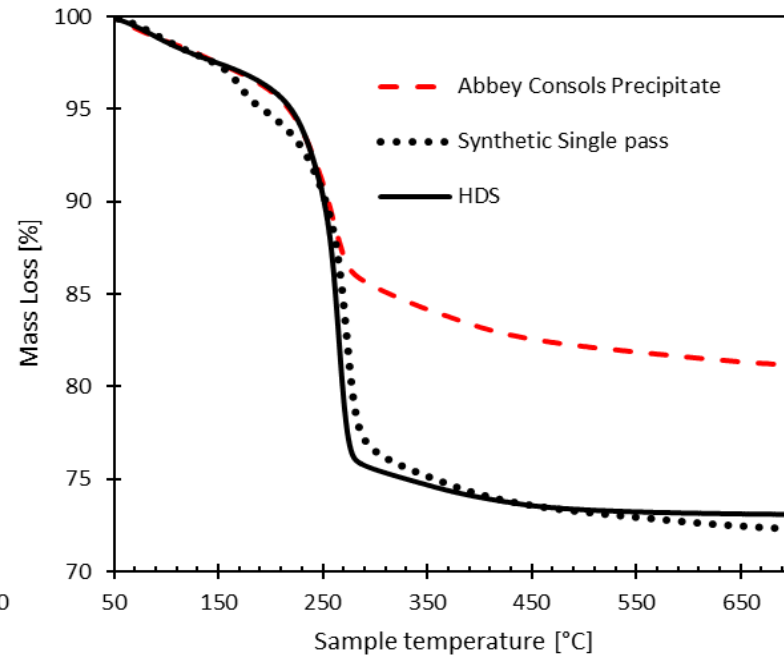
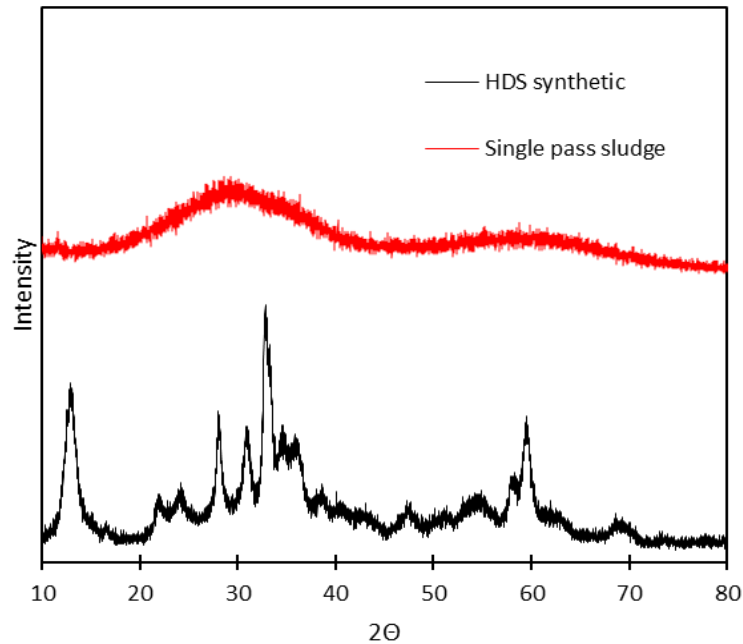
# Methods to increase settling velocity/reduce sludge volume

## High Density Sludge formation

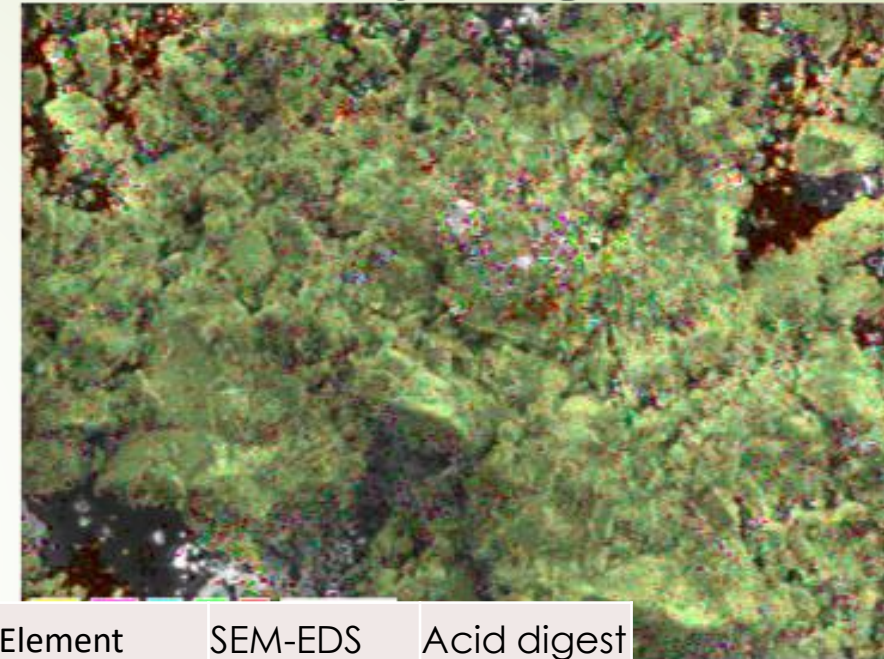
- Zn/ $\text{Na}_2\text{CO}_3$  system readily forms HDS
- Reduce sludge volume ca. 10X
- **Without use of flocculant**
- Trial recycling of sludge at full scale



# Characterization of sludge



EDS Layered Image 1

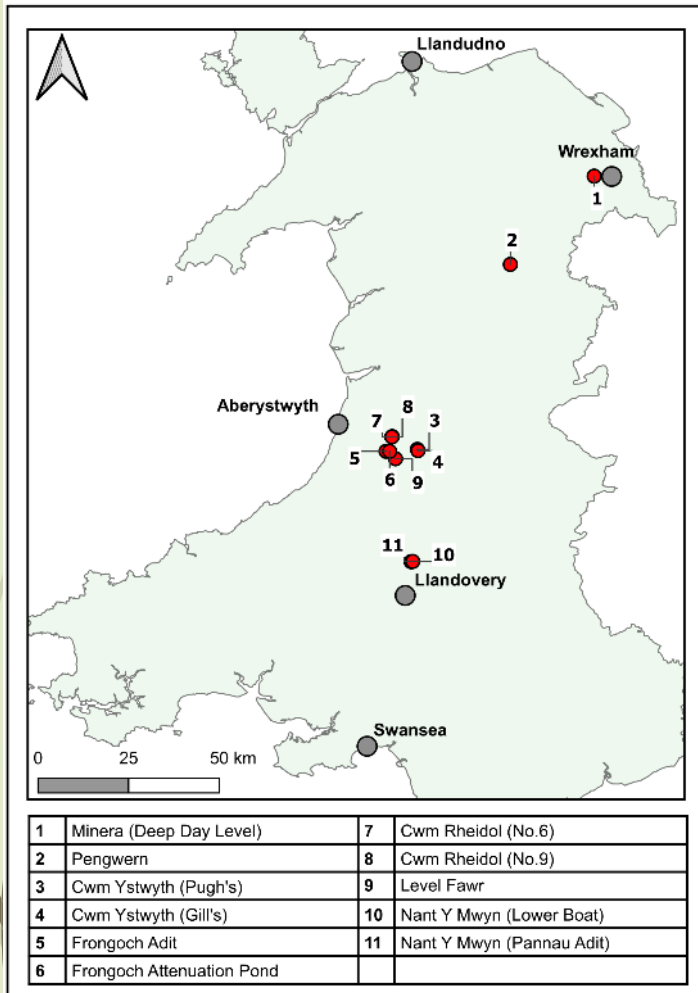


Element	SEM-EDS	Acid digest
Zn	45	48.90
O	30	NA
C	15	NA
Si	5	NA
Na	4	0.10
Pb	1	1.00
Ca	ND	0.20
Fe	ND	0.02
Al	ND	0.25

Recycle/reprocess or dispose?



# Widescale trials



Site	pH	Alkalinity as CaCO <sub>3</sub> mgL <sup>-1</sup>	Zinc mgL <sup>-1</sup>	Iron mgL <sup>-1</sup>	Estimated flow Ls <sup>-1</sup>	Zn load kg yr <sup>-1</sup>
Minera- Deep Day Level	7.4	235	1.62	0.23	50	2547
Pengwern (Llangynog)	7.4	35	4.43	N/A	15	2095
Cwmystwyth- Pugh's	6.6	14	31.8	0.40	9.6	9639
Cwmystwyth- Gill's	6.5	0	8.69	0.03	3.2	877
Frongoch Adit	7.0	13	17.9	0.03	17	9607
Frongoch attenuation pond	5.1	0	202	0.03	6	38146
Cwm Rheidol- No.6	3.7	0	51.4	3.4	8.3	13462
Cwm Rheidol- No.9	2.8	0	53.9	84	0.6	1020
Level Fawr	7.3	0	1.60	0.03	21	1058
Nant y Mwyn- Lower Boat	5.8	76	14.8	N/A	51	23787
Nant y Mwyn- Pannau Adit	7.2	76	5.70	N/A	3	539

# Field Campaign Results

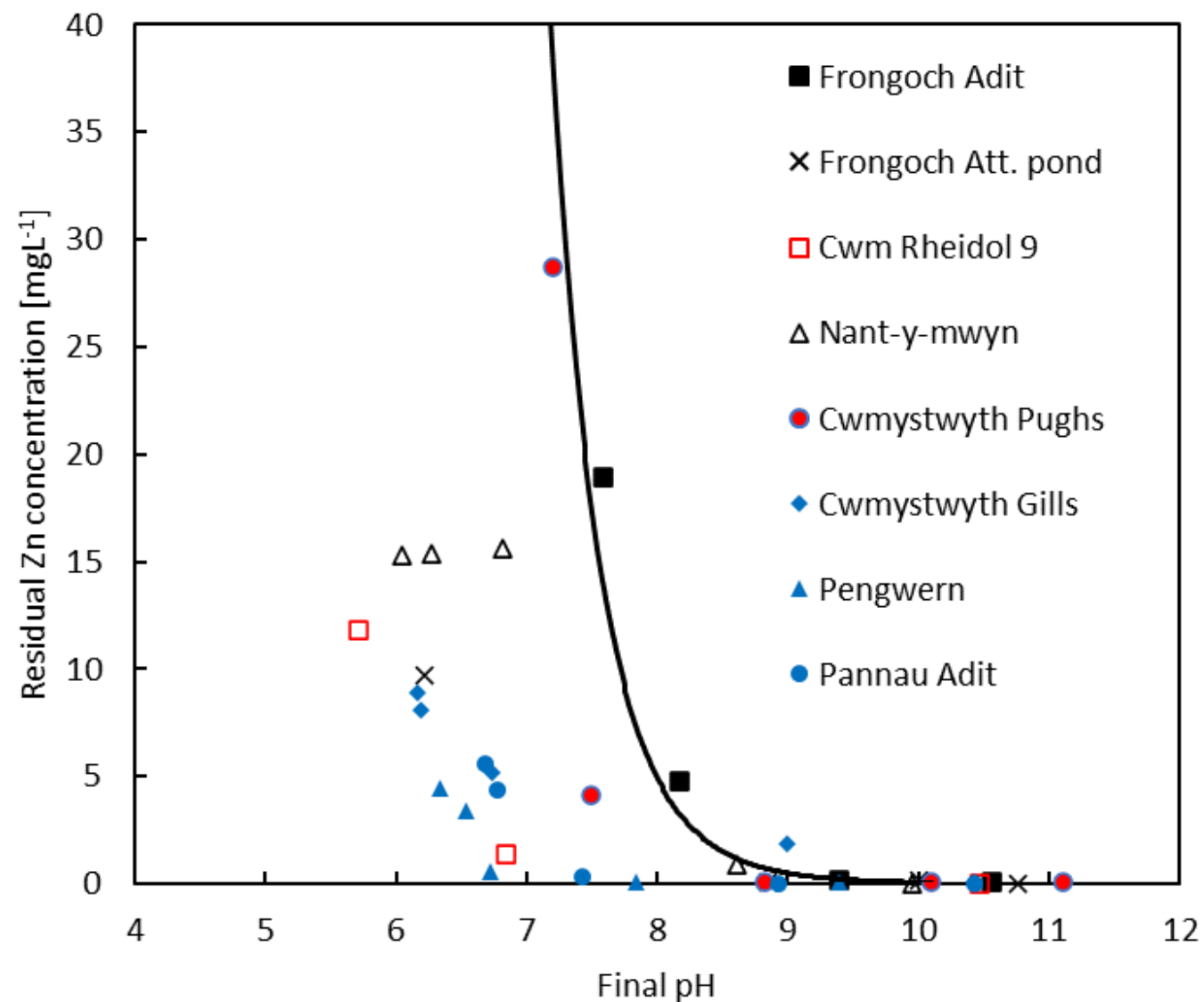
Site	Zn removal %	Na <sub>2</sub> CO <sub>3</sub> dose mgL <sup>-1</sup>	Molar ratio Zn:Na <sub>2</sub> CO <sub>3</sub>	Zinc mgL <sup>-1</sup>	Final pH
Minera- Deep Day Level*	25	74	1:28	1.210	7.4
Pengwern (Llangynog)	98	32	1:5	0.084	7.8
Cwmystwyth- Pugh's	>99	189	1:4	0.084	8.8
Cwmystwyth- Gill's	99	367	1:26	0.066	10.4
Frongoch Adit	99	224	1:8	0.145	9.4
Frongoch attenuation pond	>99	749	1:2	0.086	8.9
Cwm Rheidol- No.6	>99	209	1:3	0.056	9.1
Cwm Rheidol- No.9	99	6001	1:78	0.624	10.5
Level Fawr	95	88	1:34	0.073	9.3
Nant y Mwyn- Lower Boat	>99	874	1:37	0.876	9.9
Nant y Mwyn- Pannau Adit	>99	34	1:4	0.313	8.9

**Na<sub>2</sub>CO<sub>3</sub> dosing successful for 10 out of 11 sites**

Site	As %	Cd %	Cu %	Mn %	Ni %	Pb %
Minera- Deep Day Level	41	12	18	0	3	84
Pengwern (Llangynog)	70	80	NA	19	11	85
Cwmystwyth- Pugh's	58	98	94	81	83	96
Cwmystwyth- Gill's	74	>99	86	92	94	97
Frongoch Adit	0	99	76	91	69	88
Frongoch attenuation pond	10	99	99	96	>99	99
Cwm Rheidol- No.6	83	>99	99	93	98	>99
Cwm Rheidol- No.9	82	>99	99	>99	>99	>99
Level Fawr	29	79	47	18	8	41
Nant y Mwyn- Lower Boat	NA	>99	95	NA	99	NA
Nant y Mwyn- Pannau Adit	NA	99	NA	NA	78	NA

**Effective removal of Cd, Pb, Cu**

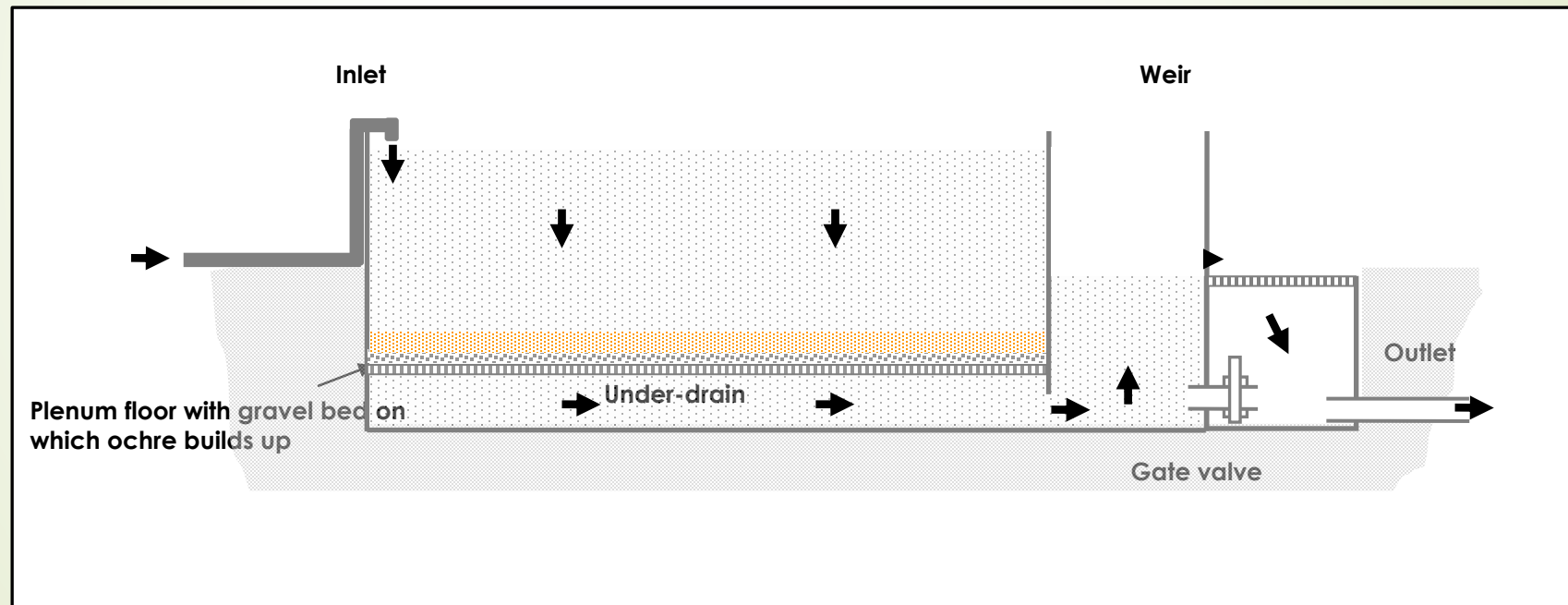




Measured residual Zn concentration at the final pH after Na<sub>2</sub>CO<sub>3</sub> dosing. Line represents hydrozincite solubility curve (logK 9.1\*) calculated using PHREEQC. Red symbols signify elevated Fe levels and blue symbols indicate mine water <15°C at time of on site dosing

# Aerobic Passive Treatment: Vertical Flow Reactors (VFRs)

Enhanced iron removal by (self) filtration of ochre particles and surface-catalysed oxidation of dissolved iron – international trials have shown excellent removal of Fe at circumneutral pH and in some cases at pH 3







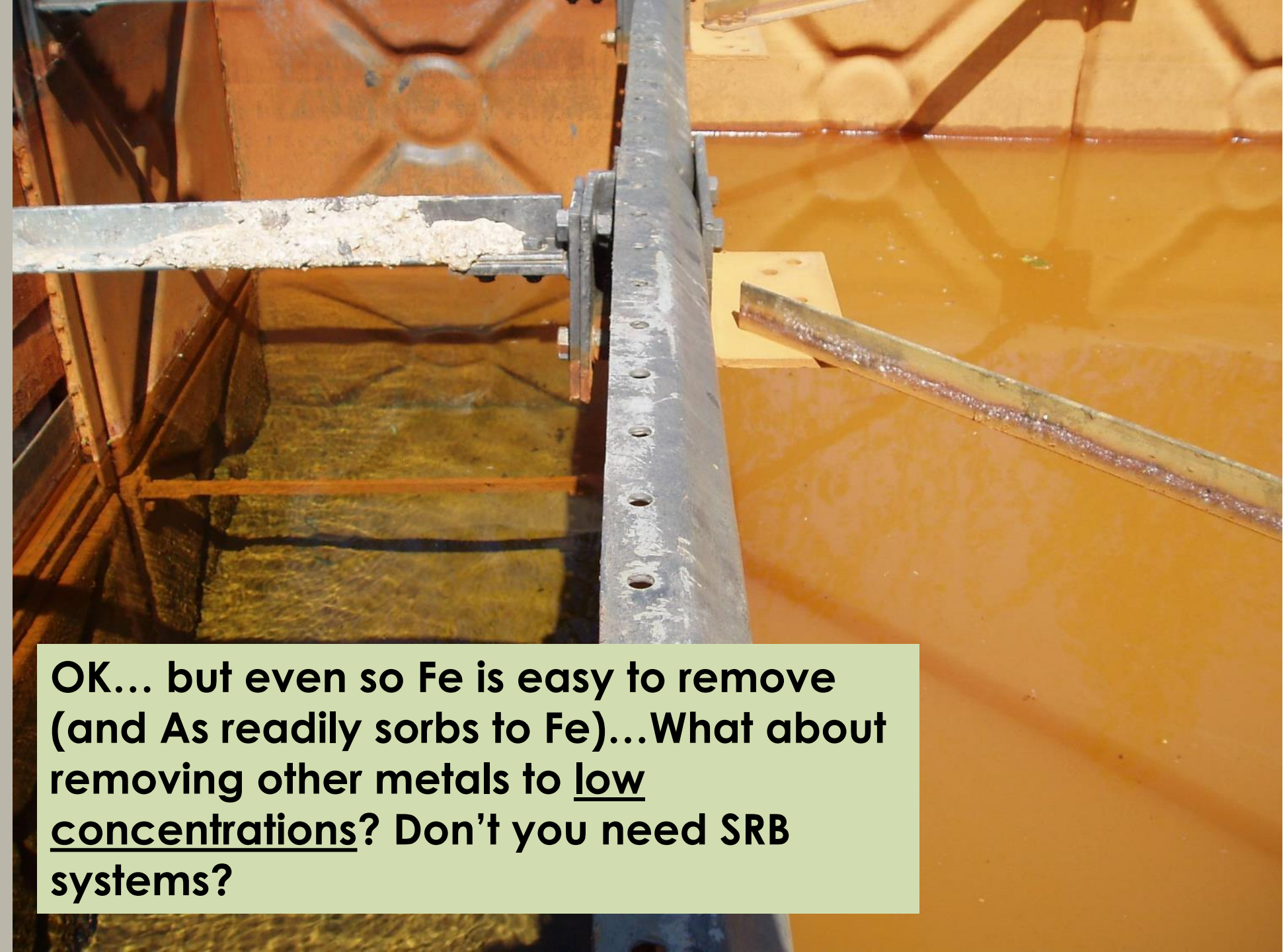
2007

**Developed originally on coal mine  
drainage**

Heterogeneous Fe(II) oxidation  
Cake filtration of particulate  
Fe(III)  
Microbiological Fe(II) and Mn(II)  
oxidation

Shown for Fe to work for  $> \text{pH } 3$





OK... but even so Fe is easy to remove  
(and As readily sorbs to Fe)...What about  
removing other metals to low  
concentrations? Don't you need SRB  
systems?



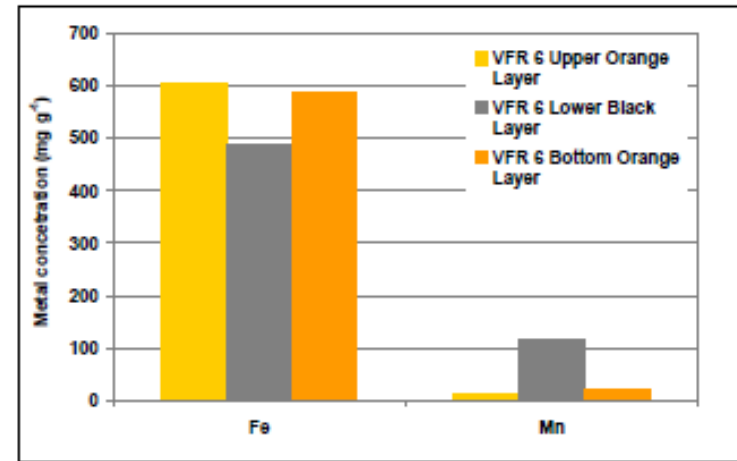
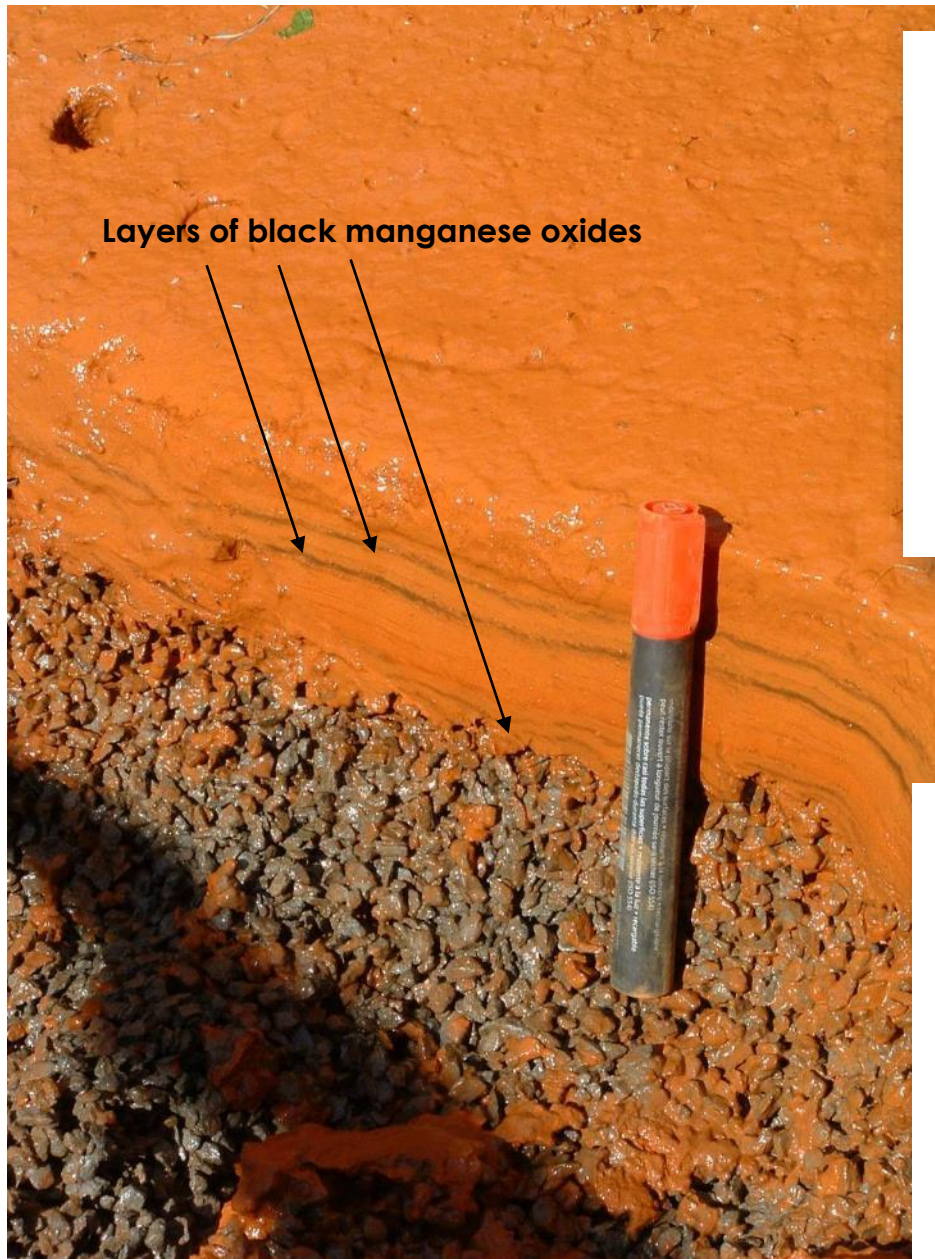


Figure 7-20: Fe and Mn concentrations in ochre bed layers

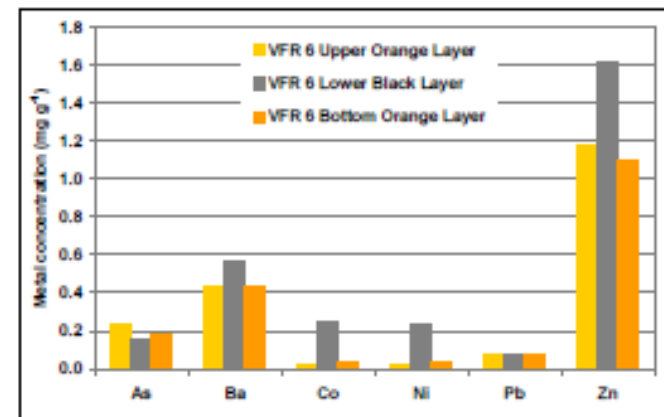


Figure 7-21: Al, As, Ba, Co, Ni, Pb and Zn concentrations in ochre bed layers

Promotion of autocatalysis and microbial oxidation (A. Barnes PhD thesis, 2008, Cardiff University)



# IBC and Column Vertical Flow Reactors (VFRs) – can the mine water be self-cleaning?



## IBC VFR:

Flow rate: 300 mL/min  
Water head: 40 cm  
20 mm gravel: 12 cm  
6 mm gravel: 10 cm  
Total nominal HRT: ~27 hrs (~22 hrs for the water head; ~5 hrs within media)



**G:** gravel only columns (5 cm)

**GS:** columns with gravel seeded with pyrolusite (2 cm)

**C:** control columns

**MH:** ManHole

**HT:** Header Tank

**G1**

**C2**

**GS3**

**G4**

**GS5**

**G6**

**G7**

**C8**

## Flow rate:

3.0 mL/min for each column

## Residence time:

**G:** ~20 hrs (~18 hrs for water head; ~1 hr within media)

**GS:** ~19 hrs (~17.5 hrs for the water head; ~1.5 hrs within media)

**C:** ~21 hrs



## Limestone Media



**GS3** and **GS5**: gravel column VFRs seeded with pyrolusite  
**LSR4** and **LSR6**: limestone reactors

**LSR Flow rate**: 3.0 mL/min

**LSR Residence time**: ~3 hrs (1 hr for the water head; 2 hrs within media)

Day  
zero

LSR  
surface



LSR column  
wall

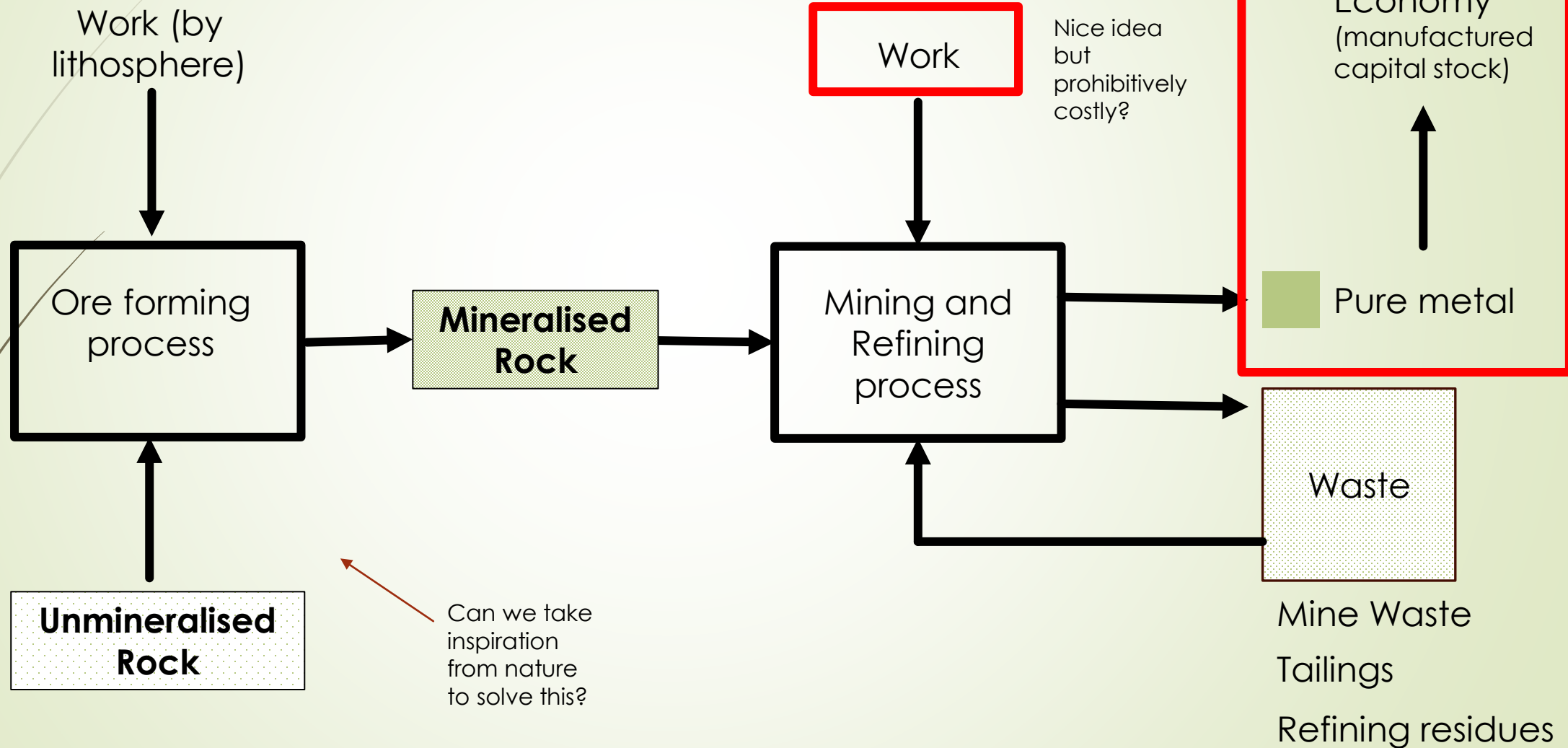


After about three months –  
excellent removal of Mn and Zn



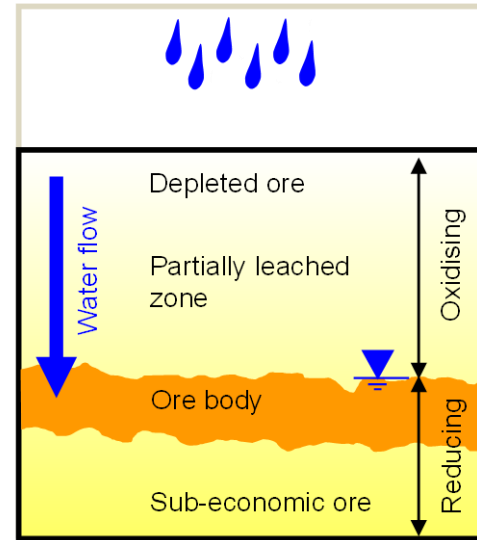
dark coating indicates Mn  
removal.

Alternative concept for mine waste management: Can we push as much of the metals as possible to the economy?

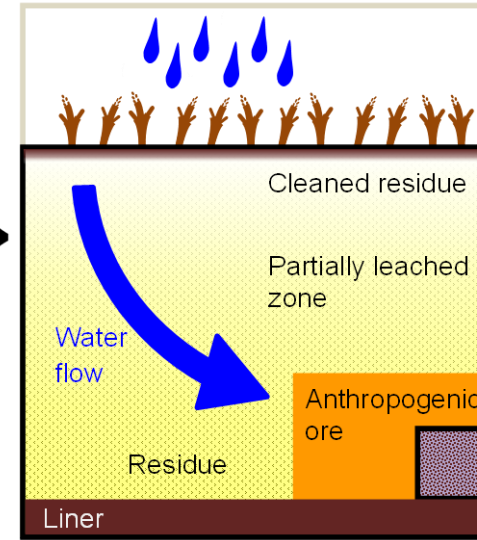




Use the prolonged time in storage to apply green low-intensity and low-cost processes



(a) Supergene ore forming processes



(b) ASPIRE repository

Now no longer AMD-ML threat and perhaps can be reused (e.g. aggregate)

Now at concentrations economically viable to process

# ASPIRE

Accelerated Supergene Processes in Repository Engineering

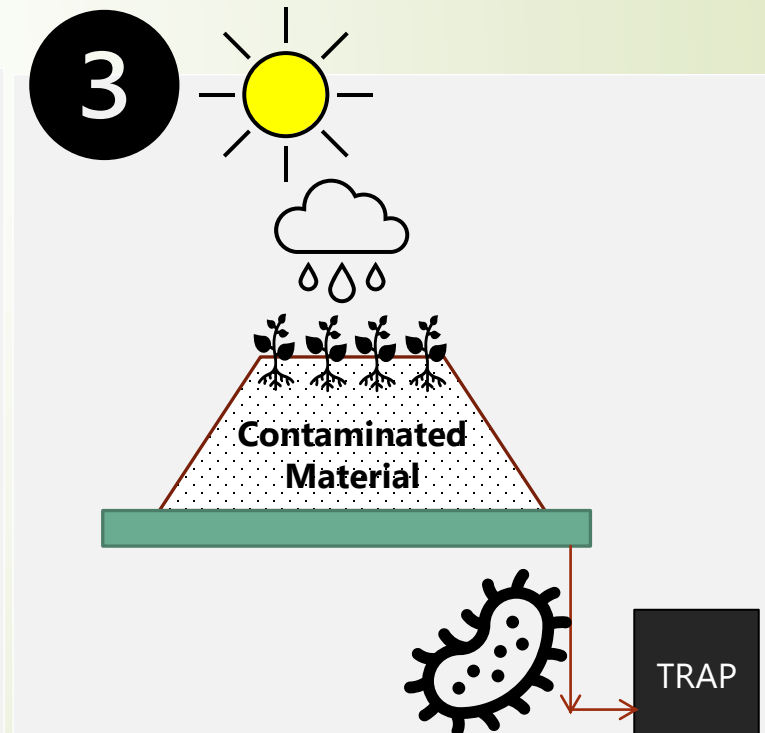
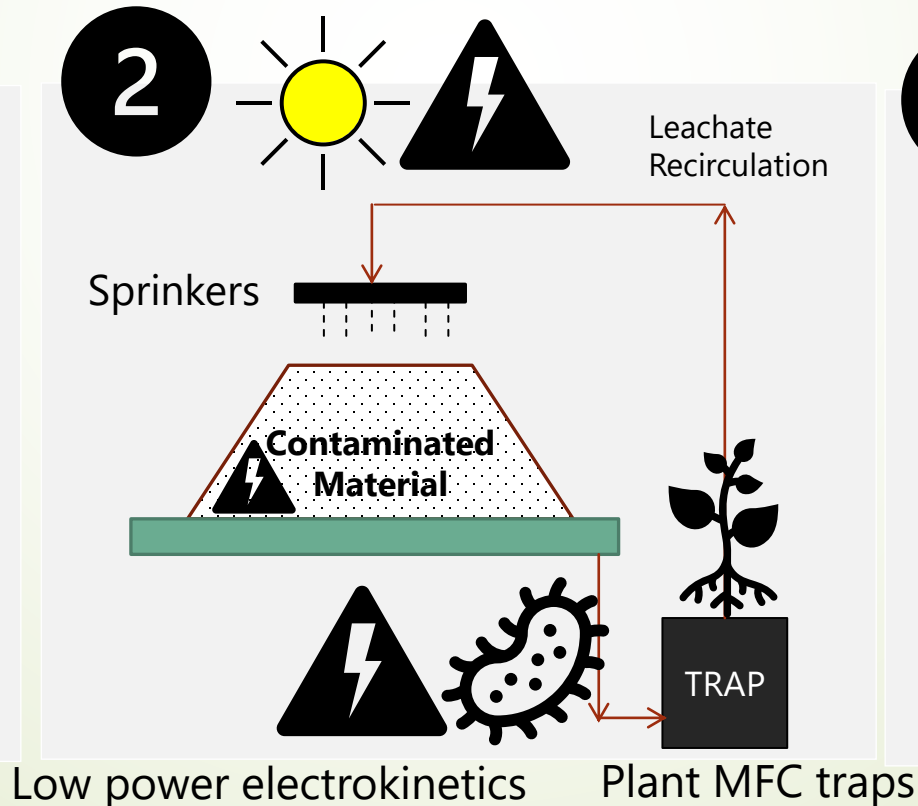
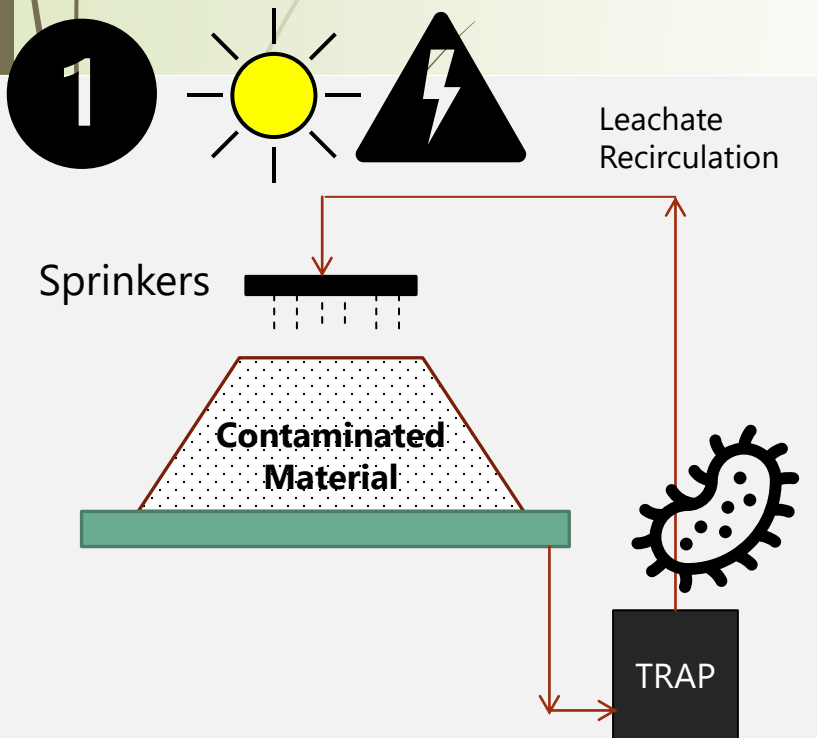
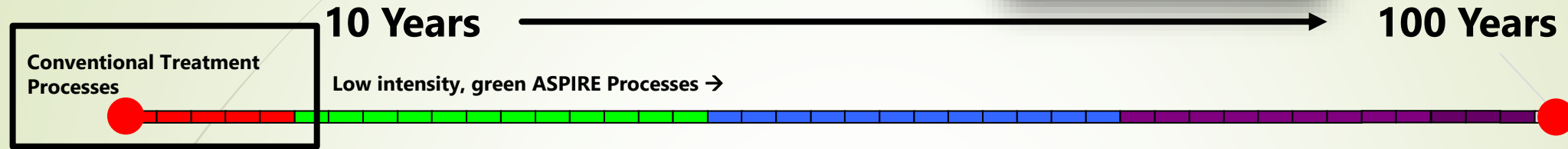
*“Developing self-cleaning, temporary storage landfills for returning materials to a Circular Economy”*



# ASPIRE Concept

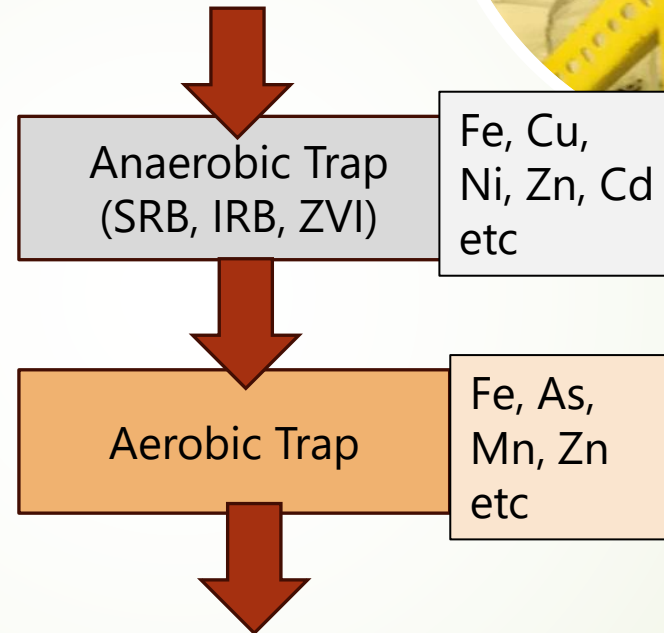
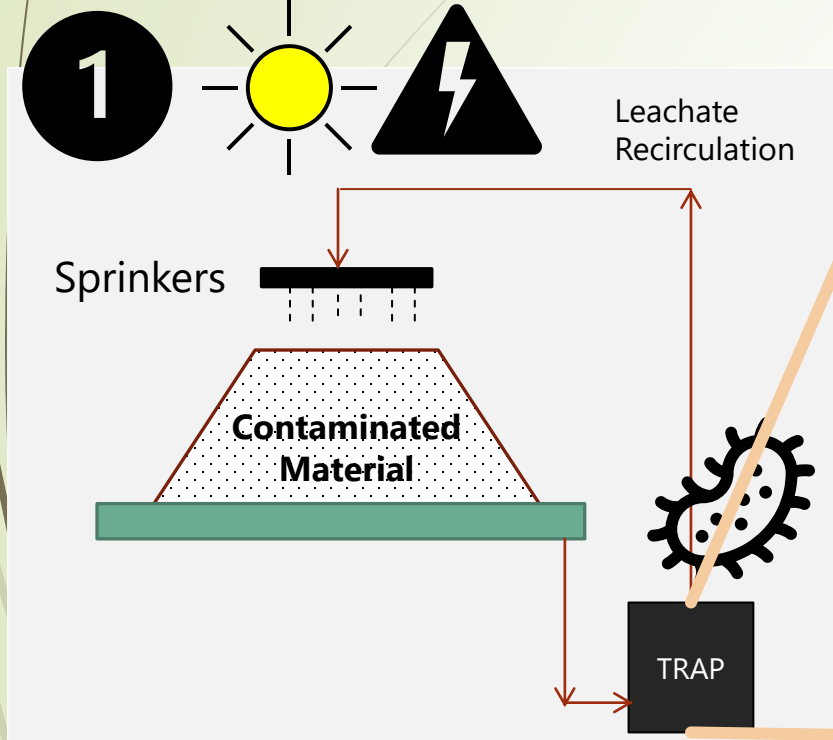


Carbon storage may become an important consideration



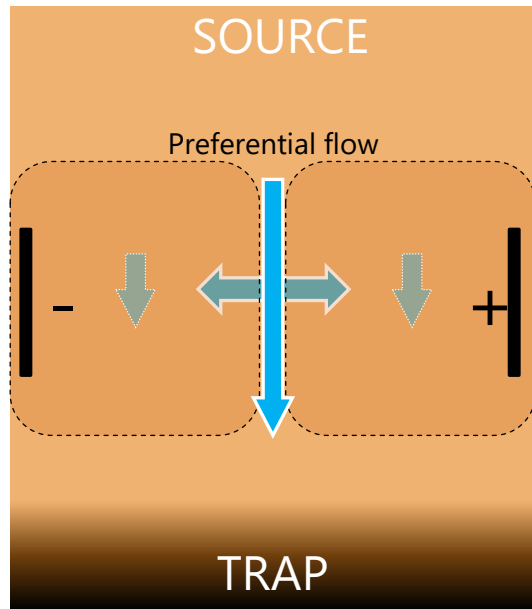
# Trapping technologies

(a.k.a anthropogenic ore forming processes?)  
(a.k.a mine water treatment!)





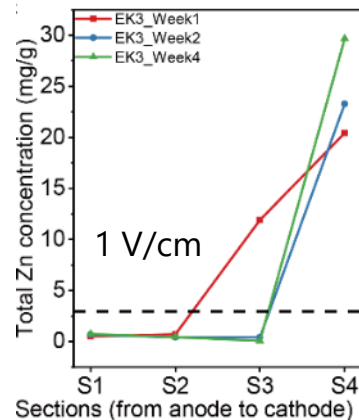
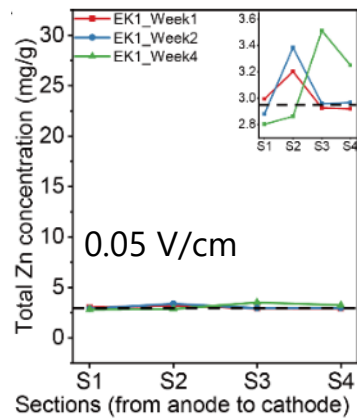
# Bioelectrochemical systems for resource mobilisation, transport and recovery



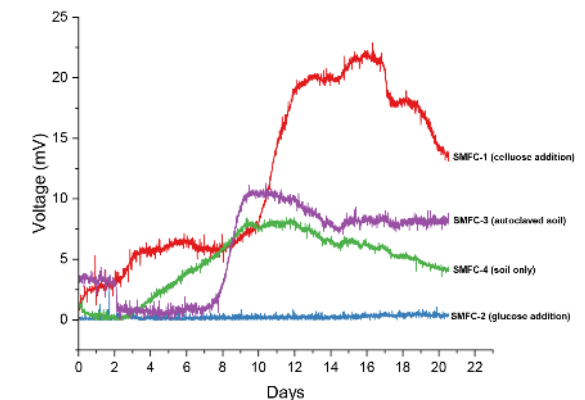
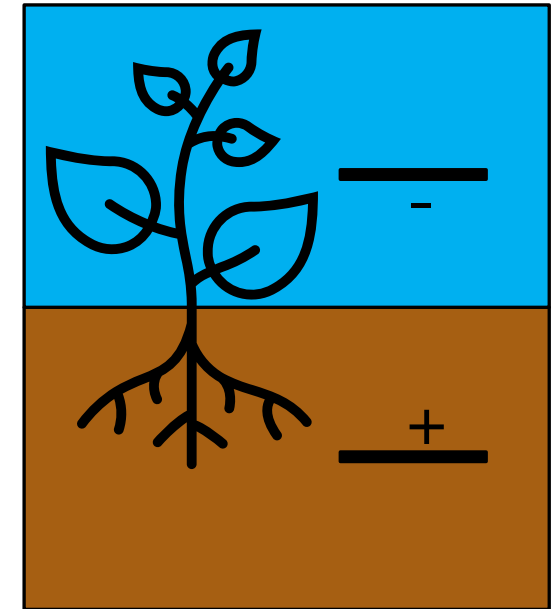
Transport – overcoming preferential flow to maximise transport through matrix

Bioelectrochemical systems – low power but self-sustaining

Low voltage gradients and their effects



Microbial & plant-microbial fuel cells can potentially mobilise, transport *and* trap resource.





# Conclusions for mine waste treatment, resource recovery and sustainability

- Current passive treatment systems produce wastes which need disposal
- Disposal of mine water treatment residues and mine wastes in landfills potentially only postpones future problematic contaminant escapes
- Is there room for new more sustainable concepts which aim to push for metals to the economy. Not for economic reasons but to avoid/minimise the waste issue?
- The problem to solve becomes one of how to do this economically. This is what we're looking at with the ASPIRE concept.
- Value-adding propositions include reuse of cleaned residue and/or CDR
- Passive, semi-passive and bioelectrochemical technologies (many already used for mine water treatment) could offer solutions



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